

## Electrocatalysis

Deutsche Ausgabe: DOI: 10.1002/ange.201713003  
Internationale Ausgabe: DOI: 10.1002/anie.201713003**Densely Packed, Ultra Small SnO Nanoparticles for Enhanced Activity and Selectivity in Electrochemical CO<sub>2</sub> Reduction**

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**Abstract:** Controlling the selectivity in electrochemical CO<sub>2</sub> reduction is an unsolved challenge. While tin (Sn) has emerged as a promising non-precious catalyst for CO<sub>2</sub> electroreduction, most Sn-based catalysts produce formate as the major product, which is less desirable than CO in terms of separation and further use. Tin monoxide (SnO) nanoparticles supported on carbon black were synthesized and assembled and their application in CO<sub>2</sub> reduction was studied. Remarkably high selectivity and partial current densities for CO formation were obtained using these SnO nanoparticles compared to other Sn catalysts. The high activity is attributed to the ultra-small size of the nanoparticles (2.6 nm), while the high selectivity is attributed to a local pH effect arising from the dense packing of nanoparticles in the conductive carbon black matrix.

**E**lectrochemical reduction of CO<sub>2</sub> to form carbon-based fuels and chemicals has been widely proposed for the storage and utilization of intermittent renewable energies such as solar and wind.<sup>[1]</sup> However, two major deficiencies have prevented CO<sub>2</sub> electroreduction from becoming a viable technology: energy inefficiency owing to large overpotentials, and poor selectivity leading to separation issues. Therefore, there is tremendous interest in developing active and selective electrocatalysts for CO<sub>2</sub> reduction. In terms of electrochemical activity, noble-metal catalysts rank the best.<sup>[2]</sup> Among non-noble metal catalysts, Sn-based catalysts stand out.<sup>[3,4]</sup> However, the major CO<sub>2</sub> reduction product using Sn catalysts is formate (HCOO<sup>-</sup>), and CO is generated only in a small amount.<sup>[5]</sup> Unlike its acidic form, formic acid which is a high-value chemical, formate has no obvious usage and is difficult to separate and convert into other high-value products without adding costly processes. CO, on the other hand, is a highly desirable product as it is a gas that can be easily separated and further converted into fuels and bulk chemicals at a large scale through existing chemical technologies. Achieving high activity and selectivity for CO formation on

a non-precious catalyst such as Sn is therefore a notable goal with practical relevance.

The CO<sub>2</sub> electroreduction performance of Sn based catalysts developed recent years is summarized in the Supporting Information, Figure S4. Modulation of size, shape, and composition (metal, oxide, or sulfide) of monometallic Sn catalysts is effective to achieve high formate formation activity, but these approaches cannot improve CO formation performance.<sup>[5a-d]</sup> Until now, cooperative promotion is required to enhance CO formation on Sn-based catalysts. For example, Cu-Sn bimetallic catalysts are reported to favor CO formation;<sup>[6]</sup> however, Cu also acts as possible catalytic sites. Herein we report a new strategy that leads to unprecedented activity and selectivity for CO formation among monometallic Sn catalysts. Key to this performance are the ultra-small size of catalyst nanoparticles and their dense packing in a conductive matrix, which lead to a high density of active site and a local pH effect that favors the formation of CO over formate.

