

An introduction to the basic principles for the analysis of calorimetric & spectroscopic data





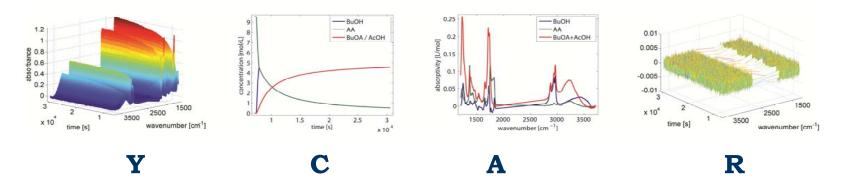




- **Spectroscopy**: Beer's law in elegant matrix notation, absorbance (**Y**) is proportional to the concentrations (**C**)
 - N_t N_{λ} N_c N_{λ} N_{λ}

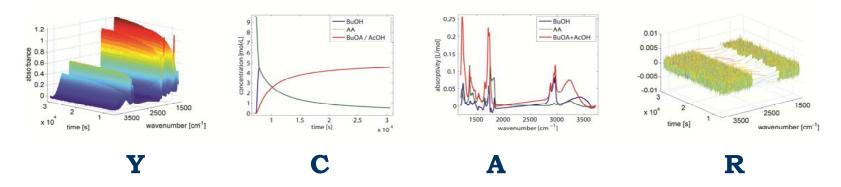


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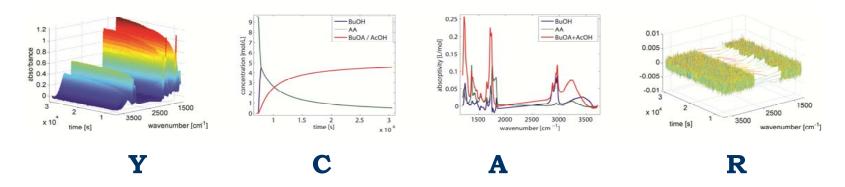


• Calorimetry: heat release (q) is proportional to the change in the reaction extent $(d\xi/dt)$

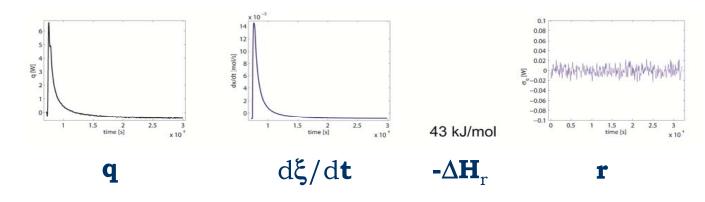
$$N_t$$
 = $\frac{N_r}{N_r}$ + $\frac{1}{N_r}$ q $d\xi/dt$ - ΔH_r r



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Soft Modelling (Part 1)

- Modelling experimental kinetic data based only on simple 'a priory' knowledge on the data structure and the results
 - Multivariate (multi wavelength spectroscopic) data and linear dependence of concentrations and data signal (Beer's law)
 - non-negativity of concentrations and species spectra
 - closure, unimodality, etc
- cannot be applied to calorimetry data (power signal is univariate)



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Hard Modelling (Part 2)

- Modelling experimental kinetic data based on a parameterised physicalchemical 'hard' model
- rate law defines the concentration profiles of the contributing species as a function of the rate constants
- applicable to both, calorimetry & spectroscopy (univariate & multivariate)



Part 1: Soft Modelling



Soft Modelling of Spectroscopic Kinetic Data

Topics

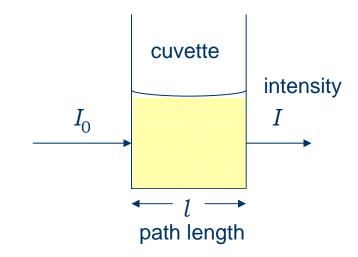
- Absorption spectroscopy
 - Beer's law in elegant matrix notation $(Y = C \times A)$
 - Non-unique factorisation of Y / rotational ambiguity
- Principal Component Analysis (PCA)
 - Abstract Factor analysis (AFA) by Singular Value Decomposition (SVD)
 - Chemical rank of the measurement matrix
 - The number of absorbing species
- Evolving Factor Analysis (EFA)
 - Evolutionary rank analysis by repeated SVD of sub matrices of Y
 - The 'Appearance' & 'Disappearance' of absorbing species
- Multivariate Curve Resolution by Alternating Least-Squares (MCR-ALS)
 - Model-free iterative decomposition of Y = C × A + R
 - Ideas, principles, limitations



Absorption Spectroscopy – Beer's Law

Absorbance y at wavelength λ :

$$y_{\lambda} = -\log\left(\frac{I}{I_0}\right)_{\lambda}$$



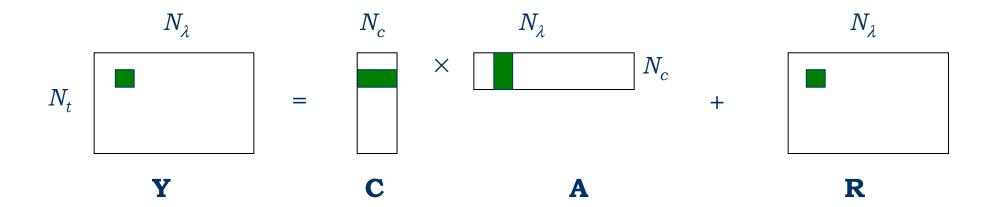
• Absorbance signal y_{λ} is linearly dependent on contributing species concentrations c_k , the corresponding coefficients are the molar absorptivities $a_{k,\lambda}$ that form the pure species spectra

$$y_{\lambda} = \sum_{k=1}^{N_c} c_k a_{k,\lambda} \times l$$

For simplicity: path length l=1



Beer's law in elegant matrix notation

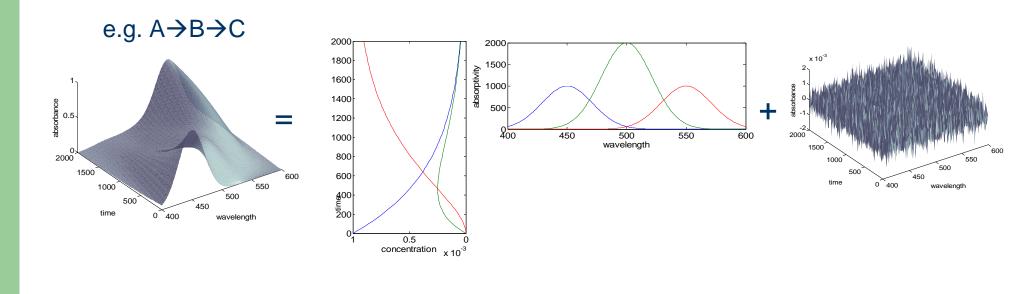


$$y_{t,\lambda} = \sum_{k=1}^{N_c} c_{t,k} a_{k,\lambda} + r_{t,\lambda}$$



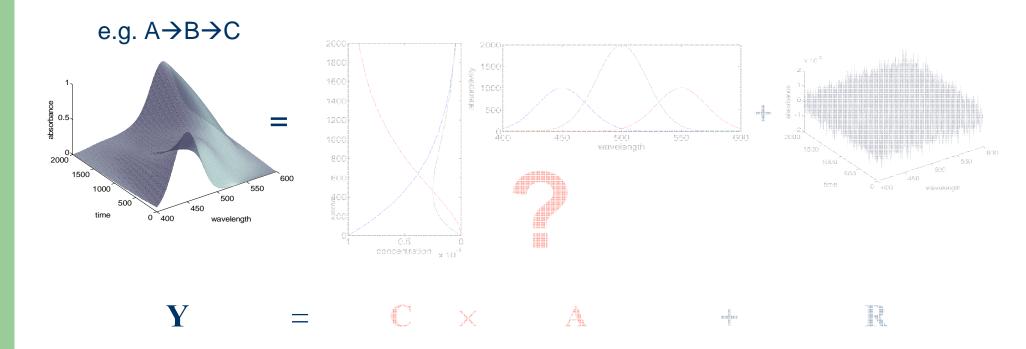
R

Rotational Ambiguity





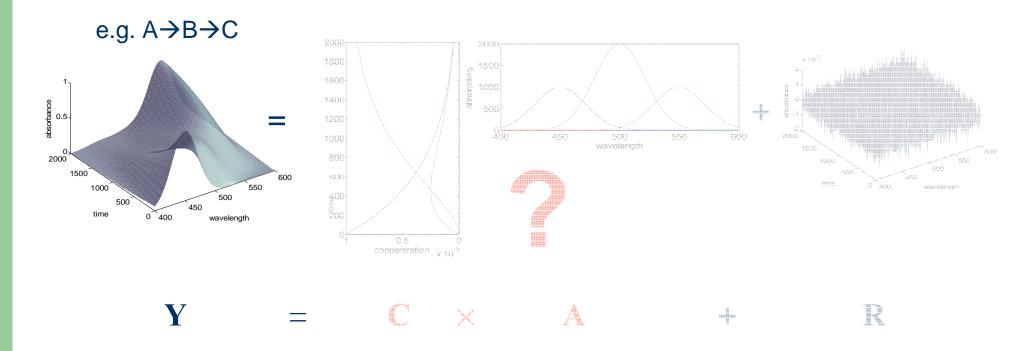
Rotational Ambiguity



Goal: Find concentration profiles **C** and species spectra **A** such that the residuals **R=Y-CA** become small only using a 'soft model', i.e. by linear factorisation



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Goal: Find concentration profiles **C** and species spectra **A** such that the residuals **R=Y-CA** become small only using a 'soft model', i.e. by linear factorisation

Problem: Factorisation is not unique (rotational ambiguity)



Major Soft-Modelling Classes

 By using appropriate 'soft' restrictions on C and A, e.g. non-negativity, windows of existence, closure, unimodality, known spectra, the number of possible solutions can be reduced, sometimes can even lead to a unique solution for C & A



Major Soft-Modelling Classes

- By using appropriate 'soft' restrictions on C and A, e.g. non-negativity, windows of existence, closure, unimodality, known spectra, the number of possible solutions can be reduced, sometimes can even lead to a unique solution for C & A
- There are 2 major classes

Factor Analysis (AFA) based

$$\mathbf{Y} = \overline{\mathbf{U}}\overline{\mathbf{S}}\overline{\mathbf{V}} = \overline{\mathbf{U}}\mathbf{T}\mathbf{T}^{-1}\overline{\mathbf{S}}\overline{\mathbf{V}} = \mathbf{C}\mathbf{A}$$

Find \mathbf{T} such that

$$\mathbf{C} = \overline{\mathbf{U}}\mathbf{T}$$
, and $\mathbf{A} = \mathbf{T}^{-1}\overline{\mathbf{S}}\overline{\mathbf{V}}$

Alternating Least Squares (ALS) based Start from some guessed **C**, then recalculate **A** and **C** until satisfied:

$$\mathbf{A} = (\mathbf{C}^{t}\mathbf{C})^{-1}\mathbf{C}^{t}\mathbf{Y} = \mathbf{C}^{+}\mathbf{Y}$$
$$\mathbf{C} = \mathbf{Y}\mathbf{A}^{t}(\mathbf{A}\mathbf{A}^{t})^{-1} = \mathbf{Y}\mathbf{A}^{+}$$







 One very well defined solution is the one received from Abstract Factor Analysis (AFA) using Singular Value Decomposition (SVD)

$$N_{\lambda}$$
 N_{λ} N_{λ}



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in Matlab:

$$[U,S,Vt] = svd(Y,0);$$



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Some properties of U, S and V

$$\mathbf{YY}^t\mathbf{U} = \mathbf{U}\mathbf{\Lambda}$$
 $\mathbf{Y}^t\mathbf{YV}^t = \mathbf{V}^t\mathbf{\Lambda}$
 $\mathbf{\Lambda} = \mathbf{S}^2$
 $\mathbf{U}^t\mathbf{U} = \mathbf{VV}^t = \mathbf{I}$
columns of \mathbf{U} (rows of \mathbf{V}) are eigenvectors of \mathbf{YY}^t ($\mathbf{Y}^t\mathbf{Y}$)
$$\mathbf{S} \text{ is a diagonal matrix with the square root of their eigenvalues}$$

$$\mathbf{U} \text{ and } \mathbf{V}^t \text{ are orthonormal}$$

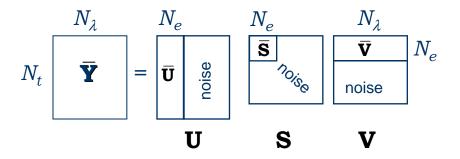




 Eigenvectors in U (columns) and V (rows) are arranged in decreasing order of magnitude of their corresponding singular values in S

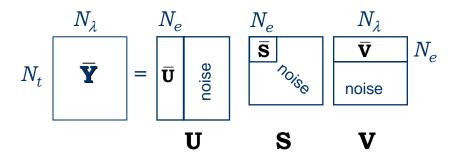


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- The diagonal elements of \bar{S} , the singular values, can be seen as normalisation coefficients for \bar{U} or \bar{V}



