## Micro-solid oxide fuel cells running on reformed hydrocarbon fuels

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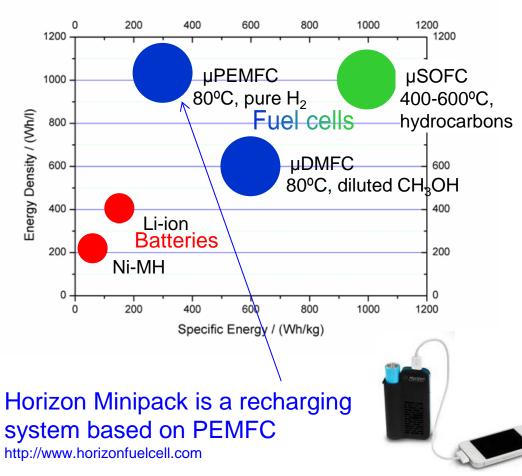
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### Sources for mobile energy



Advantages of micro-SOFC:

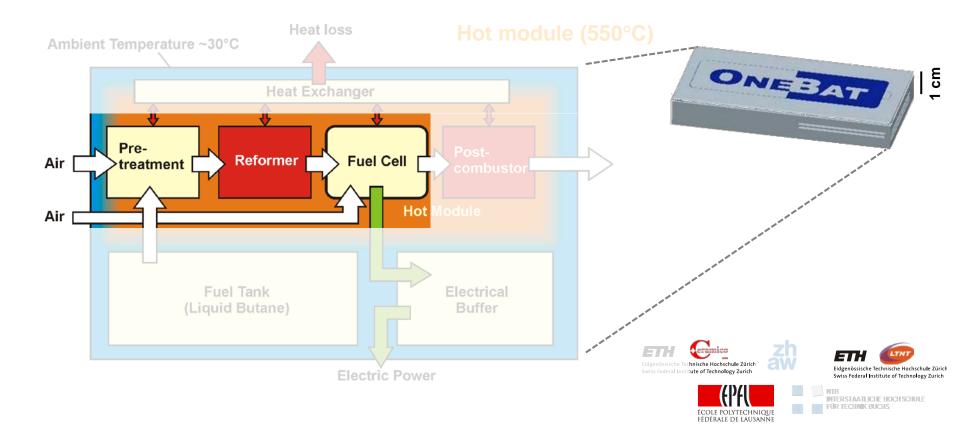
- high efficiency
- high energy density
- fuel flexibility
- geographically independent

Challenges of micro-SOFC:

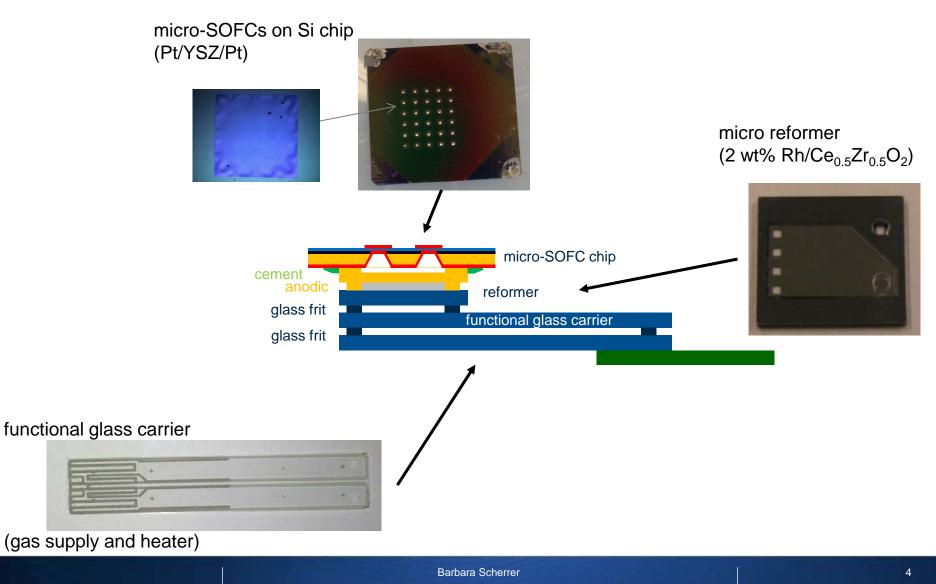
high temperature

Adapted from: Manhattan Scientifics & L. Livermore National Laboratories and Sulzer Hexis, 2002.