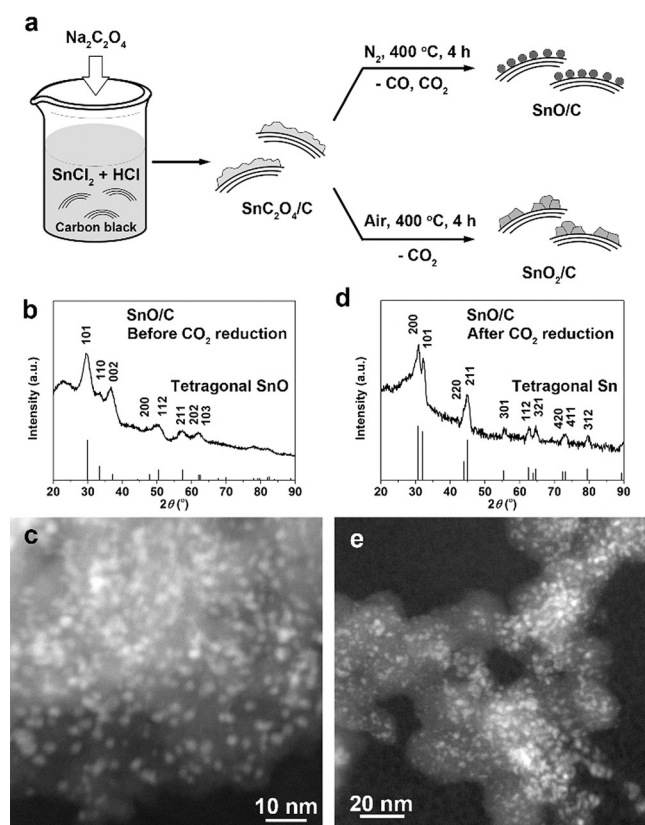
To prepare densely packed ultra-small Sn nanoparticles, we considered to derive them from a suitable tin oxide. Sn is a low melting-point metal, and thus many synthetic methods for nanoparticles that involve thermal treatments are more adapted for tin oxides than for Sn.<sup>[7]</sup> Moreover, previous work showed that oxide-derived metal catalysts can have higher roughness and surface areas, which is beneficial for CO<sub>2</sub> reduction.<sup>[8]</sup> We chose SnO because unlike SnO<sub>2</sub>, it has not been explored as precursors for catalysts for CO<sub>2</sub> electroreduction. Figure 1a shows the synthetic strategy of carbon-black-supported SnO (SnO/C) as the precatalyst. A composite of carbon black and Sn<sup>II</sup> oxalate (SnC<sub>2</sub>O<sub>4</sub>/C; Supporting Information, Figure S5) was first prepared by co-precipitation. Pyrolysis of SnC<sub>2</sub>O<sub>4</sub>/C at 400 °C in an N<sub>2</sub> atmosphere then yielded SnO/C. For comparison purpose, precatalysts based on SnO<sub>2</sub> (SnO<sub>2</sub>/C) and Sn nanoparticles (Sn/C) were also fabricated. SnO<sub>2</sub>/C was prepared similarly to SnO/C, except that the pyrolysis was conducted in air (Figure 1a). Sn/C was prepared by reducing SnCl<sub>2</sub> with NaBH<sub>4</sub> in the presence of carbon black.

The X-ray diffraction (XRD) patterns confirm the crystallographic phase of SnO/C (Figure 1b), SnO<sub>2</sub>/C and Sn/C (Supporting Information, Figure S6), and the broad diffraction peaks of SnO/C and SnO<sub>2</sub>/C indicate the nanosized features of SnO and SnO<sub>2</sub>. The loadings of SnO, SnO<sub>2</sub>, and Sn in the composites determined by thermal gravity analysis (TGA) in air were 46.0%, 49.2%, and 49.3%, respectively (Supporting Information, Figure S7). X-ray photoelectron spectroscopy (XPS) analyses (Supporting Information, Figure S8 and Table S2) show that the surfaces of Sn and SnO were partially oxidized to form SnO<sub>2</sub> species when exposed to

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**Figure 1.** a) Synthetic strategies of SnO/C and SnO<sub>2</sub>/C. b), d) XRD patterns and c), e) HAADF-STEM images of SnO/C before (b, c) and after (d, e) electrolysis at  $-0.66$  V vs. RHE in CO<sub>2</sub> saturated 0.5 M KHCO<sub>3</sub> electrolyte for 1800 s. Vertical lines in (b) and (d) are standard diffraction patterns of tetragonal SnO (JCPDS no. 06-0395) and tetragonal Sn (JCPDS no. 04-0673), respectively.