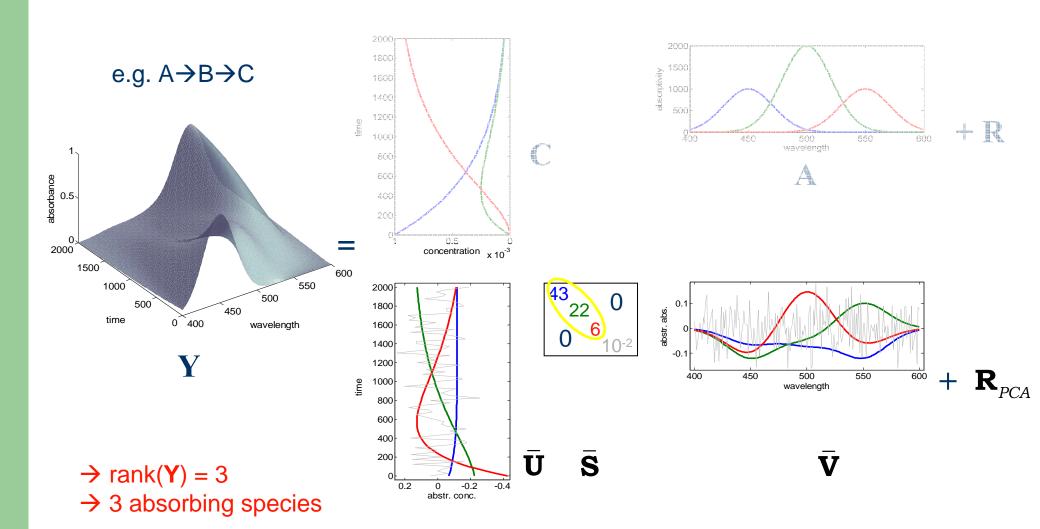


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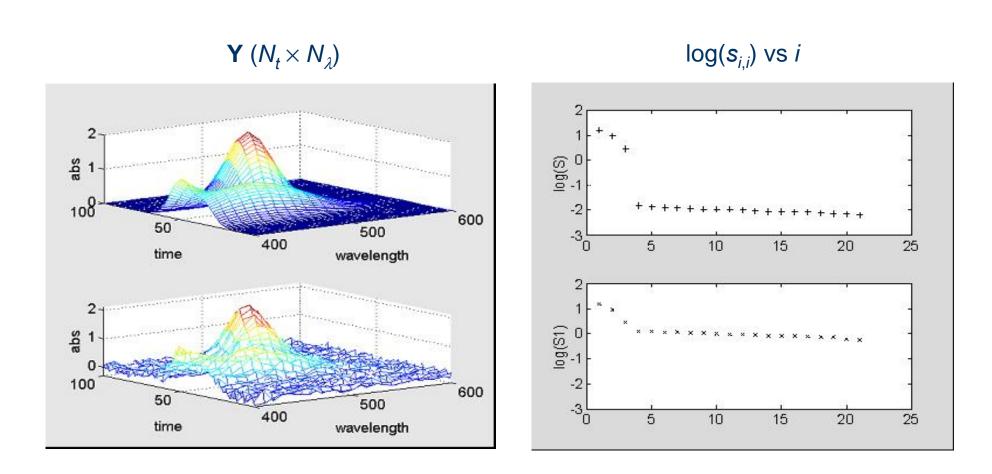
$$N_{t} \begin{bmatrix} N_{\lambda} & N_{e} & N_{e} & N_{\lambda} & N_{e} & N_{\lambda} & N_{e} & N_{\lambda} & N_{c} & N_{\lambda} & N_{\lambda$$

• The number of significant singular(eigen) values and –vectors is the chemical rank of **Y** and a 1st estimate on the number of absorbing species



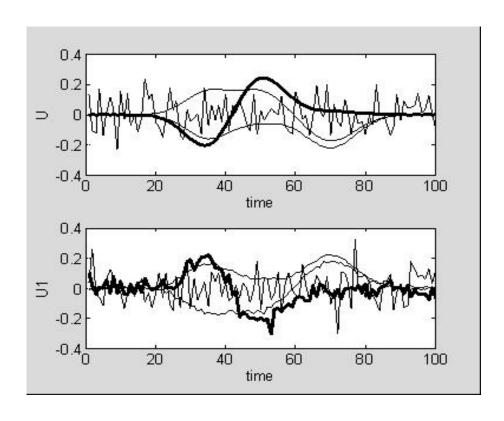






The noise level in the data matrix **Y** determines the drop in the magnitude from significant to insignificant singular values





The noise level in the data matrix **Y** also determines the remaining noise in the significant singular vectors

The signs of the singular vectors can interchange between **U** and **V**)

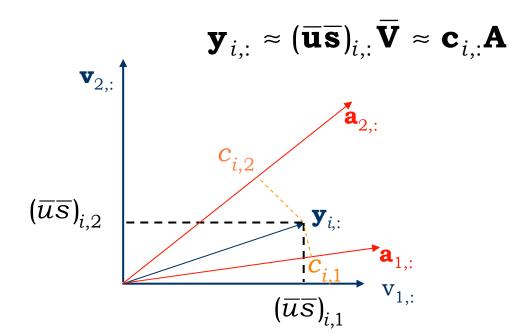




- e.g. 2 species, A→ B
- the (significant) eigenvectors v_{1,:} and v_{2,:} form an orthonormal base in the same 'plane' as the pure species spectra a_{1,:} and a_{2,:}

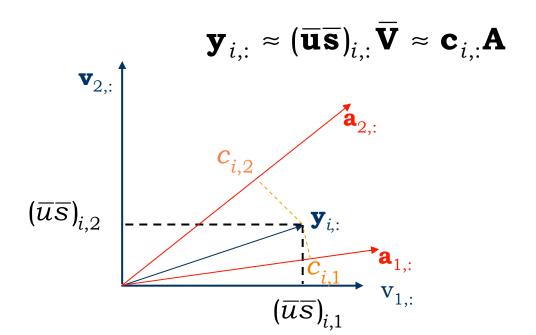


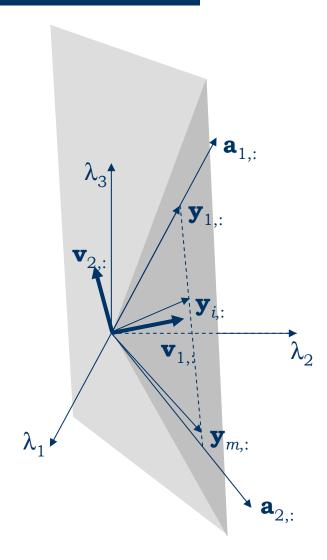
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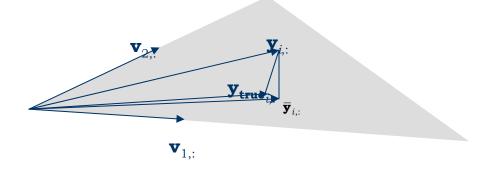


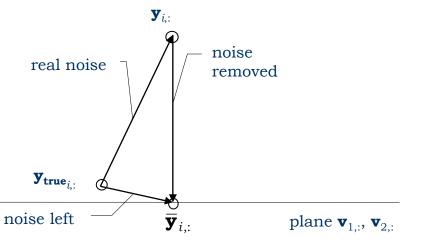
Some noise reduction



Some noise reduction

$$\mathbf{Y} = \overline{\mathbf{Y}} + \mathbf{R}_{PCA} = \sum_{i=1}^{N_e} \mathbf{u}_{:,i} \mathbf{s}_{i,i} \mathbf{v}_{i,:} + \sum_{j=N_e+1}^{N_{\lambda}} \mathbf{u}_{:,j} \mathbf{s}_{j,j} \mathbf{v}_{j,:} = \sum_{k=1}^{N_c} \mathbf{c}_{:,k} \mathbf{a}_{k,:} + \mathbf{R}_{noise}$$

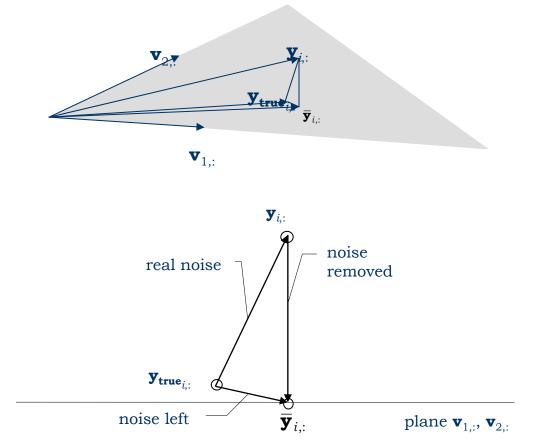


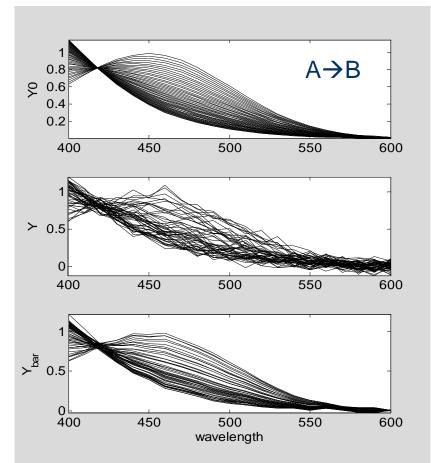




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- linear dependencies in C due to the kinetic model are common and sometimes difficult to predict (e.g. A+B→C)
- linear dependencies in A are less common





 sequential rank analysis of the data matrix along its time domain by repeated SVD



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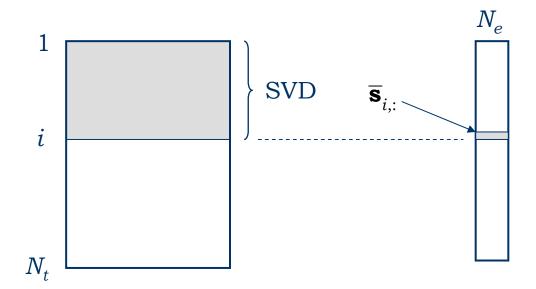
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- ideally designed to follow chromatography experiments
 - species appear & disappear sequentially
- capable of roughly following kinetic profiles
 - species can appear & dissappear simultaneously



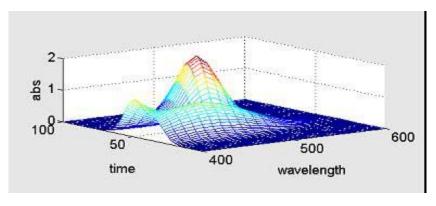
Forward EFA



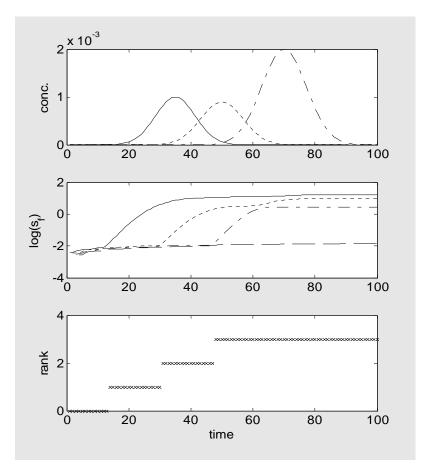
- Repeated rank analysis by SVD in forward direction
- The appearance of a new 'species' is indicated by a gradual rise of a new singular value



Chromatography

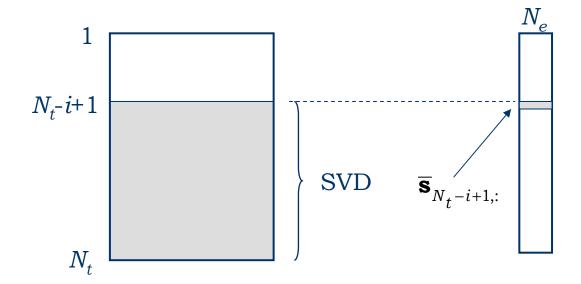


Forward EFA





Backward EFA

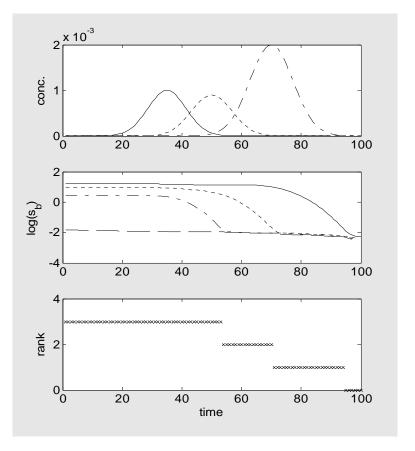


- Repeated rank analysis by SVD in backward direction
- A 'disappearing species' is indicated by a gradual rise of a new singular value



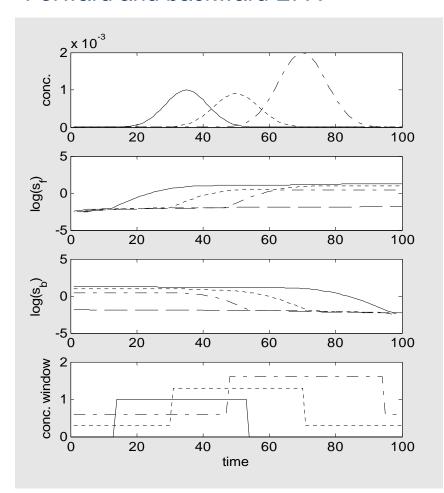
Matlab script using a function for forward/backward EFA

Backward EFA

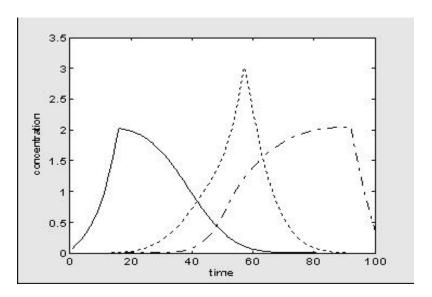




Forward and backward EFA



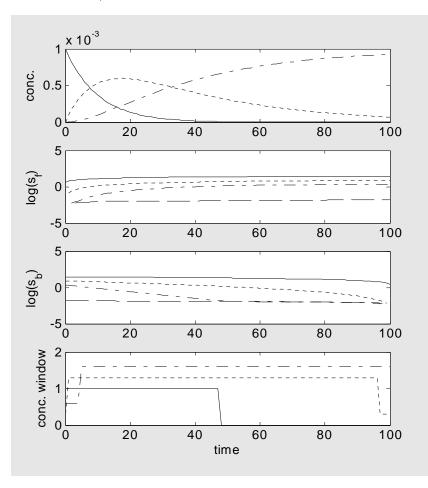
Combined forward/backward EFA results can be used as reasonable initial guesses of concentration profiles for subsequent iterative refinement e.g. by ALS



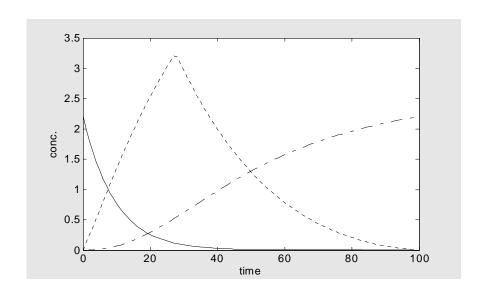
```
% combined SV curves
C=min(EFA_f(:,1:nc),fliplr(EFA_b(:,1:nc)));
```



A→B→C, Forward and backward EFA

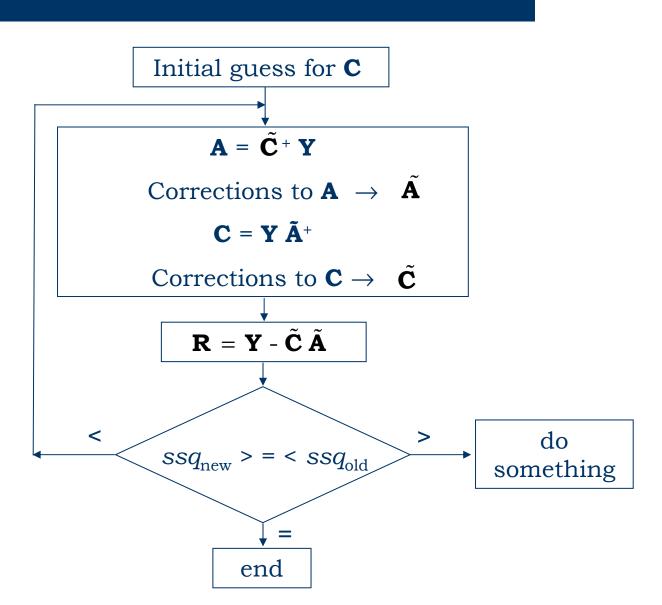


- Combined forward/backward EFA results are not as accurate as in chromatography regarding the appearance and disappearance of species
- But they can still be used as initial guesses of concentration profiles for subsequent iterative refinement e.g. by ALS