### **Micro-fuel cell systems for battery replacement**

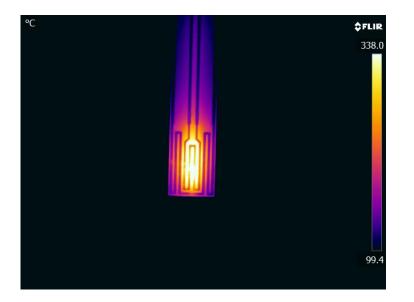


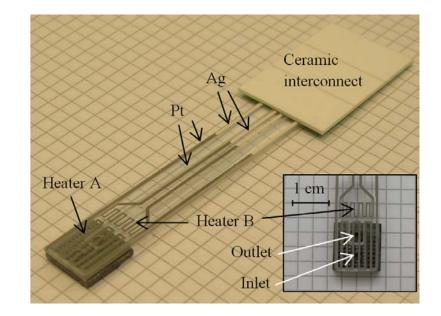




### **Functional glass carrier**

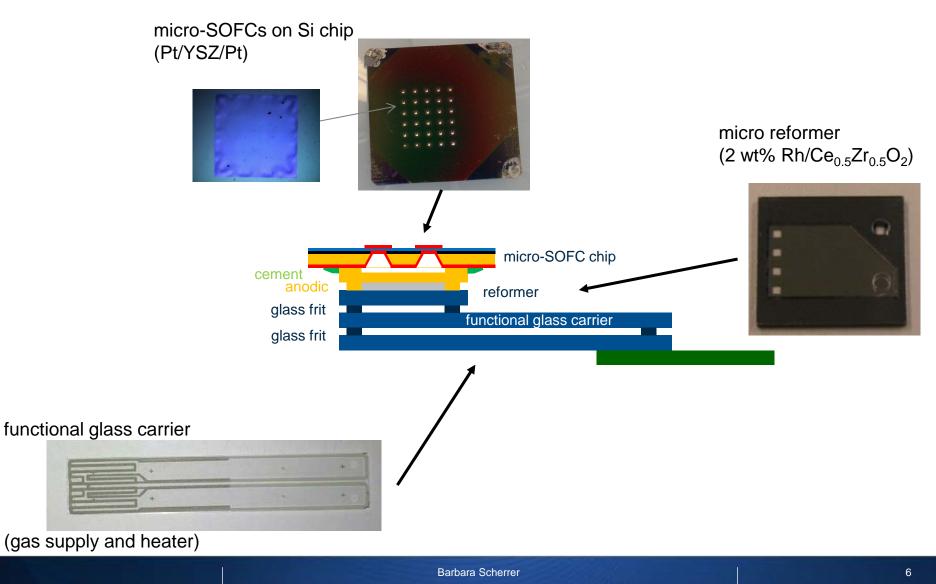
- Fabrication of carrier:
  - Schott AF 32®
    - T<sub>G</sub> = 717 <sup>0</sup>C
  - Glass frit bonding
    - H = 100 µm





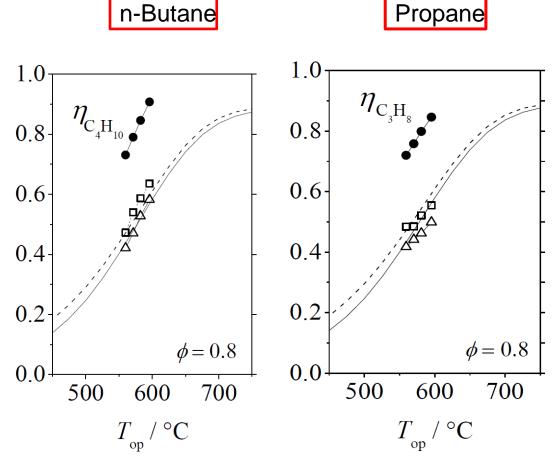
- Fabrication of heaters:
  - Pt and Ag heaters
  - Screen printed heaters
    - Height < 50 µm</p>
  - Heater A: bottom of MR
  - Heater B: before MR inlet