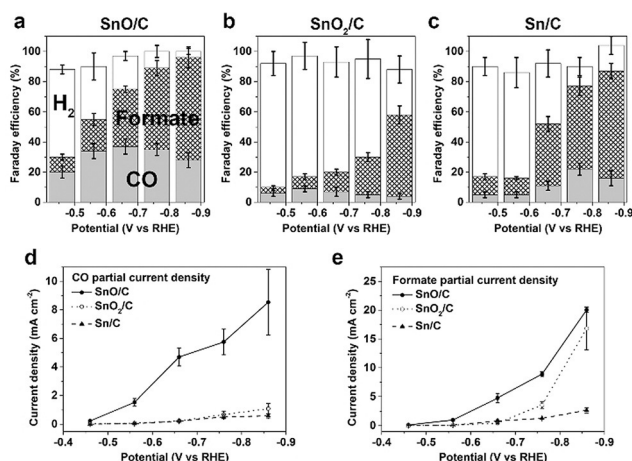
air. The high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) images of SnO/C are shown in the Figure 1c and the Supporting Information, Figure S9a. These images reveal ultra-small SnO nanoparticles as bright dots with an average size of  $2.6 \pm 0.4$  nm, homogeneously dispersed on the carbon black substrate, which appears as a gray background. The interparticle distance is about 4 nm. High-resolution transmission electron microscopy (HRTEM) image reveals the single-crystalline nature of SnO nanoparticles (Supporting Information, Figure S9b). On the other hand, SnO<sub>2</sub> nanoparticles in SnO<sub>2</sub>/C (Supporting Information, Figure S10) have an average size of  $5.0 \pm 0.9$  nm, twice as large as SnO, and aggregation occurs to some degree. Sn particles in Sn/C have a wide size distribution of 30 to 200 nm (Supporting Information, Figure S11).

The post-catalytic characterizations of SnO/C after electrolysis at  $-0.66$  V versus reversible hydrogen electrode (RHE) in CO<sub>2</sub> saturated 0.5 M KHCO<sub>3</sub> electrolyte for 1800 s are shown in Figure 1d,e. The applied potential is much more negative than the reduction potential of SnO and SnO<sub>2</sub>, that is  $-0.10$  V and  $-0.09$  V vs. RHE, respectively.<sup>[9]</sup> The XRD pattern of SnO/C after electrolysis indeed only shows the peaks of metallic Sn. However, peaks of SnO<sub>2</sub> still exist with those of metallic Sn in the XRD pattern of SnO<sub>2</sub>/C after

electrolysis (Supporting Information, Figure S13a), indicating incomplete reduction, which is probably due to the larger size and aggregation. After electrolysis, Sn nanoparticles derived from SnO maintained a similar size ( $3.0 \pm 0.9$  nm), high dispersity, and single-crystalline nature as their SnO precursors (Figure 1e; Supporting Information, Figure S12). Although ultra-small Sn nanoparticles should be easily oxidized when exposed to air, the Nafion binder in the catalyst seems to prevent this oxidation. In contrast, SnO<sub>2</sub>-derived nanoparticles after electrolysis have a much larger size ( $8.3 \pm 1.8$  nm), polycrystalline nature, and suffer from aggregation (Supporting Information, Figure S13b,c).

The catalytic activity and selectivity of SnO/C, SnO<sub>2</sub>/C, and Sn/C in CO<sub>2</sub> electroreduction were tested in CO<sub>2</sub> saturated 0.5 M KHCO<sub>3</sub> electrolyte. H<sub>2</sub>, CO, and formate were the only products detected by gas chromatography and <sup>1</sup>H NMR spectroscopy. SnO/C showed the highest current density in both linear sweep voltammetry (LSV) curves (Supporting Information, Figure S14) and chronoamperometry (CA) curves (Supporting Information, Figure S15). An induction period was observed for every pre-catalyst in the CA curves, which is most likely attributed to the reduction of tin oxides to Sn. SnO/C showed good stability in a 1-day CA test at  $-0.66$  V vs. RHE (Supporting Information, Figure S16), with a stable current density about  $13 \text{ mA cm}^{-2}$  and the Faraday efficiency of CO constantly between 30% and 40%. The Faraday efficiency of formate of the one-day electrolysis was 36%.