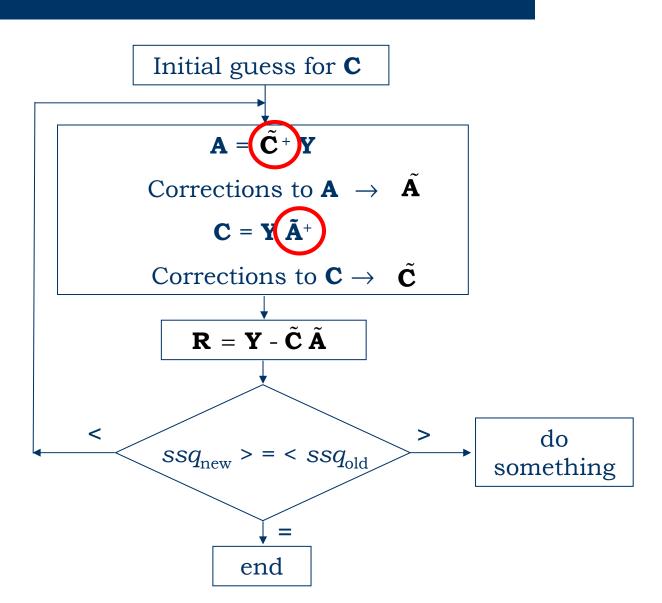


conceptually very simple





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$$Y = C \times A + R$$

$$R = Y - C \times A$$

$$\mathbf{R} \coloneqq f(\mathbf{Y}, \ \mathbf{C}, \ \mathbf{A})$$

The residuals **R** are a function of **Y** and the two linear parameters **C** & **A**



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1) Y & C known: $\min_{\mathbf{R}} \| \Sigma \Sigma r_{i,j}^2(\mathbf{A}) \|$ R is minimal in the least squares sense if

$$\mathbf{A} = (\mathbf{C}^{t}\mathbf{C})^{-1}\mathbf{C}^{t} \times \mathbf{Y} = \mathbf{C}^{+} \times \mathbf{Y}$$



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Matlab: A = C \ Y
to use the left pseudo inverse of C



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Matlab: A = C \ Y
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2) Y & A known: $\min \|\Sigma \Sigma r_{i,j}^2(\mathbf{C})\|$ R is minimal in the least squares sense if

$$\mathbf{C} = \mathbf{Y} \times \mathbf{A}^{\mathrm{t}} (\mathbf{A} \mathbf{A}^{\mathrm{t}})^{-1} = \mathbf{Y} \times \mathbf{A}^{+}$$



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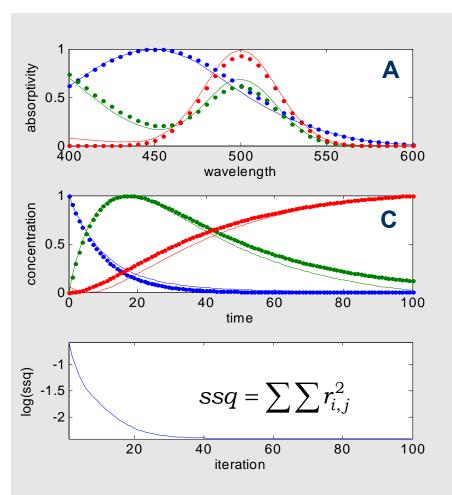
Matlab: C = Y / A
to use the left pseudo inverse of C



Normalisation to the maximum in each conc. profile

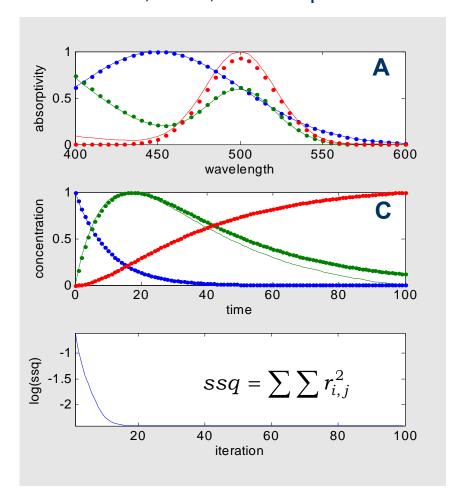
$$\begin{bmatrix} \mathbf{C}_{\mathrm{n}} \end{bmatrix} = \begin{bmatrix} \mathbf{C} \end{bmatrix} \times \begin{bmatrix} \mathbf{C} \end{bmatrix}$$
 and $\mathbf{A}_{\mathrm{n}} = diag(\max(\mathbf{C})) \times \mathbf{A}$

$A \rightarrow B \rightarrow C$ constraints: **C**, **A** >0



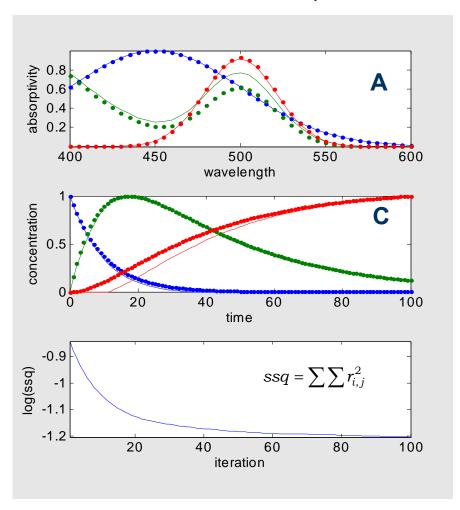


 $A \rightarrow B \rightarrow C$ constraints: **C**, **A** >0, known spectrum of *B*



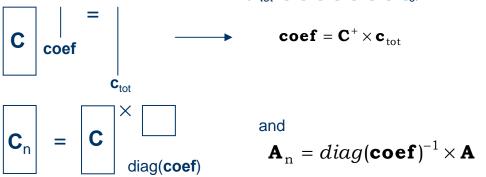


 $A \rightarrow B \rightarrow C$ constraints: **C**, **A** >0, known spectrum of *A* & *C*





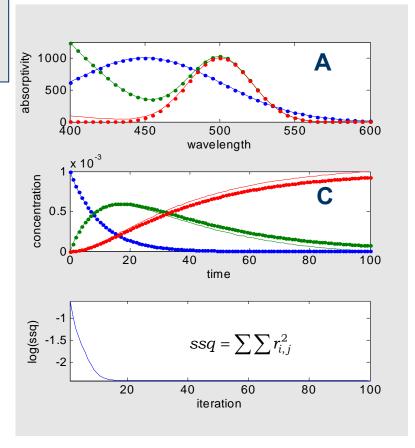
Normalisation to the total conc. $(c_{tot}=[A]+[B]+[C]=[A]_0)$



```
function [Cn,An] = norm_closure(C,A,c_tot)

coef=C\(ones(size(C,1),1)*c_tot); % norm. coeff.
Cn=C*diag(coef); % apply to C
if ~isempty(A)
   An=diag(1./coef)*A; % apply inv. to A
end
```

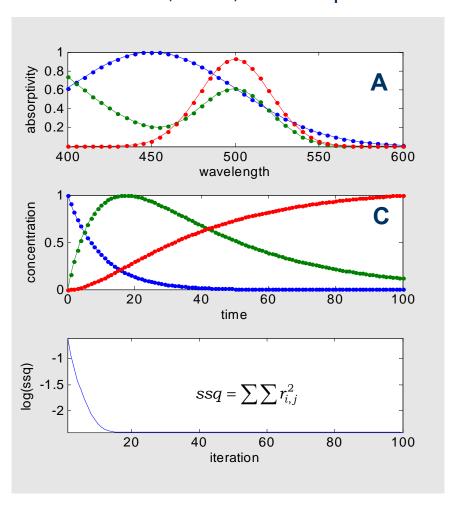
 $A \rightarrow B \rightarrow C$ constraints: **C**, **A** >0, known spectrum of *B*, closure





As full conversion is not reached for intermediate *B* and product *C*, corresponding known spectra are required for full resolution!

 $A \rightarrow B \rightarrow C$ constraints: **C**, **A** >0, known spectrum of *B* & *C*





Conclusions: 'Soft'-Modelling

Advantages

- No prior knowledge on the chemical system required
- Estimation of the number of linearly dependent absorbing species and their approximate evolution from PCA, EFA & ALS
- Info for the development of a 'hard' model
- 'Better than nothing'

Drawbacks

- No physical model
- No predictions for other exp. conditions possible
- Uniqueness of the result is rarely given and difficult to validate



Reading Material

Factor Analysis in Chemistry

E.R. Malinowski, 3rd ed., Wiley, New York 2002

Practical Data Analysis in Chemistry

M. Maeder, Y.M. Neuhold, Elsevier, Amsterdam 2007

Practical Guide to Chemometrics

P. Gemperline (editor), 2nd ed., CRC Press, Boca Raton 2006

The Investigation of Organic Reactions and their Mechanisms

H. Maskill (editor), Blackwell Publishing, Oxford 2006

Evolving factor analysis for the resolution of overlapping chromatographic peaks

M. Maeder, Anal. Chem. 59 (1987), 527-530

Nonlinear Least-Squares Fitting of Multivariate Absorption Data

M. Maeder, A. Zuberbühler. Anal. Chem. 62 (1990), 2220-2224

Analyses of 3-way data from equilibrium and kinetic investigations

R. Dyson , M. Maeder, Y.M. Neuhold, G. Puxty. Anal. Chim. Act. 490 (2003), 99-108

 Empirical kinetic modelling of on-line simultaneous infrared and calorimetric measurement using a pareto optimal approach and multi-objective genetic algorithm

S.I. Gianoli, G. Puxty, U. Fischer, M. Maeder, K. Hungerbühler. Chemom. Int. Lab. Syst. 85 (2007), 47-62

 Tutorial on the Fitting of Kinetic Models to Multivariate Spectroscopic Measurements with Non-Linear Regression

G. Puxty, M. Maeder, K. Hungerbühler. Chemom. Int. Lab. Syst. 81 (2006), 149-164

Data Oriented Process Development: Determination of Reaction Parameters by Small-Scale
 Calorimetry with in situ Spectroscopy

G. Puxty, U. Fischer, M. Jecklin, K. Hungerbühler. Chimia 60 (2006), 605-610



Soft- & Hard Modelling of Kinetic Data

Part 2: Hard Modelling



Introduction

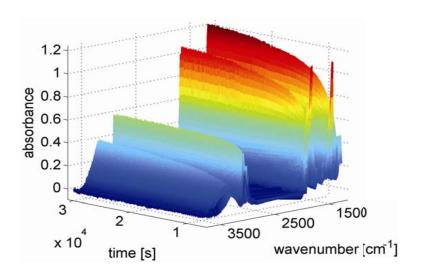
 You follow the reaction between BuOH and the Acetic Acid in the IR range and you get the following absorbance profile:

$$k$$
 TMG
 k
 TMG
 AA
 $BuOA$
 AH

-AL

Introduction

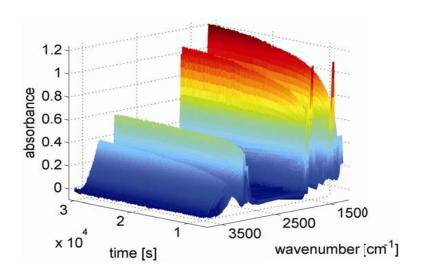
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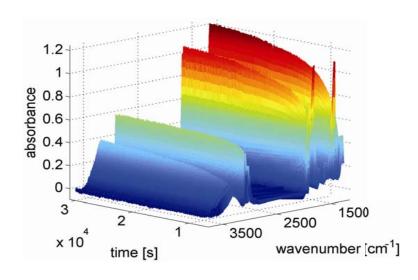
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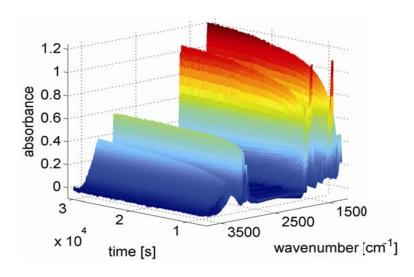
How can the rate constant be extracted from this profile?