### **Micro reactor**

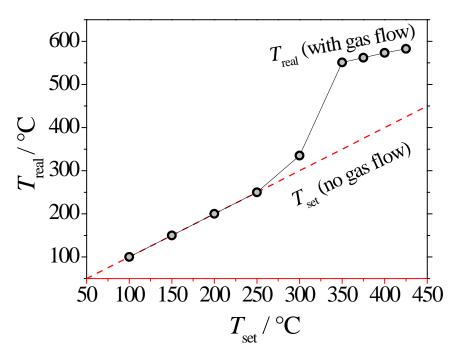
- Conversion of C<sub>4</sub>H<sub>10</sub> is higher
- H<sub>2</sub> production from C<sub>4</sub>H<sub>10</sub> is higher
- <u>n-Butane</u>: C/O = 0.7 and C/O = 0.8 are best dilutions
- <u>Propane</u>: C/O = 0.8 is best dilution



			C <sub>x</sub> H <sub>y</sub> -species		Syngas-species		
	$\phi$		$\eta$	$x_{\rm CH_4}$	$\psi_{ extsf{H}_2}$	$\psi_{ m co}$	$\psi_{ m syngas}$
n-Butane	0.7	Average $\pm \sigma$ [%]	95.2 ±0.1	0.18 ±0.0	66.7 ±0.4	51.7 ±0.5	60.1 ±0.5
		Outlet flow rate [µmol/s]	0.06 ±0.01	0.24 ±0.01	4.43 ±0.14	2.74 ±0.11	7.17 ±0.13
Propane	0.8	Average $\pm \sigma$ [%]	84.3 ±0.4	$0.16 \pm 0.0$	$55.4 \pm 0.1$	$42.5 \pm 0.1$	49.8 ±0.1
		Outlet flow rate [µmol/s]	0.31 ±0.01	0.32 ±0.01	4.33 ±0.01	2.50 ±0.01	6.83 ±0.01

### **Micro reactor**

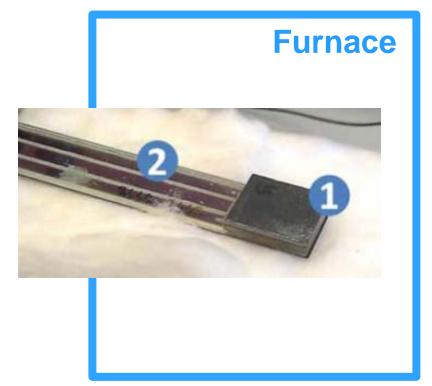
- Temperature increase behavior during testing
  - Reaction starts > 300 °C
- Higher flow rate results in higher temperature.