The potential-dependent Faraday efficiency (Figure 2a–c) and partial current density (Figure 2d–e) for CO and formate formation of the SnO/C, SnO<sub>2</sub>/C and Sn/C pre-catalysts were then determined. SnO/C shows the highest Faraday efficiency to CO<sub>2</sub> reduction, and more importantly, to CO formation at all applied potentials, which keeps above 20% and has the maximum of 37% at  $-0.66$  V vs. RHE. The partial current density for CO formation of SnO/C is about an order of magnitude higher than that of SnO<sub>2</sub>/C and Sn/C. At  $-0.66$  V



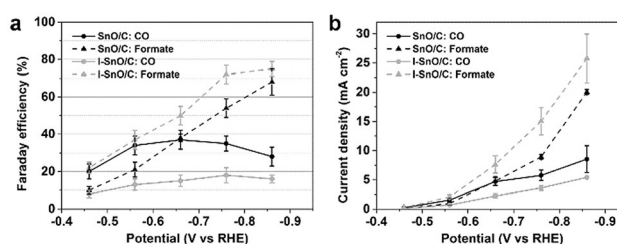
**Figure 2.** a)–c) Faraday efficiencies of CO (gray), formate (hashed), and H<sub>2</sub> (white) of a) SnO/C, b) SnO<sub>2</sub>/C, and c) Sn/C at different applied potentials. d), e) Partial current densities of d) CO and e) formate of SnO/C (solid), SnO<sub>2</sub>/C (dotted), and Sn/C (dashed) at different applied potentials.

and  $-0.86$  V vs. RHE, the current density was  $4.7$  and  $8.5$   $\text{mA cm}^{-2}$ , respectively. The partial current density for formate formation of SnO/C is higher than SnO<sub>2</sub>/C and Sn/C as well. As shown in the Supporting Information, Figure S4, the Faraday efficiency and partial current density of CO formation of SnO/C were substantially higher than those of other Sn based catalysts in previous reports.<sup>[5]</sup> The partial current density of formate formation of SnO/C is also among the highest in Sn-based catalysts.<sup>[5]</sup>

Since post-catalytic characterization data indicate that SnO and SnO<sub>2</sub> precursors were transformed into metallic Sn during electrolysis, the superior activity and selectivity of SnO/C warrants additional analysis. Compared to SnO<sub>2</sub>/C and Sn/C, the Sn nanoparticles derived from SnO/C has a significantly smaller size. As a result, SnO/C possessed a higher surface area, as indicated by the measurements of double-layer capacitances (Supporting Information, Figure S17) and Brunauer–Emmett–Teller (BET) analysis (Supporting Information, Figure S18 and Table S3). However, the less than two-fold increase in surface area cannot account for the more than 10 times higher partial current densities of CO formation on SnO/C.

Nanoparticles with smaller size expose a higher proportion of step and corner sites, which might bind adsorbates stronger than terrace sites. As indicated by the anodic LSV curves in N<sub>2</sub> saturated 0.1M KOH electrolyte (Supporting Information, Figure S19), the potential for oxidative adsorption of OH<sup>-</sup> on SnO/C was more negative than that of the other two samples, revealing a stronger binding to OH group. OH has been considered as a surrogate of CO<sub>2</sub><sup>-</sup>, while the adsorption energy of CO<sub>2</sub><sup>-</sup> is a descriptor of the activity of CO<sub>2</sub> reduction.<sup>[5a-c,10]</sup> This result implies Sn nanoparticles derived from SnO/C adsorb CO<sub>2</sub><sup>-</sup> stronger than those derived from SnO<sub>2</sub>/C and Sn/C. The better stabilization of CO<sub>2</sub><sup>-</sup> intermediate, probably attributed to the ultra-small particle size, is likely the origin of the higher activity of SnO/C.