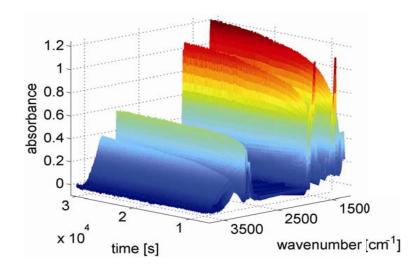
1. You determine the extinction coefficients of all species with known concentrations





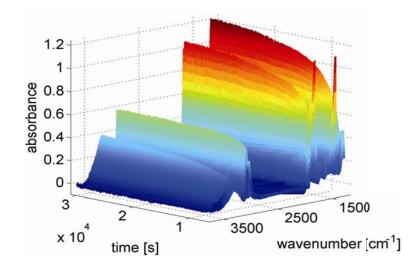
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$$\Rightarrow \text{all } \epsilon_{\lambda}$$



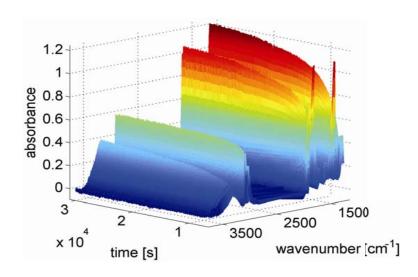


- 1. You determine the extinction coefficients of all species with known concentrations
 - $\Rightarrow \text{all } \epsilon_{\lambda}$
- 2. You integrate the set of differential equations (2nd order reaction) with the used initial concentrations



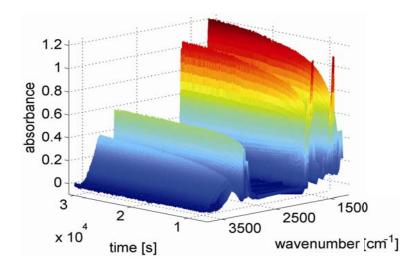


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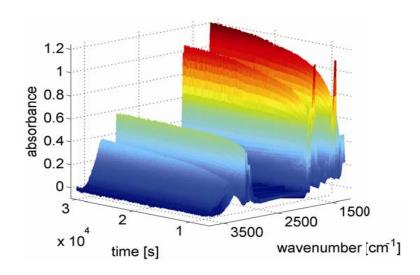
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$$abs_{\lambda}(t) = c_{BuOH}(t, k) \cdot \varepsilon_{BuOH, \lambda} + c_{AA, \lambda}(t, k) \cdot \varepsilon_{AA, \lambda}$$
$$+ c_{BuOA}(t, k) \cdot \varepsilon_{BuOA, \lambda} + c_{HA}(t, k) \cdot \varepsilon_{HA, \lambda}$$

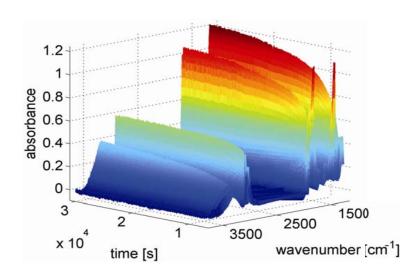




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You find k that best approximate the measured $abs_{\lambda}(t)$ in the least squares sense





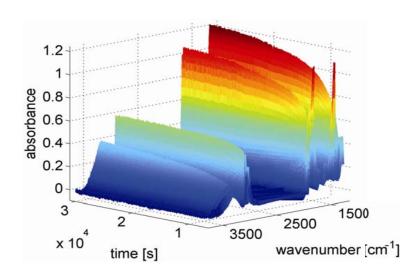
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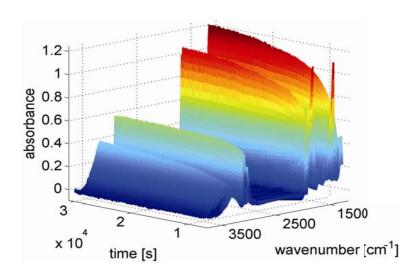


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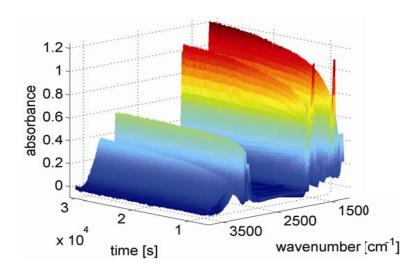
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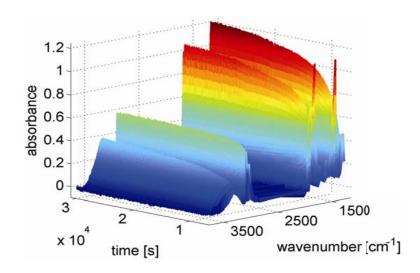


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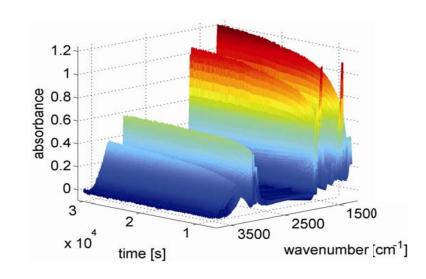


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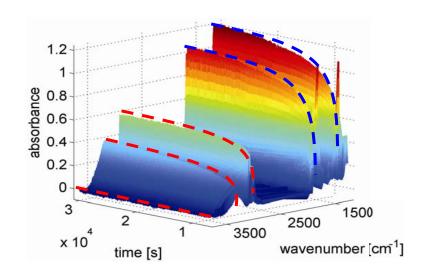
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KINETIC HARD-MODELING!!!



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KINETIC HARD-MODELING!!!

Question:

Which wavelength do you follow?
What about the rest of the spectrum?





KINETIC HARD-MODELING !!!

Question:

Which wavelength do you follow?







- Typical fitted signals
 - Multivariate Spectroscopy (Beer's law)
 - Univariate Calorimetry



- Typical fitted signals
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- Generalisation of the Rate Law



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The following topics will be addressed:

- Typical fitted signals
 - Multivariate Spectroscopy (Beer's law)
 - Univariate Calorimetry
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Two common problems will also be treated:



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1. Divergence problems (Levenberg-Marquardt modification)



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Two common problems will also be treated:

- 1. Divergence problems (Levenberg-Marquardt modification)
- 2. Rank deficiency (methods of annihilation)



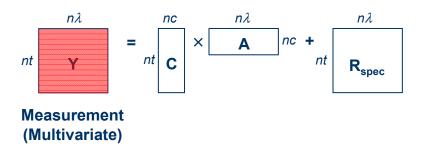
$$n\lambda = nc \times n\lambda = n\lambda$$

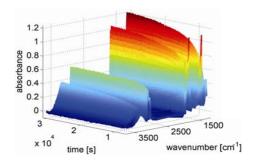
$$T \times A = nt \times A = nc + nt$$

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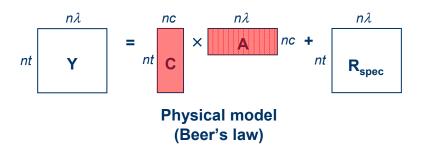
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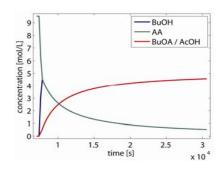


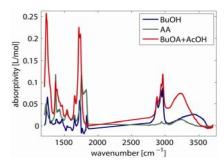




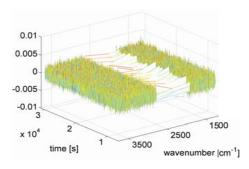














$$n\lambda = nc \times n\lambda = n\lambda$$

$$\mathbf{r} \times \mathbf{A} = nc + nc$$

$$\mathbf{R}_{spec}$$



Spectroscopy (IR, UV, Raman, fluorescence ...)

$$nt \qquad \mathbf{r} \qquad \mathbf{$$

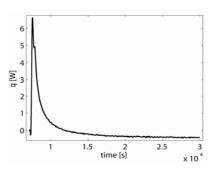
Calorimetry



Spectroscopy (IR, UV, Raman, fluorescence ...)

Calorimetry

Measurement (Univariate)

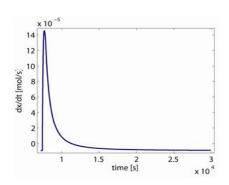




Spectroscopy (IR, UV, Raman, fluorescence ...)

Calorimetry

Physical model (Reaction heat balance)



× 43 kJ/mol



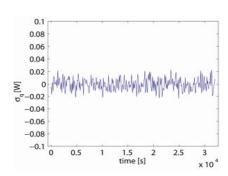
Spectroscopy (IR, UV, Raman, fluorescence ...)

Calorimetry

$$nt \begin{bmatrix} 1 \\ -nt \end{bmatrix} = \begin{bmatrix} np \\ nt \end{bmatrix} \times \begin{bmatrix} 1 \\ np \\ -\Delta H_R \end{bmatrix} + \begin{bmatrix} 1 \\ nt \end{bmatrix}$$

$$q \qquad \frac{d\xi_{mol}}{dt} \qquad r_{cal}$$

Unmodelled effects (Vector)



Spectroscopy (IR, UV, Raman, fluorescence ...)

Calorimetry

$$nt = \frac{np}{nt} \times \frac{1}{np} + \frac{1}{nt}$$

$$q \quad \frac{d\xi_{mol}}{dt} \qquad r_{cal}$$

$$\frac{\mathrm{d}\xi_{\mathrm{mol}}}{\mathrm{d}t} = \mathbf{V}(t) \cdot \mathbf{r}(t)$$



 The residuals are defined as the difference between the measurement and the model

$$\mathbf{Y} = \mathbf{C} \cdot \mathbf{A} + \mathbf{R}_{\text{spec}}$$

$$\mathbf{q} = \frac{\mathbf{d}\xi_{mol}}{\mathbf{d}t} \cdot \left(-\Delta \mathbf{H}_{R}\right) + \mathbf{r}_{cal}$$



 The residuals are defined as the difference between the measurement and the model

$$\mathbf{R}_{\mathrm{spec}} = \mathbf{Y} - \mathbf{C} \cdot \mathbf{A}$$

$$\mathbf{r}_{\mathrm{cal}} = \mathbf{q} - \frac{\mathbf{d}\xi_{\mathrm{mol}}}{\mathbf{d}t} \cdot \left(-\Delta \mathbf{H}_{\mathrm{R}}\right)$$



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As the mass balance part is :

$$\mathbf{C} = f(model, \mathbf{p})$$

$$\frac{\mathbf{d}\boldsymbol{\xi}_{\mathbf{mol}}}{\mathbf{d}\mathbf{t}} = g\left(model, \ \mathbf{p}\right)$$



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$$\mathbf{C} = f (model, \mathbf{p})$$

$$\frac{\mathbf{d}\boldsymbol{\xi}_{\mathbf{mol}}}{\mathbf{d}\mathbf{t}} = g\left(model, \ \mathbf{p}\right)$$

The optimisation problem is :

minimize
$$\mathbf{R}_{\text{spec}} = f(\mathbf{Y}, model, \mathbf{p})$$

in the least square sense
by changing \mathbf{p}

minimize
$$\mathbf{r}_{cal} = f(\mathbf{q}, model, \mathbf{p})$$

in the least square sense
by changing \mathbf{p}



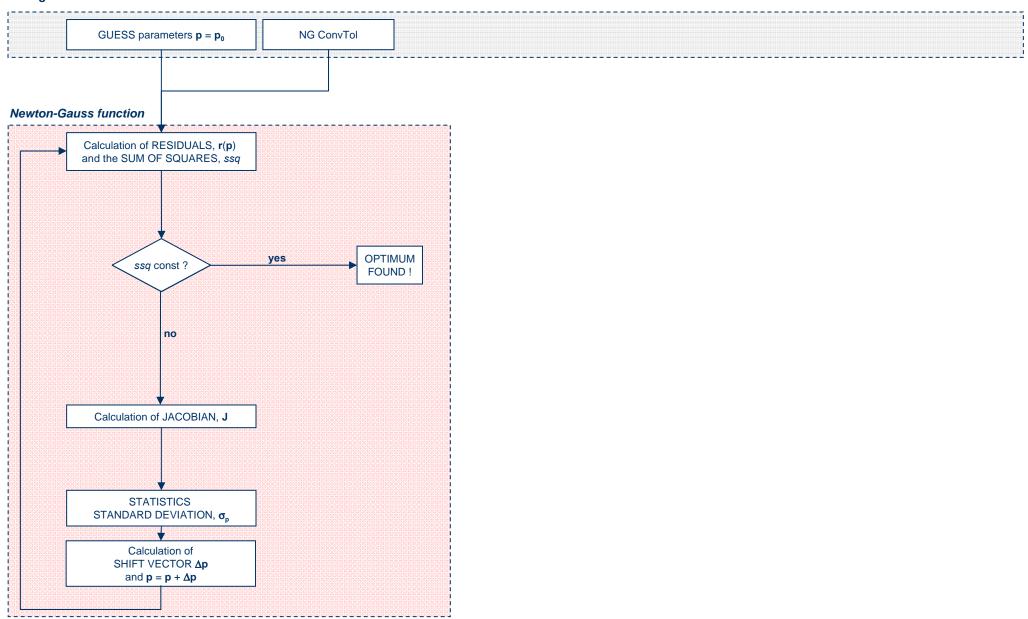


Settings

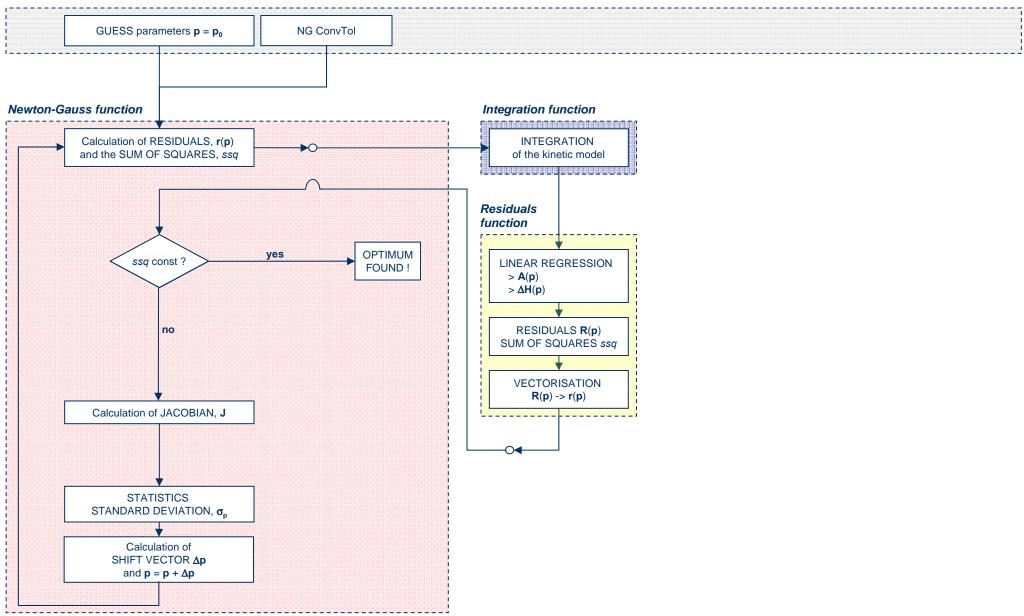
GUESS parameters $\mathbf{p} = \mathbf{p}_0$