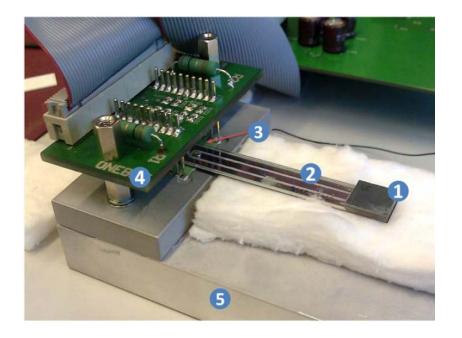


### **Characterization of micro reformer**

... in the furnace





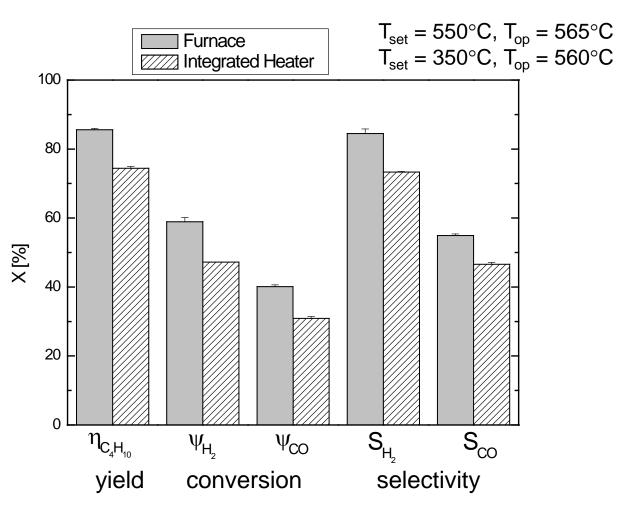


### **Results of gas analysis**

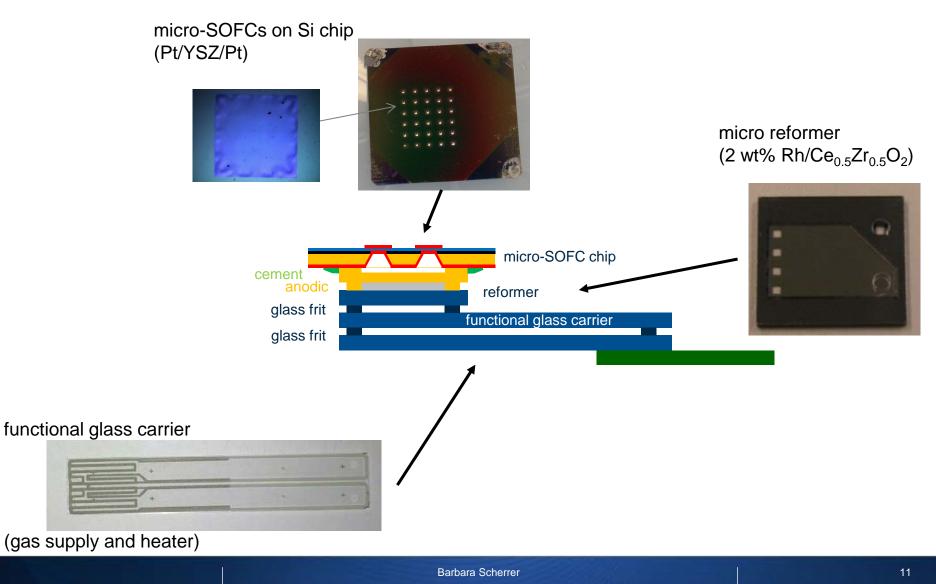
 Less even temperature distribution results in lower yield, conversion and selectivity for the integrated heater setup.

 Better insulation will improve it again.

Literature







### **Micro-SOFC** fabrication

Si Wafer (380  $\mu$ m), LPCVD-Si<sub>3</sub>N<sub>4</sub> (200 nm) on both sides

Window opening (900  $\mu$ m): photolitho + RIE of Si<sub>3</sub>N<sub>4</sub>

Si wet etching: KOH 20%, 90 °C

YSZ deposition: AA-CVD, PLD, spray pyrolysis

Release of the YSZ membrane by reactive ion etching

Top-side electrode deposition

Back-side electrode deposition



comp.

stress

Top-view light micrographs

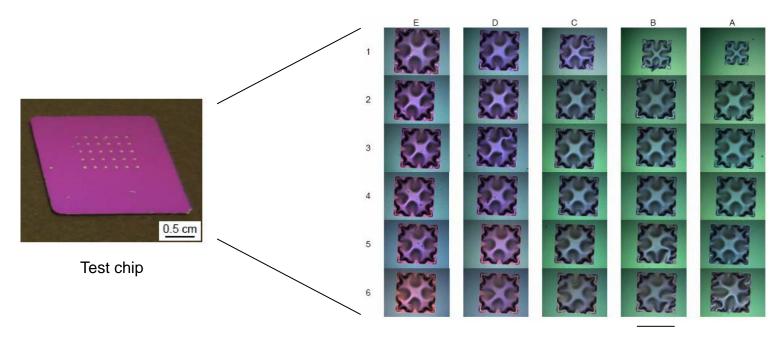
390 µm

tens.

stress

### **Micro-SOFC** fabrication



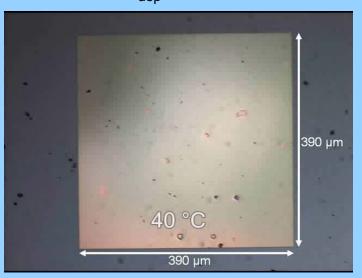


membrane side length: 390 µm

- Test chip: 30 free-standing micro-SOFC membranes
- Membrane yield (%): number of surviving membranes / 30 \* 100
- Membrane yield target: ~100 %