However, the size effect cannot explain the high selectivity of SnO/C towards CO formation. In our SnO/C sample, nanoparticles of the SnO pre-catalyst, and the actual Sn catalyst, are densely distributed in the carbon matrix. We hypothesized that this dense distribution might affect microscopic diffusion, and thus, influence the CO<sub>2</sub> reduction selectivity.<sup>[11]</sup> To probe the effect of SnO density, we synthesized another sample of carbon black supported SnO nanoparticles with a lower weight fraction (8.4%) of SnO (denoted as l-SnO/C). The average size of SnO nanoparticles was  $3.0 \pm 0.8$  nm (Supporting Information, Figure S20), similar to that of SnO/C. As indicated by the averaged nanoparticle-centered radial distribution diagrams of particle density (Supporting Information, Figure S3), the particle density within a short radius of one SnO nanoparticle of SnO/C is significantly higher than that of l-SnO/C. Figure 3a and 3b compare the Faraday efficiencies and partial current densities of CO and formate formation on SnO/C and l-SnO/C, at a similar loading of SnO. Compared to SnO/C, l-SnO/C has a much lower selectivity towards CO formation while favoring formate formation. As the particle sizes of SnO/C and l-SnO/C were similar, the particle density in the carbon



**Figure 3.** a) Faraday efficiencies and b) partial current densities of CO (solid curves) and formate (dashed curves) of SnO/C (black) and l-SnO/C (gray) at different applied potentials.

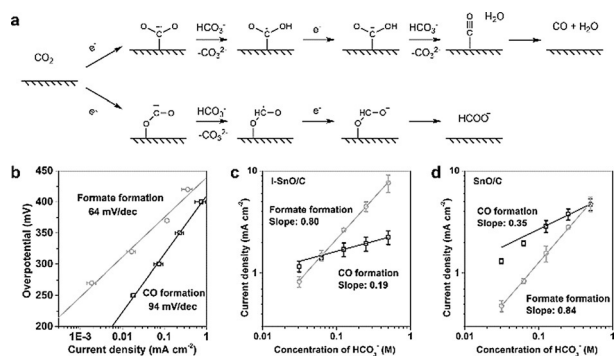
black matrix seems to be the main factor affecting the selectivity.

It has been observed in previous work<sup>[5b,c]</sup> that on tin-based catalysts, by applying larger bias, an increase of current density was accompanied by an increase of the Faraday efficiency of CO. High current density, namely higher consuming rate of proton source, leads to a significant raise in local pH value near the catalytic sites, which might be the origin of the increased CO selectivity. In 0.5M KHCO<sub>3</sub> electrolyte, the proton donor was HCO<sub>3</sub><sup>-</sup> ( $pK_a = 10.3$ ).<sup>[9]</sup> The simulation<sup>[12]</sup> showed that in the electrolyte containing 0.5M KHCO<sub>3</sub>, the local pH value at a flat electrode is about 2 pH units higher than that in bulk electrolyte when the current density is  $5$   $\text{mA cm}^{-2}$ , and this difference increase significantly as the current density increases. We consider that in the catalyst composed of more densely packed nanoparticles, in this case, the SnO/C sample, the local current density around one nanoparticle at a given overpotential is higher, and the local pH value should be higher. If the formation rates of CO and formate show different dependence on the concentration of proton donor, this local pH effect will lead to the variation of the selectivity between CO and formate.

The local pH effect is expected to be more pronounced in electrolytes with weaker buffer capacities.<sup>[8c,13]</sup> The product distribution of CO<sub>2</sub> reduction on SnO/C in three different electrolytes (0.5M K<sub>2</sub>HPO<sub>4</sub>, 0.5M KHCO<sub>3</sub>, and 0.5M KCl) is compared in the Supporting Information, Figure S21. As the buffer capacity of electrolyte decreases from K<sub>2</sub>HPO<sub>4</sub> to KHCO<sub>3</sub> to KCl, the Faraday efficiency of CO increases gradually. This result supports that a higher local pH effect enhances CO selectivity.

The possible pathways of CO and formate formation on Sn are shown in Figure 4a.<sup>[3,6b]</sup> For each pathway, if the first step, the single electron transfer to CO<sub>2</sub>, is the rate determining step (RDS), the Tafel slope should be  $118$   $\text{mV dec}^{-1}$ . If this step is reversible, followed by a rate-limiting proton transfer from HCO<sub>3</sub><sup>-</sup>, the Tafel slope should be  $59$   $\text{mV dec}^{-1}$ .<sup>[14,15]</sup> As indicated by the Tafel plots of SnO/C (Figure 4b), the Tafel slopes of formate formation is  $64$   $\text{mV dec}^{-1}$ , close to  $59$   $\text{mV dec}^{-1}$ , similar to that reported for other Sn-based catalysts,<sup>[4,5a,b]</sup> suggesting that the RDS is the protonation of the adsorbed CO<sub>2</sub><sup>-</sup>. Meanwhile, the Tafel slope of CO formation is  $94$   $\text{mV dec}^{-1}$ , close to  $118$   $\text{mV dec}^{-1}$ , suggesting that the formation rate of CO is more limited by the first single electron transfer step. The Tafel analysis suggests that