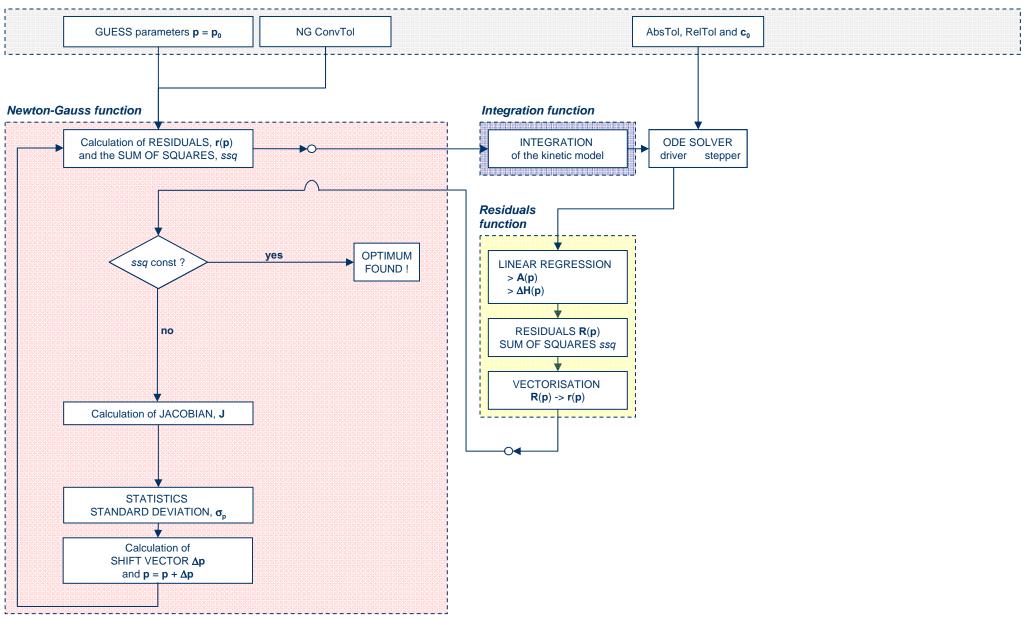




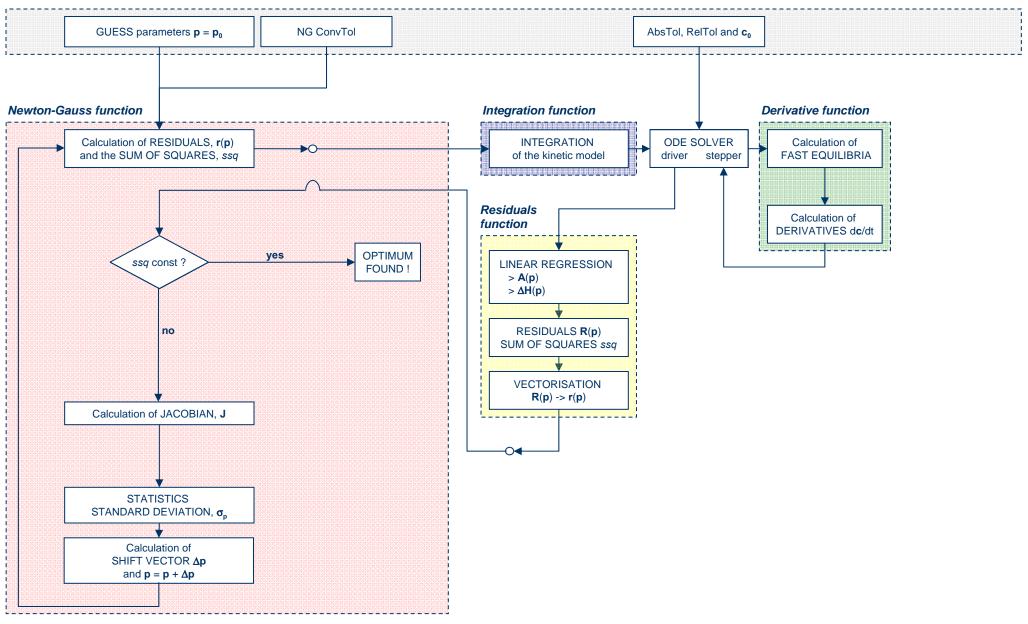




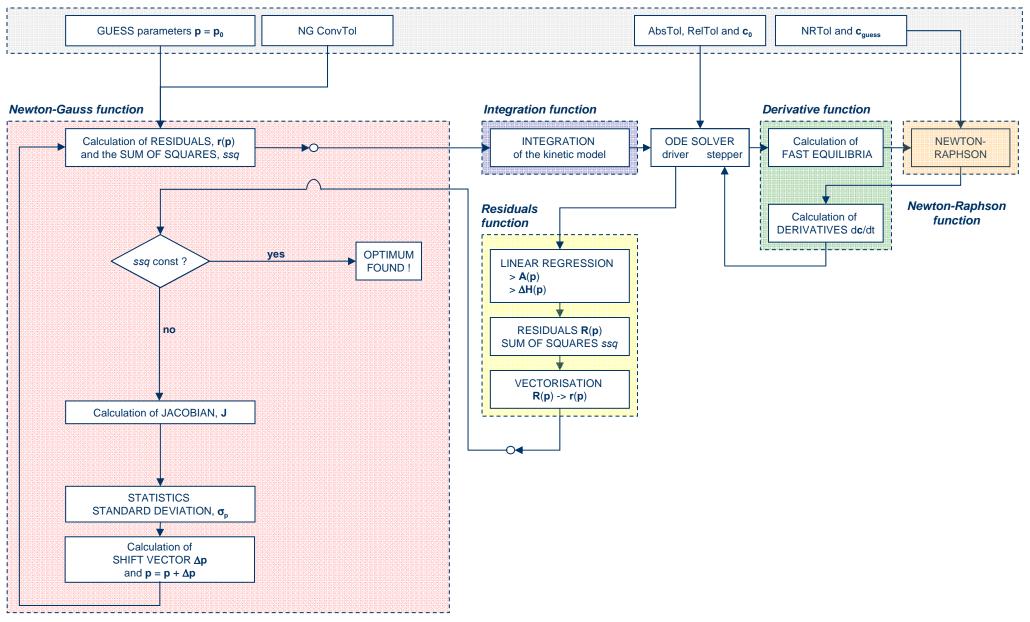




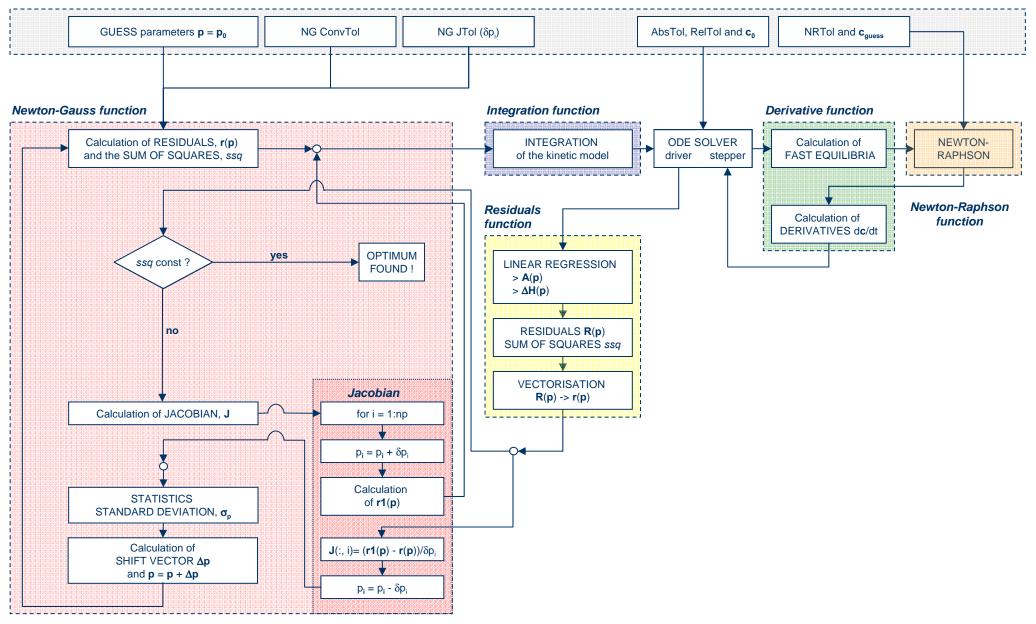




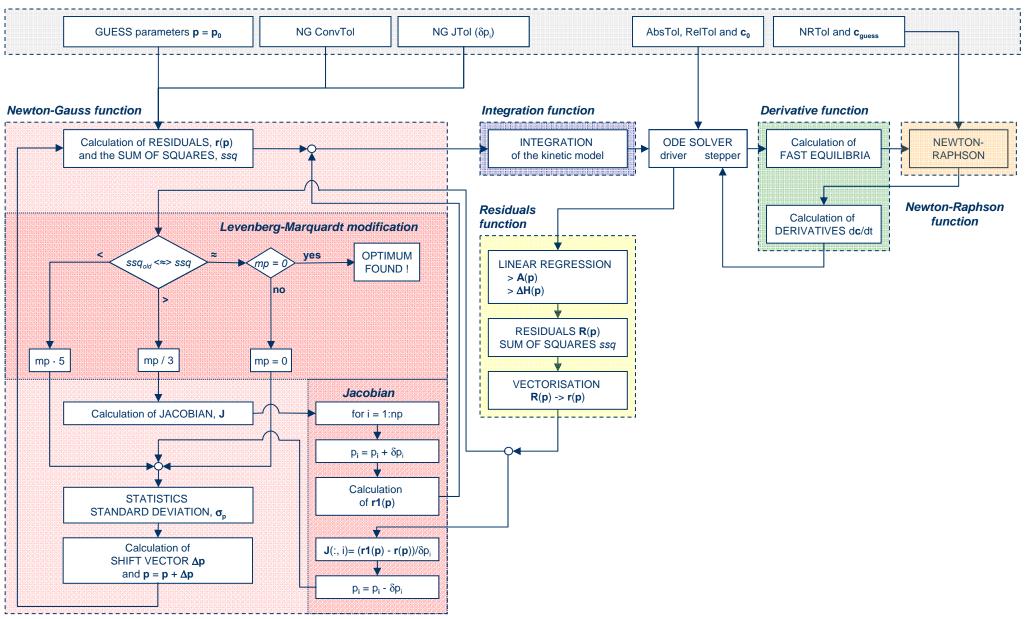






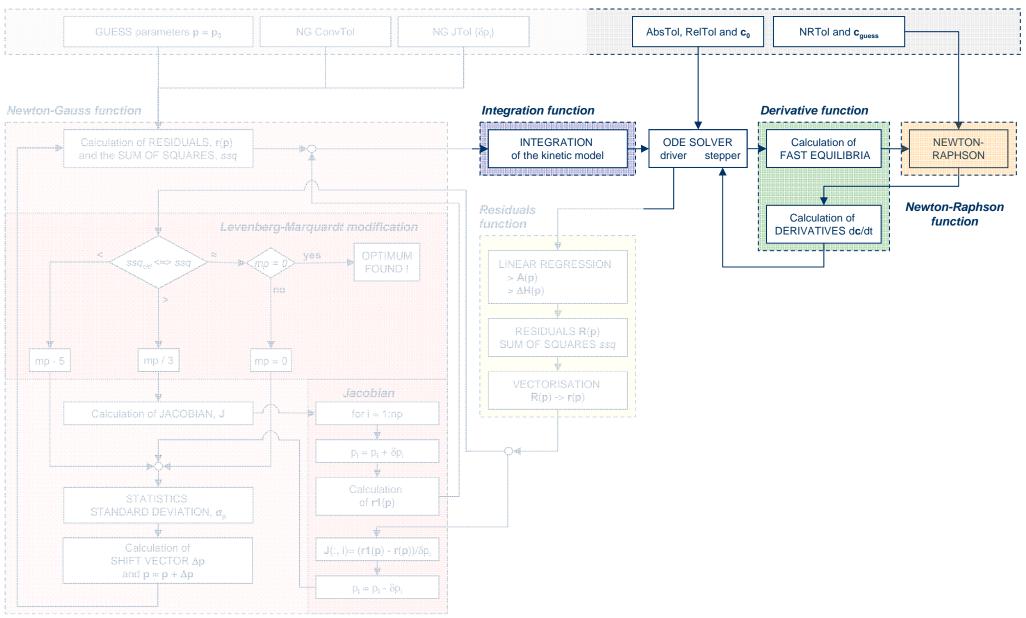














$$A + B \xrightarrow{k_1} C$$

$$2C \xrightarrow{k_2} D$$





$$\begin{array}{ccc}
A + B & \xrightarrow{k_1} & C \\
2C & \xrightarrow{k_2} & D
\end{array}$$



$$\begin{array}{ccc}
A + B & \xrightarrow{k_1} & C \\
2C & \xrightarrow{k_2} & D
\end{array}$$

$$\mathbf{X}_{p} = k_{1} & \mathbf{A} & \mathbf{B} & \mathbf{C} & \mathbf{D} \\ k_{2} & \mathbf{0} & \mathbf{0} & \mathbf{1} & \mathbf{0} \\ \mathbf{0} & \mathbf{0} & \mathbf{0} & \mathbf{1} & \mathbf{0} \\ \end{array}$$

$$X = X_p - X_R =$$
 k_1
 k_2
 k_3
 k_4
 k_5
 k_6
 k_7
 k_8
 k_8
 k_9
 k_9



Rate laws

$$r_{j} = k_{j} \prod_{i=1}^{nc} c_{i}^{\mathbf{X_{r}}_{j,i}} \qquad for \ j = 1:np$$

$$for j = 1: np$$

$$r_1 = k_1 \cdot [A]_t \cdot [B]_t$$
$$r_2 = k_2 \cdot [C]_t^2$$



$$\begin{array}{ccc}
A + B & \xrightarrow{k_1} & C \\
2C & \xrightarrow{k_2} & D
\end{array}$$

$$\mathbf{X}_{p} = \begin{array}{c|ccccc} & A & B & C & D \\ \hline & \mathbf{0} & \mathbf{0} & \mathbf{1} & \mathbf{0} \\ & k_{2} & \mathbf{0} & \mathbf{0} & \mathbf{0} & \mathbf{1} \\ \hline \end{array}$$

$$r_{j} = k_{j} \prod_{i=1}^{nc} c_{i}^{\mathbf{X_{r}}_{j,i}} \qquad for \ j = 1: np$$

$$for j = 1: np$$

$$\begin{bmatrix} r_1 = k_1 \cdot [A]_t \cdot [B]_t \\ r_2 = k_2 \cdot [C]_t^2 \end{bmatrix}$$

$$\frac{dc_i}{dt} = \sum_{j=1}^{np} \mathbf{X}_{j,i} \cdot r_j \qquad \text{for } i = 1:nc$$

for
$$i = 1 : nc$$

$$\frac{d[A]_{t}}{dt} = \frac{d[B]_{t}}{dt} = -r_{1}$$

$$\frac{d[C]_{t}}{dt} = r_{1} - 2 \cdot r_{2}$$

$$\frac{d[D]_{t}}{dt} = r_{2}$$



$$\begin{array}{ccc}
A + B & \xrightarrow{k_1} & C \\
2C & \xrightarrow{k_2} & D
\end{array}$$

$$\mathbf{X}_{p} = k_{1} & \mathbf{A} & \mathbf{B} & \mathbf{C} & \mathbf{D} \\ k_{2} & \mathbf{0} & \mathbf{0} & \mathbf{1} & \mathbf{0} \\ \mathbf{0} & \mathbf{0} & \mathbf{0} & \mathbf{1} & \mathbf{0} \\ \end{array}$$

$$X = X_{p} - X_{R} =$$
 k_{1}
 k_{2}
 k_{2}
 k_{3}
 k_{4}
 k_{5}
 k_{6}
 k_{7}
 k_{8}
 k_{7}
 k_{8}
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 k_{9}
 k_{9}
 k_{9}
 k_{9}

$$r_{j} = k_{j} \prod_{i=1}^{nc} c_{i}^{\mathbf{X_{r}}_{j,i}} \qquad for \ j = 1: np$$

$$for j = 1: np$$

$$r_1 = k_1 \cdot [A]_t \cdot [B]_t$$
$$r_2 = k_2 \cdot [C]_t^2$$

$$\frac{dc_i}{dt} = \sum_{j=1}^{np} \mathbf{X}_{j,i} \cdot r_j \qquad for \ i = 1 : nc$$

for
$$i = 1 : nc$$

$$\begin{vmatrix} \frac{d[A]_{t}}{dt} = \frac{d[B]_{t}}{dt} = -r \\ \frac{d[C]_{t}}{dt} = r_{1} - 2 \cdot r_{2} \\ \frac{d[D]_{t}}{dt} = r_{2} \end{vmatrix}$$