### **Thermomechanical stress**

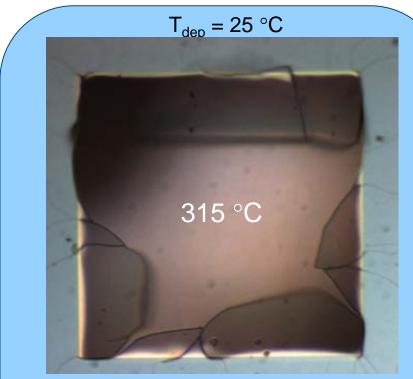
 $T_{dep} = 25 \ ^{\circ}C$ 



Partially crystalline as-deposited film (PLD) Yield after free-etching: ca. 100% Tensile stress (flat membrane)  $F_{dep} = 700 \text{ °C}$ 

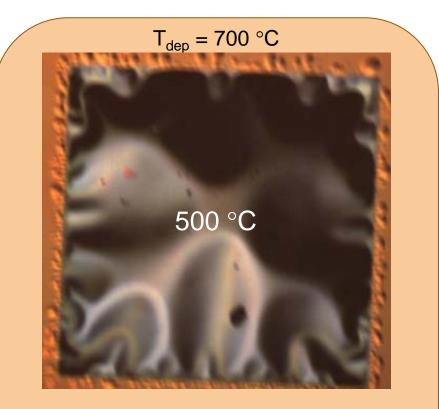
Fully crystalline as-deposited film (PLD)Yield after free-etching: ca. 100%Compressive stress (buckled membrane)

### **Thermomechanical stress**



Crystallization during heating >> tensile stress

Membrane rupture (low yield: < 10 %)



Buckling «apparently» unchanged during heating

Robust membrane (high yield: 100%)

A. Evans et al., Fuel Cells, 2012.

### Residual stress in free-standing YSZ membranes

 $\rm PLD \ T_{\rm depo}$ 

free-standing membrane (390x390 µm<sup>2</sup> 300nm 8YSZ)

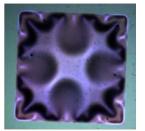
Yield: after deposition after annealing at 500 °C SAMLAB



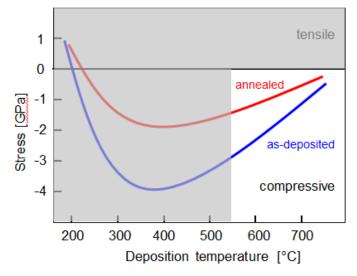
98% 0%



0% 0% -2.1 GPa 700°C



>99% >99% -1.4 GPa



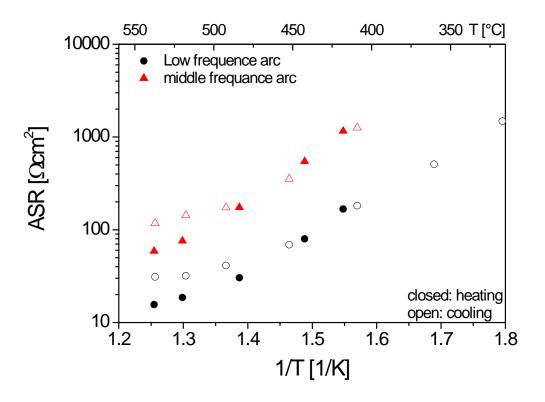
Adapted from: I. Garbayo et al., Solid State Ionics, 2012.

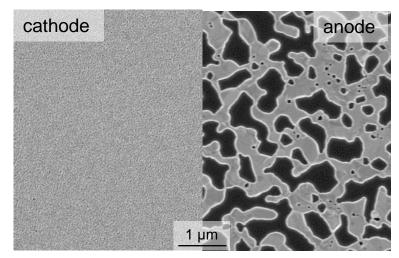
Different stresses *f*(T<sub>depo</sub>):

 Tensile and too much compressive stress result in membrane rupture.