**Figure 4.** a) Proposed reaction pathways of CO and formate formation on Sn. b) Tafel plots of CO (black) and formate (gray) formation on SnO/C. c,d) Partial current densities of CO (black) and formate (gray) depending on the concentration of HCO<sub>3</sub><sup>-</sup> for l-SnO/C (c) and SnO/C (d) at -0.66 V vs. RHE.

the change of local pH will largely change the rate of formate formation, but not CO formation.

To provide further support to the above Tafel analysis, the apparent reaction orders of HCO<sub>3</sub><sup>-</sup> in CO and formate formation for l-SnO/C and SnO/C were measured (Figure 4c,d). The reaction order of HCO<sub>3</sub><sup>-</sup> in formate formation was about 0.8, which is close to first order. This result agrees with the previous report on nanosized SnO<sub>2</sub>/C<sup>[5a]</sup> and supports that the protonation of adsorbed CO<sub>2</sub><sup>-</sup> is the RDS for formate formation. The rate orders of HCO<sub>3</sub><sup>-</sup> for CO formation was much smaller, being 0.19 for l-SnO/C and 0.35 for SnO/C. This result agrees with previous studies on Au<sup>[15]</sup> and Ag<sup>[8c]</sup> where the rate order of HCO<sub>3</sub><sup>-</sup> for CO formation was close to zero. It is consistent with the reduction of CO<sub>2</sub> to CO<sub>2</sub><sup>-</sup> being the RDS for CO formation. Based on the reaction orders, a 10-fold increase of the concentration of HCO<sub>3</sub><sup>-</sup> will lead to a 4-fold increase in the selectivity of CO over formate. These results indicate that formate formation is greatly disfavored over CO formation when the concentration of proton source is decreased, consistent with the local pH effect proposed above.

Because CO formation also involves protonation (Figure 4a), when the concentration of HCO<sub>3</sub><sup>-</sup> is low enough, the protonation step will be slowed down sufficiently to have a comparable rate to the reduction of CO<sub>2</sub> to CO<sub>2</sub><sup>-</sup>. This analysis gives a possible explanation for the non-zero order of HCO<sub>3</sub><sup>-</sup> in CO formation. The higher order of our optimized catalyst, SnO/C than l-SnO/C (which has a lower packing density than SnO/C) suggests that the local concentration of HCO<sub>3</sub><sup>-</sup> around SnO/C is lower than around l-SnO/C, again consistent with a higher local pH effect for the more densely packed particles.

In summary, a simple synthetic method has been developed for ultra-small (2.6 nm) SnO nanoparticles densely dispersed in carbon black. These SnO nanoparticles are completely reduced to Sn nanoparticles of similar size and dispersion under conditions employed for CO<sub>2</sub> electroreduction. Compared to other Sn-based catalysts, the SnO/C derived catalyst exhibits remarkably high selectivity and partial current density of CO formation, as well as one of the highest partial current densities of formate formation. The

high activity originates from its ultra-small particle size, which enhances CO<sub>2</sub><sup>-</sup> absorption, and the high selectivity for CO formation is attributed to a local pH effect arising from the high density of nanoparticles in the conductive carbon black matrix. Local pH increase suppresses formate formation while shows less influence on the formation rate of CO. The tuning of the distribution of nanocatalysts in a conductive matrix might be further exploited as a design strategy for the development of selective CO<sub>2</sub> reduction electrocatalysts.

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## Conflict of interest

The authors declare no conflict of interest.

**Keywords:** carbon dioxide reduction · electrocatalysis · nanoparticles · particle density · tin oxide

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