Most of the time: no analytical solution for this system of ODEs

→ Numerical integration



$$A + B \xrightarrow{k_1} C$$

$$2C \xrightarrow{k_2} D$$

In case of dosing, the set of ODEs is modified accordingly:



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$$r_j = k_j \prod_{i=1}^{ns} c_i^{\mathbf{X_{r}}_{j,i}}$$

for
$$j = 1: np$$

$$\begin{bmatrix} r_1 = k_1 \cdot [A]_t \cdot [B]_t \\ r_2 = k_2 \cdot [C]_t^2 \end{bmatrix}$$



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$$r_j = k_j \prod_{i=1}^{ns} c_i^{\mathbf{X_{r}}_{j,i}}$$

for
$$j = 1: np$$

for i = 1 : nc

$$r_1 = k_1 \cdot [A]_t \cdot [B]_t$$
$$r_2 = k_2 \cdot [C]_t^2$$

$$\frac{dc_{i}}{dt} = \left(\sum_{j=1}^{np} \mathbf{X}_{j,i} \cdot r_{j}\right) + \frac{F}{V_{t}} \cdot \left(c_{i}^{feed} - c_{i}\right)$$

$$\frac{dV}{dt} = F$$

$$for \ i = 1: r$$

$$\frac{d\left[A\right]_{t}}{dt} = -r_{1} + \frac{F}{V_{t}} \cdot \left(\left[A\right]^{feed} - \left[A\right]_{t}\right)$$

$$\frac{d\left[B\right]_{t}}{dt} = -r_{1} + \frac{F}{V_{t}} \cdot \left(\left[B\right]^{feed} - \left[B\right]_{t}\right)$$

$$\frac{d\left[C\right]_{t}}{dt} = r_{1} - 2 \cdot r_{2} + \frac{F}{V_{t}} \cdot \left(\left[C\right]^{feed} - \left[C\right]_{t}\right)$$

$$\frac{d\left[D\right]_{t}}{dt} = r_{2} + \frac{F}{V_{t}} \cdot \left(\left[D\right]^{feed} - \left[D\right]_{t}\right)$$

$$\frac{dV}{dt} = F$$



$$A + B \xrightarrow{k_1} C$$

$$2C \xrightarrow{k_2} D$$

In case of dosing, the set of ODEs is modified accordingly:

$$r_j = k_j \prod_{i=1}^{ns} c_i^{\mathbf{X_{r}}_{j,i}}$$

$$for j = 1:np$$

$$r_1 = k_1 \cdot [A]_t \cdot [B]_t$$
$$r_2 = k_2 \cdot [C]_t^2$$

$$\frac{dc_{i}}{dt} = \left(\sum_{j=1}^{np} \mathbf{X}_{j,i} \cdot r_{j}\right) + \frac{F}{V_{t}} \cdot \left(c_{i}^{feed} - c_{i}\right)$$

$$\frac{dV}{dt} = F$$

$$for \ i = 1:nc$$

$$\frac{d[A]_{t}}{dt} = -r\left(+\frac{F}{V_{t}}\cdot\left([A]^{feed} - [A]_{t}\right)\right)$$

$$\frac{d[B]_{t}}{dt} = -r_{1} + \frac{F}{V_{t}}\cdot\left([B]^{feed} - [B]_{t}\right)$$

$$\frac{d[C]_{t}}{dt} = r_{1} - 2\cdot r_{2} + \frac{F}{V_{t}}\cdot\left([C]^{feed} - [C]_{t}\right)$$

$$\frac{d[D]_{t}}{dt} = r_{2} + \frac{F}{V_{t}}\cdot\left([D]^{feed} - [D]_{t}\right)$$

$$\frac{dV}{dt} = F$$

$$NB: \quad + \frac{F}{V_t} \cdot A_{in} \quad = \text{added material}$$

$$- \frac{F}{V_t} \cdot A \quad = \text{dilution phenomenon}$$



Numerical integration of the model

First Approach : Euler's method

$$c_i(t + \Delta t) \approx c_i(t) + \left(\frac{dc_i}{dt}\right)_t \cdot \Delta t$$



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Applied to our specific example without dosing

$$A + B \xrightarrow{k_1} C$$

$$2C \xrightarrow{k_2} D$$

$$[C]_{t+\Delta t} \approx [C]_t + \left(\frac{d[C]_t}{dt}\right)_t \cdot \Delta t$$
$$= [C]_t + \left(k_1 \cdot [A]_t \cdot [B]_t - k_2 \cdot [C]_t^2\right) \cdot \Delta t$$



Numerical integration of the model

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 Nowadays, more sophisticated integration methods exist (e.g. ode45) with a stepsize control



Stepsize control and stiff problems

• In stepsize controlled ODE solvers, the stepsize is adjusted at each step to meet the user-specified accuracy



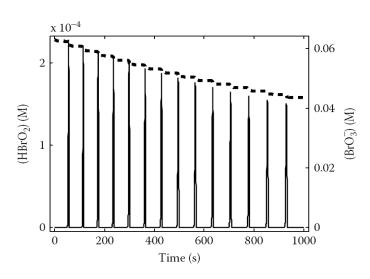
Stepsize control and stiff problems

- In stepsize controlled ODE solvers, the stepsize is adjusted at each step to meet the user-specified accuracy
- The accuracy is measured with absolute (*AbsToI*) and relative (*ReIToI*) tolerance's values.



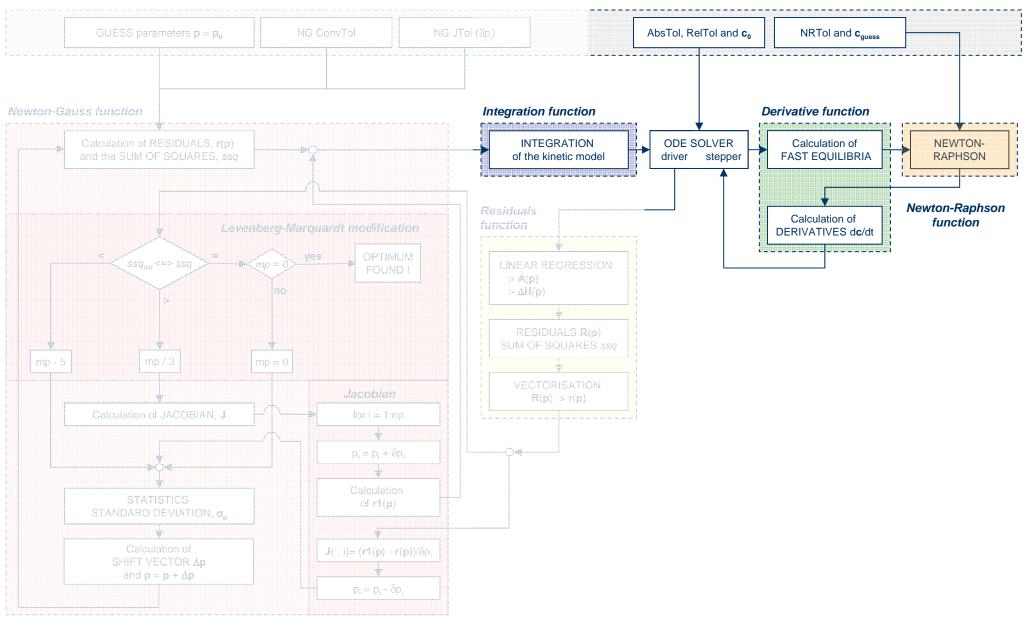
Stepsize control and stiff problems

- In stepsize controlled ODE solvers, the stepsize is adjusted at each step to meet the user-specified accuracy
- The accuracy is measured with absolute (AbsTol) and relative (RelTol) tolerance's values.
- For some kinetic models, the slopes of the concentration profiles are dramatically different (stiff problem) and require the use of a stiff ODE solver (eg. ode15s)



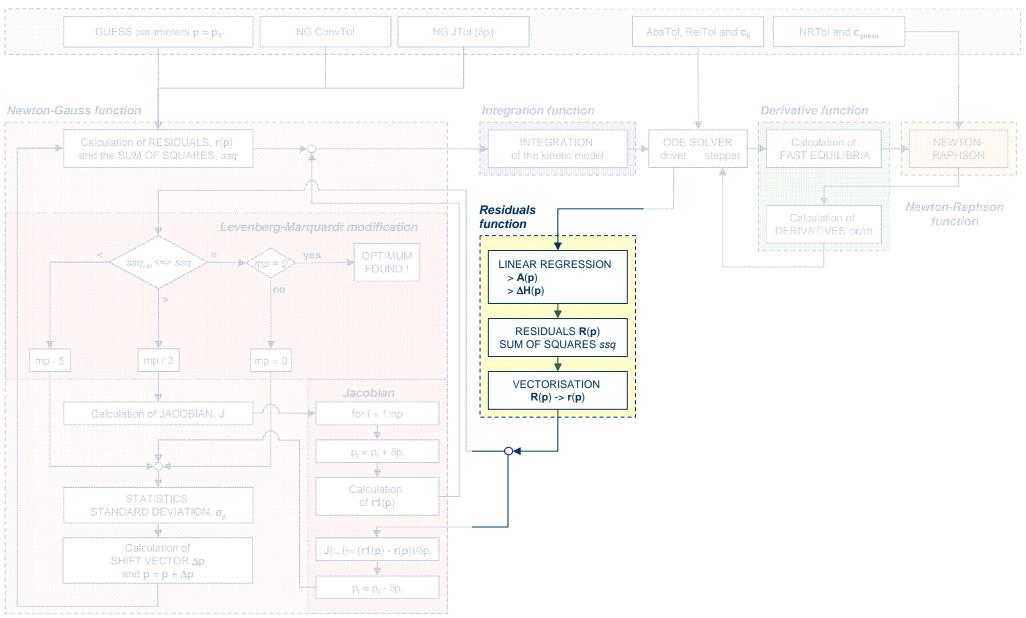
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Linear and Nonlinear parameters

GENERAL CONSIDERATION



Linear and Nonlinear parameters

GENERAL CONSIDERATION

• If $S(\mathbf{p})$ is a measured signal depending on the parameters vector \mathbf{p}

Linear parameters are defined as: $\left(\frac{\partial S(\mathbf{p})}{\partial p_i}\right)_{p_{\text{tot}}} \neq f(p_i)$

and **Nonlinear parameters** defined as: $\left(\frac{\partial S(\mathbf{p})}{\partial p_i}\right)_p = f(p)$



Linear and Nonlinear parameters

GENERAL CONSIDERATION

• If $S(\mathbf{p})$ is a measured signal depending on the parameters vector \mathbf{p}

Linear parameters are defined as: $\left(\frac{\partial S(\mathbf{p})}{\partial p_i}\right)_{p_i} \neq 0$

and **Nonlinear parameters** defined as: $\left(\frac{\partial S(\mathbf{p})}{\partial p_i}\right)_{i=1}^{\infty} = f(p_i)$

APPLIED TO KINETIC MODELING:

• C and A are LINEAR parameters with respect to Y (Beer's law)

$$Y = C \cdot A$$

• $d\xi_{mol}/dt$ and ΔH_r are LINEAR parameters with respect to q (Reaction heat balance)

$$q = \frac{d\xi_{mol}}{dt} \cdot \left(-\Delta H_R\right)$$

• Rate constants are NONLINEAR parameters with respect to $\bf C$ and ${d\xi_{mol}}/{dt}$ so are they for $\bf Y$ and for $\bf q$



Separation of linear parameters – LINEAR REGRESSION

• At each iteration, the linear parameters are calculated in one step as the best linear estimate in the least squares sense



Separation of linear parameters – LINEAR REGRESSION

 At each iteration, the linear parameters are calculated in one step as the best linear estimate in the least squares sense

$$\mathbf{A} = \mathbf{C}^{+} \cdot \mathbf{Y} = \left(\mathbf{C}^{t} \cdot \mathbf{C}\right)^{-1} \cdot \mathbf{C}^{t} \cdot \mathbf{Y}$$

$$\Delta H_{R} = -\left(\frac{d\xi_{mol}}{dt}\right)^{+} \cdot q = -\left(\left(\frac{d\xi_{mol}}{dt}\right)^{t} \cdot \left(\frac{d\xi_{mol}}{dt}\right)\right)^{-1} \cdot \left(\frac{d\xi_{mol}}{dt}\right)^{t} \cdot q$$

Remarks:

- The above formula is a multidimensional linear regression in a matrix notation
- The superscript + is meant for the PSEUDO-INVERSE.
 As the matrices are not square, the inverse is not defined.



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THIS LINEAR REGRESSION MAKES ANY CALIBRATION OF THE ABSORPTIVITIES REDUNDANT!



The Residuals and the sum of squares

- The residuals are defined as the difference between the measurement and the model (matrix!)
- By the sum of squares we mean the sum of all squared residuals (scalar!)



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Residuals

Spectroscopy: $R_{spec} = Y - Y_{calc} = Y - C \cdot A$

Calorimetry:
$$\mathbf{r_{cal}} = \mathbf{q} - \mathbf{q_{calc}} = \mathbf{q} - \frac{d\xi_{mol}}{dt} \cdot (-\Delta H_R)$$

Sum of squares

$$ssq_{spec} = \sum_{i=1}^{nt} \sum_{j=1}^{nw} \mathbf{R}_{spec} (i, j)$$

$$ssq_{cal} = \sum_{i=1}^{nt} \mathbf{r_{cal}}(i)$$



The Residuals and the sum of squares

- The residuals are defined as the difference between the measurement and the model (matrix!)
- By the sum of squares we mean the sum of all squared residuals (scalar!)

Residuals

$\mathbf{R}_{\text{snec}} = \mathbf{Y} - \mathbf{Y}_{\text{calc}} = \mathbf{Y} - \mathbf{C} \cdot \mathbf{A}$

Spectroscopy:

$$\mathbf{r_{cal}} = \mathbf{q} - \mathbf{q_{calc}} = \mathbf{q} - \frac{d\xi_{mol}}{dt} \cdot (-\Delta H_R)$$

Sum of squares

$$ssq_{spec} = \sum_{i=1}^{nt} \sum_{j=1}^{nw} \mathbf{R}_{spec} (i, j)$$

$$ssq_{cal} = \sum_{i=1}^{nt} \mathbf{r_{cal}}(i)$$

ADVANCED PROBLEM:

• Combination of the signals: $ssq_{total} = w \cdot ssq_{spec} + (1-w) \cdot ssq_{cal}$, w = ?