A. Evans et al., Fuel Cells, 2012.

### **ASR of Pt in fuel cell conditions**



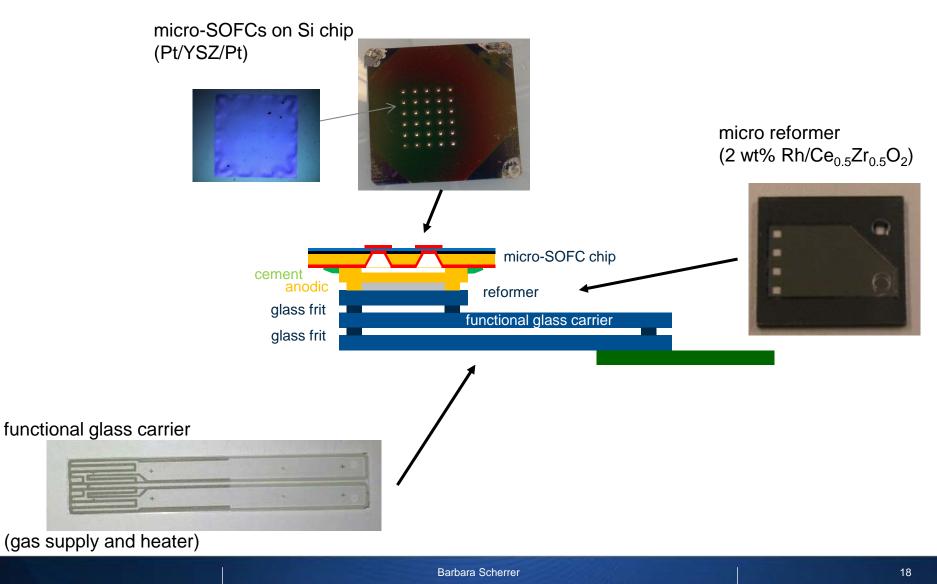


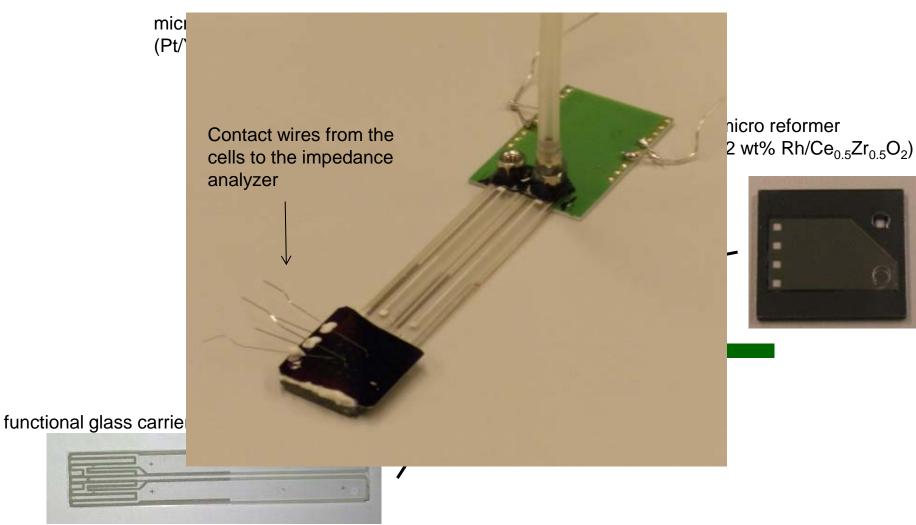
cathode: 300 sccm air anode: 60 sccm  $H_2$  in 240 sccm  $N_2$ 

Pt thin films tested on YSZ single crystal

- ASR of the electrodes are stable over heating and cooling
- Microstructure is different depending on the seen environment