 The residuals of Spectroscopy and Calorimetry do not have the same dimension (How to combine a matrix with a vector ?)



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AND

 For practical reasons in the Newton-Gauss algorithm (see later)



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VECTORISATION:

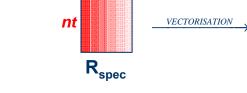
 $R_{\rm spec}$ and $r_{\rm cal}$ are unfolded into a long column vector r



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nλ

nλ x nt



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 The residuals of Spectroscopy and Calorimetry do not have the same dimension (How to combine a matrix with a vector ?)

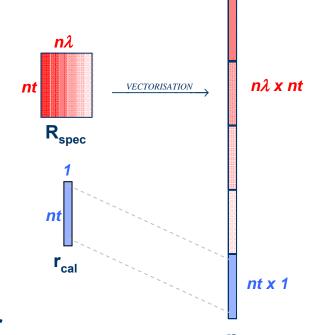
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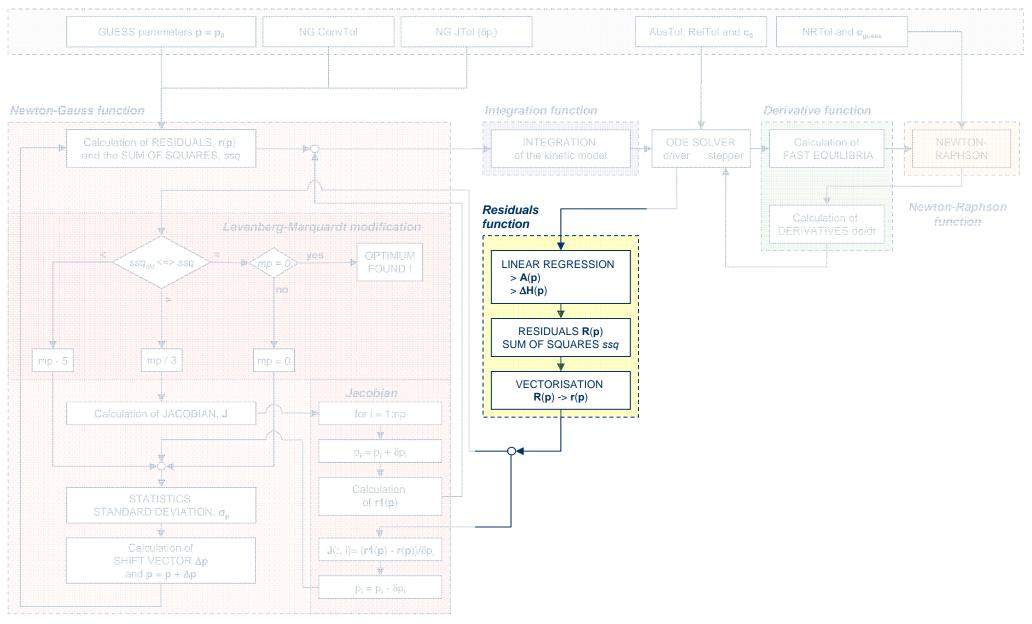
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Kinetic modeling algorithm



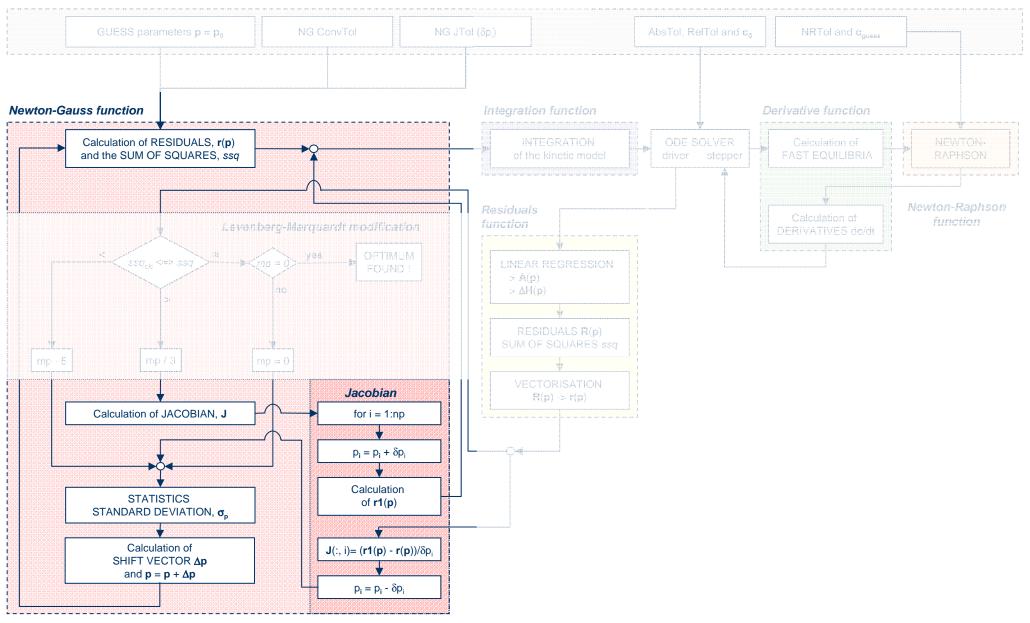




Kinetic modeling algorithm









• To find the direction towards the minimum, the residuals are approximated by a **Taylor series expansion truncated after the first derivative**



To find the direction towards the minimum, the residuals are approximated by a
 Taylor series expansion truncated after the first derivative

$$\mathbf{r}(\mathbf{p} + \Delta \mathbf{p}) = \mathbf{r}(\mathbf{p}) + \frac{\partial \mathbf{r}(\mathbf{p})}{\partial \mathbf{p}} \cdot \Delta \mathbf{p}$$



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$$\downarrow \qquad \text{Rearranging for } \mathbf{r}(\mathbf{p})$$

$$\mathbf{r}(\mathbf{p}) \qquad = -\mathbf{J} \cdot \Delta \mathbf{p} + \mathbf{r}(\mathbf{p} + \Delta \mathbf{p})$$



To find the direction towards the minimum, the residuals are approximated by a
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$$r(p + \Delta p) = r(p) + \frac{\partial r(p)}{\partial p} \cdot \Delta p$$

$$\downarrow \qquad \text{Rearranging for } r(p)$$

$$r(p) \qquad = -J \cdot \Delta p + r(p + \Delta p) \approx 0!$$

-

The Newton-Gauss algorithm

To find the direction towards the minimum, the residuals are approximated by a
 Taylor series expansion truncated after the first derivative

$$\Delta \mathbf{p} = -\mathbf{J}^+ \cdot \mathbf{r}(\mathbf{p})$$

The **SHIFT VECTOR** is added to **p** for the next iteration



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 Taylor series expansion truncated after the first derivative

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The Newton-Gauss algorithm requires the calculation of the Jacobian

$$\mathbf{J} = \frac{\partial \mathbf{r}(\mathbf{p})}{\partial \mathbf{p}}$$



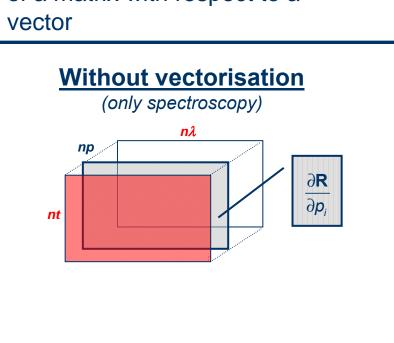
$$\mathbf{J} = \frac{\partial \mathbf{r}(\mathbf{p})}{\partial \mathbf{p}}$$

The Jacobian is a derivative of a matrix with respect to a vector



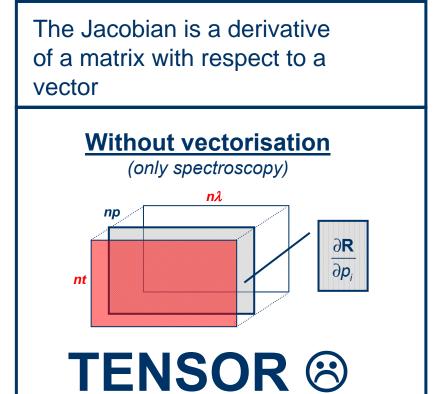
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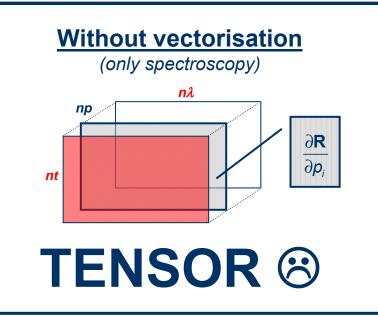


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To compute the Jacobian, one needs to vectorise the residuals **R** into a long vector **r**



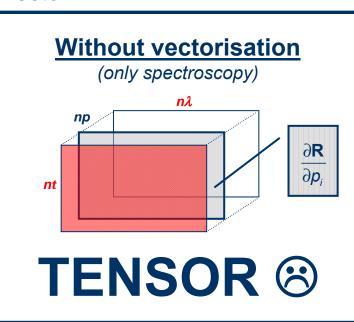


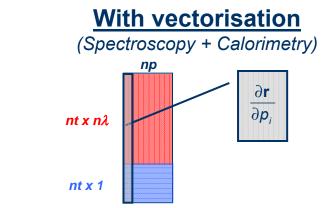
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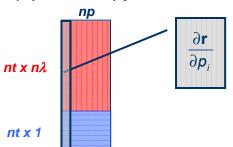
To compute the Jacobian, one needs to vectorise the residuals **R** into a long vector **r**

Without vectorisation (only spectroscopy) na np oR op,

TENSOR (2)

With vectorisation

(Spectroscopy + Calorimetry)



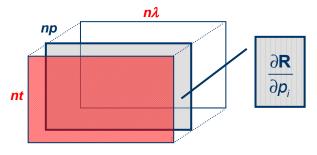
MATRIX ©



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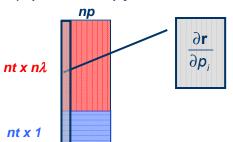
TENSOR 🐵



To compute the Jacobian, one needs to vectorise the residuals **R** into a long vector **r**

With vectorisation

(Spectroscopy + Calorimetry)



MATRIX ©

The Jacobian is computed using a forward finite difference

$$\frac{\partial \mathbf{r}(\mathbf{p})}{\partial p_i} = \frac{\mathbf{r}(\mathbf{p} + \delta p_i) - \mathbf{r}(\mathbf{p})}{\delta p_i}$$

with
$$\delta p_i \approx 10^{-6} \cdot p_i$$



The Hessian (statistics)

$$\mathbf{H} = \mathbf{J}^{\mathsf{t}} \cdot \mathbf{J}$$

• Knowing that $\mathbf{H} = \mathbf{J}^t \cdot \mathbf{J}$ the shift vector can be re-written as:

$$\Delta \mathbf{p} = -\mathbf{H}^{-1} \cdot \mathbf{J}^{\mathbf{t}} \cdot \mathbf{r}(\mathbf{p})$$



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The Hessian \mathbf{H} is a square matrix ($np \times np$) and is the inverse of the variance/covariance matrix of \mathbf{p} !



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The Hessian **H** is a square matrix (*np* x *np*) and is the inverse of the variance/covariance matrix of **p**!

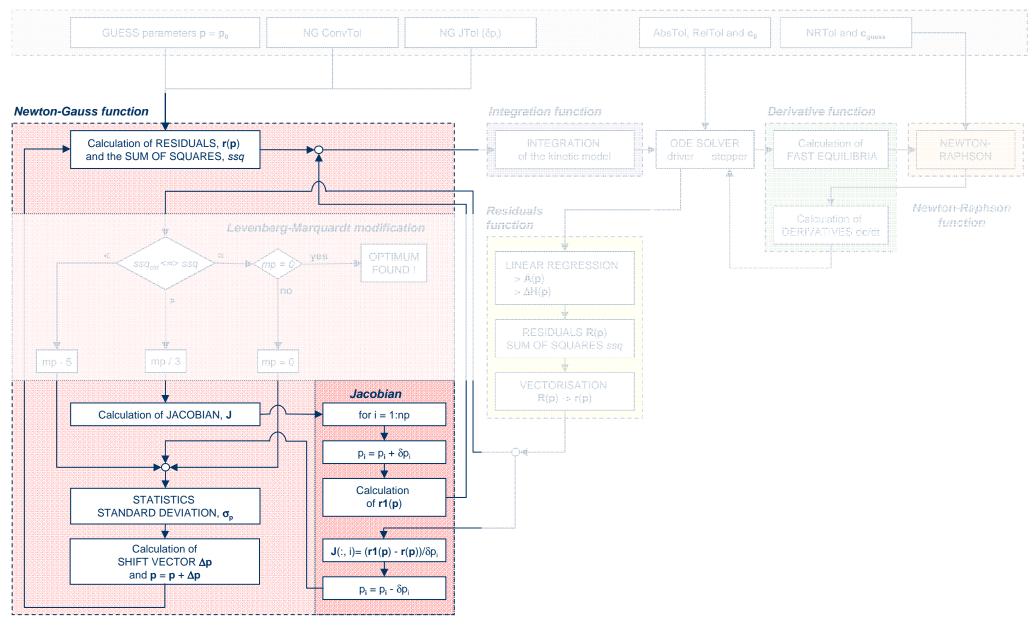
This allows the calculation of the **Standard Error** of each parameter :

$$\sigma_{\rm p} = \sigma_{\rm r} \cdot \sqrt{diag\left(H^{-1}\right)}$$
 with $\sigma_{\rm r} = \sqrt{\frac{ssq}{df}} \approx \sigma_{\rm Y}$

Kinetic modeling algorithm



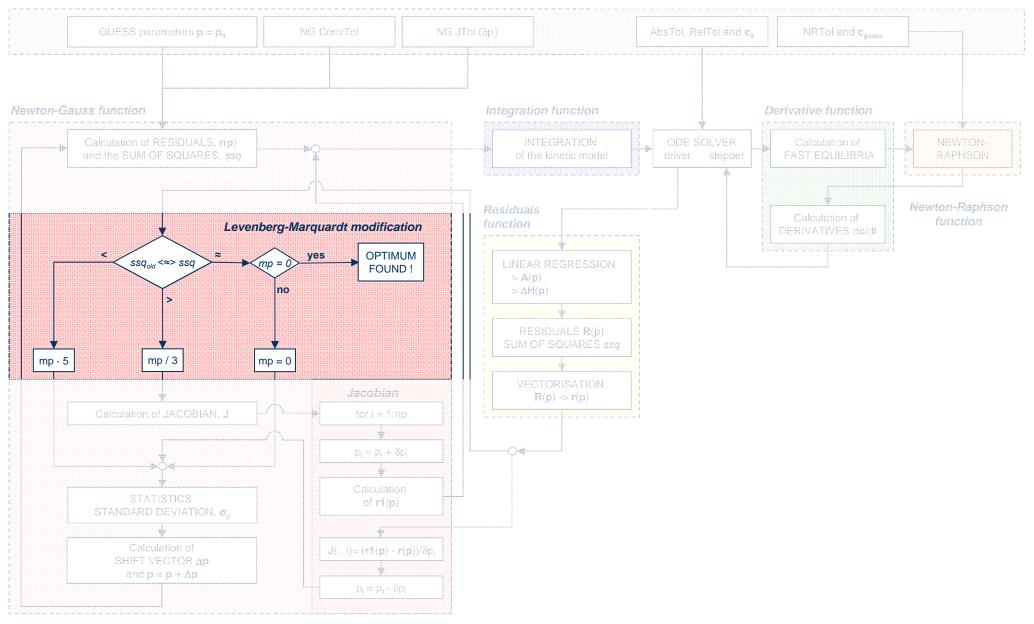
Setting



Kinetic modeling algorithm









PROBLEM: The NG algorithm **DIVERGES** if the Taylor series expansion

is not a good approximation for the residuals function

(eg. poor initial guesses)



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$$\Delta \mathbf{p} = -\mathbf{H}^{-1} \cdot \mathbf{J}^{\mathbf{t}} \cdot \mathbf{r}(\mathbf{p})$$
Is there a way to switch progressively from one method to the other?