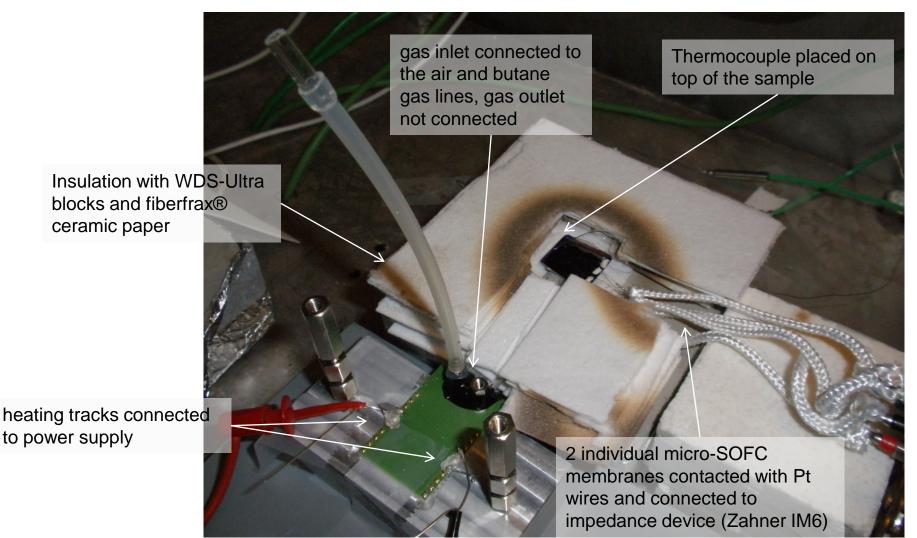


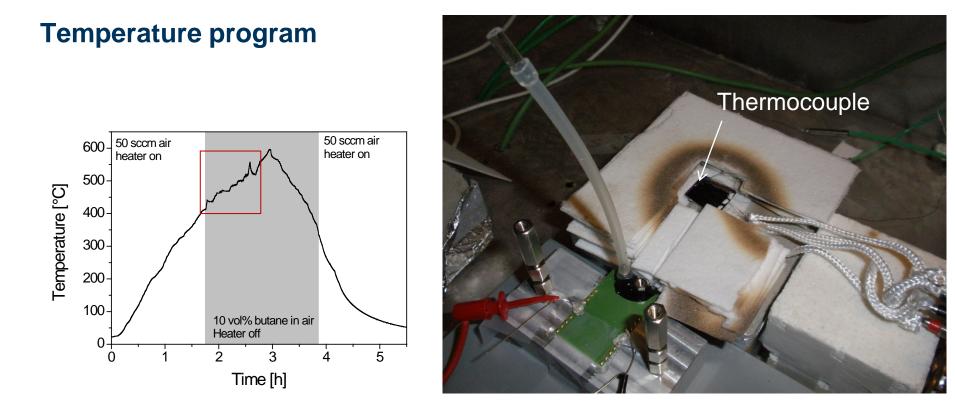




(gas supply and heater)

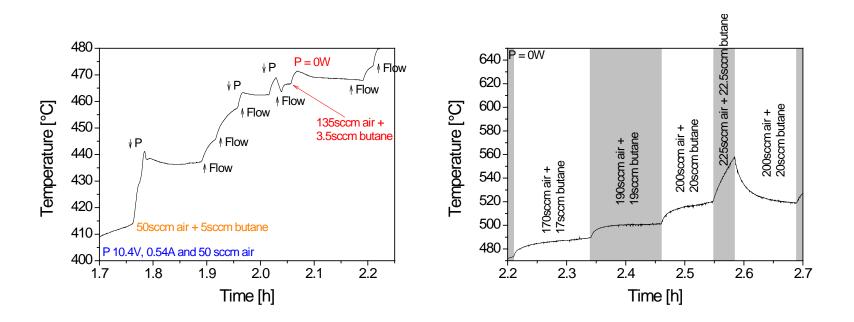






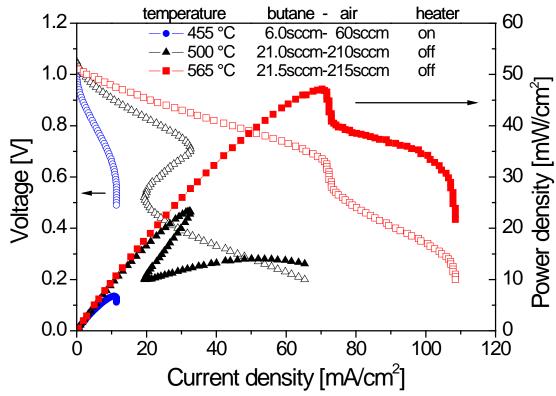
- Heating ramp done by increasing voltage
- Temperature measurement on the sample is accurate

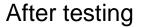
### **Temperature program**

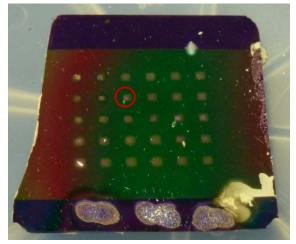


- Self sustained reaction of the reformer heats the assembly further
  - Increasing flow results in increasing temperature
- Almost stable temperature reached after 2 min

### Cell voltage and power density

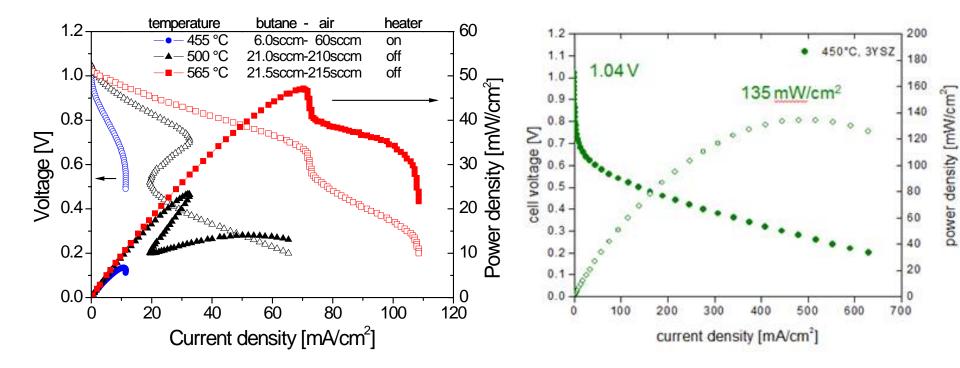






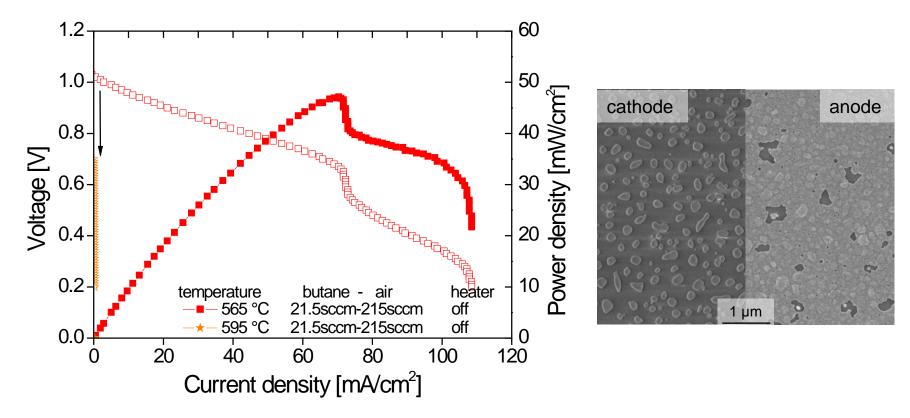
- Theoretical open circuit voltage was achieved!
  - Gas-tight membranes
- Maximum power density of about 50 mW/cm<sup>2</sup> at 565 °C!
- All membranes survived the testing program (maximal temperature of 596 °C)!

### Cell voltage and power density – comparison



Strange curve shape at ~0.7 V, most likely due to excess water at the gas outlet.

### Cell voltage and power density – decrease in OCV



- Long-term testing not possible due to instable Pt-electodes
  - Cathode agglomerates more severe most likely due to the surface roughness of the electrolyte layer
- Gas leak of ceramic paste results in lower OCV

### Summary

- Assembly of the glass carrier, reformer and micro-SOFC chip works.
- The heater was able to heat up the assembly till the self sustained reaction of the reformer sets in.
- Further heating was achieved by increasing the flow of butane and air.
- Theoretical OCV and a maximum power density of about 50 mW/cm<sup>2</sup> at 565 ° C was achieved.

### Outlook

- Excess of water results in unstable current-voltage curve.
- Integration of more stable (and active) electrode materials in order to achieve a better stability and higher power density
  - Metal alloys: Pt-Y-Al
  - Ceramics: LSC, LSMC
- Cement paste starts to leak at 550 ° C, which resulted in an unstable temperature due to complete combustion of the fuel.
- Current collection of the membranes should be improved
  - On the chip with connection path
  - To the out side with wire bonding





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# Thank you for your attention!



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