Inverse Hessian method (Newton-Gauss)

$$\Delta \mathbf{p} = -\mathbf{J}^{t} \cdot \mathbf{r} (\mathbf{p})$$



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$$\Delta \mathbf{p} = -\mathbf{H}^{-1} \cdot \mathbf{J}^{t} \cdot \mathbf{r}(\mathbf{p})$$

$$\Delta \mathbf{p} = -(\mathbf{H} + mp \cdot \mathbf{I})^{-1} \cdot \mathbf{J}^{t} \cdot \mathbf{r}(\mathbf{p})$$

Inverse Hessian method

(Newton-Gauss)

Levenberg-Marquardt modification

$$\Delta \mathbf{p} = -\mathbf{J}^{t} \cdot \mathbf{r} \left(\mathbf{p} \right)$$

Steepest Descent Method



Divergence in the NG algorithm

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$$\Delta \mathbf{p} = -\mathbf{J}^{t} \cdot \mathbf{r}(\mathbf{p})$$

Inverse Hessian method

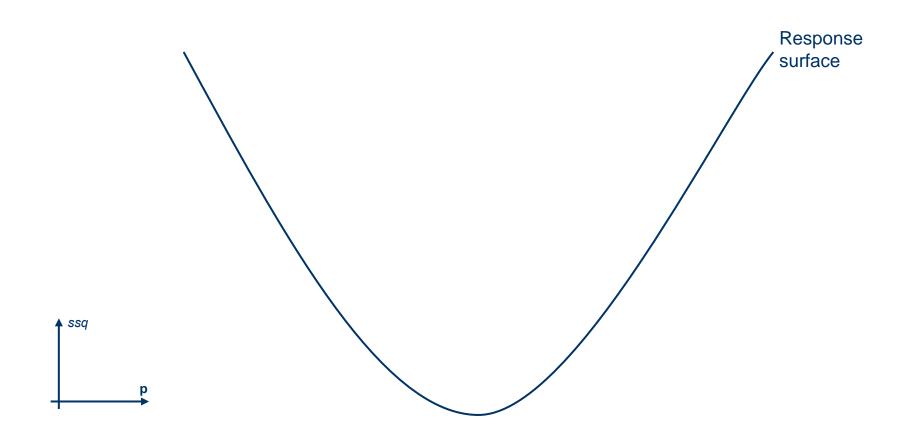
(Newton-Gauss)

Levenberg-Marquardt modification

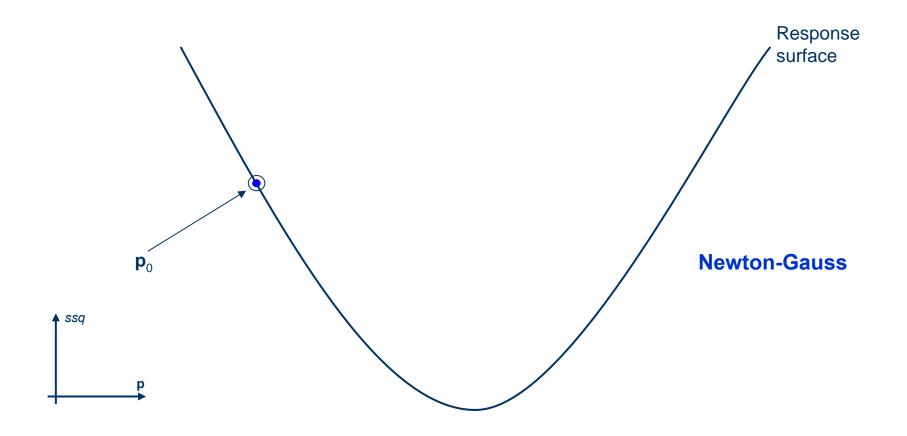
The Marquardt parameter (mp) is a scalar added to the diagonal elements of $\bf H$ to decrease its influence on $\Delta \bf p$ and shorten the magnitude of $\Delta \bf p$

Steepest Descent Method

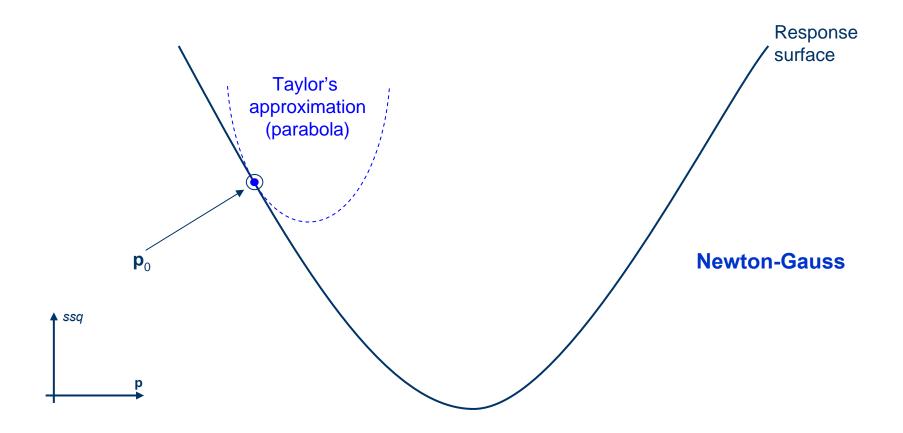




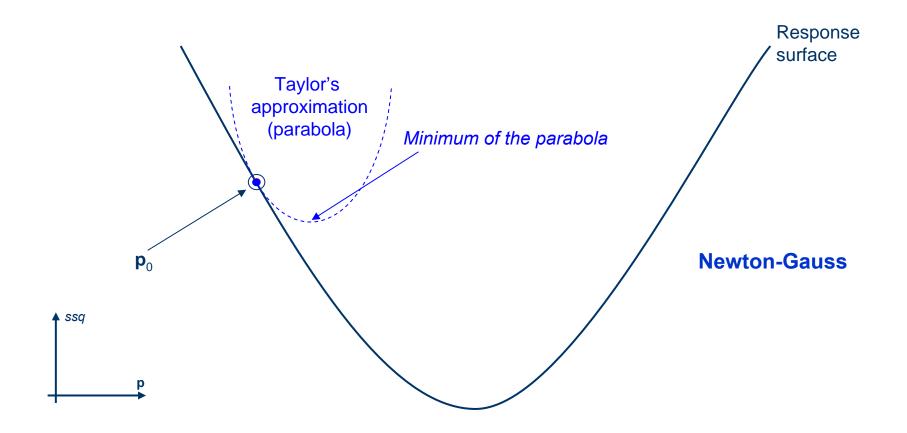




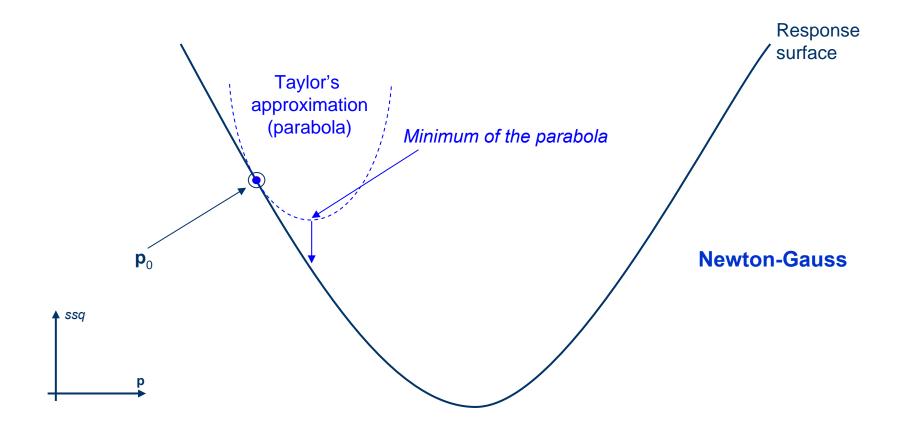




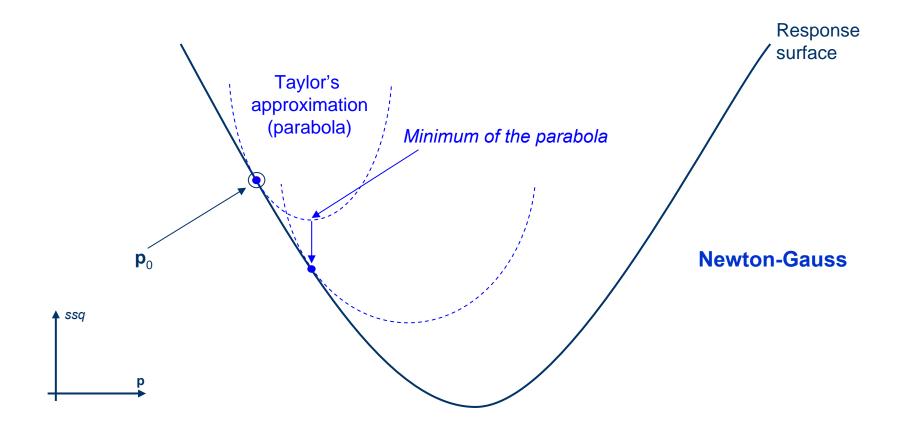




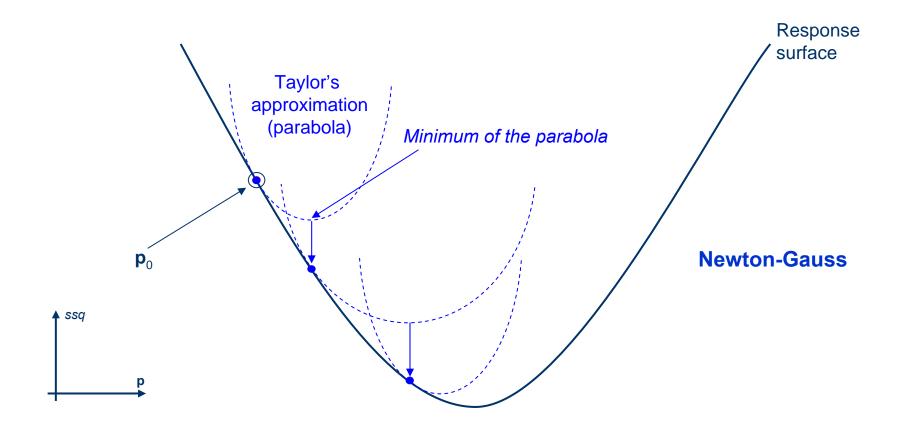




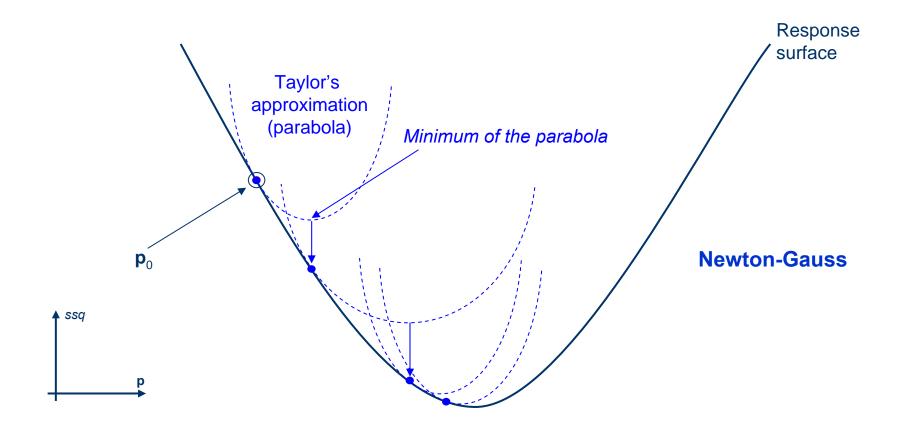




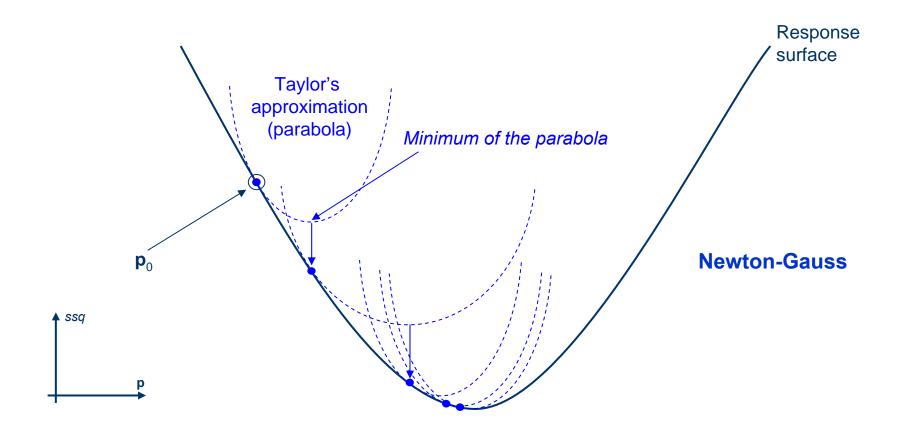




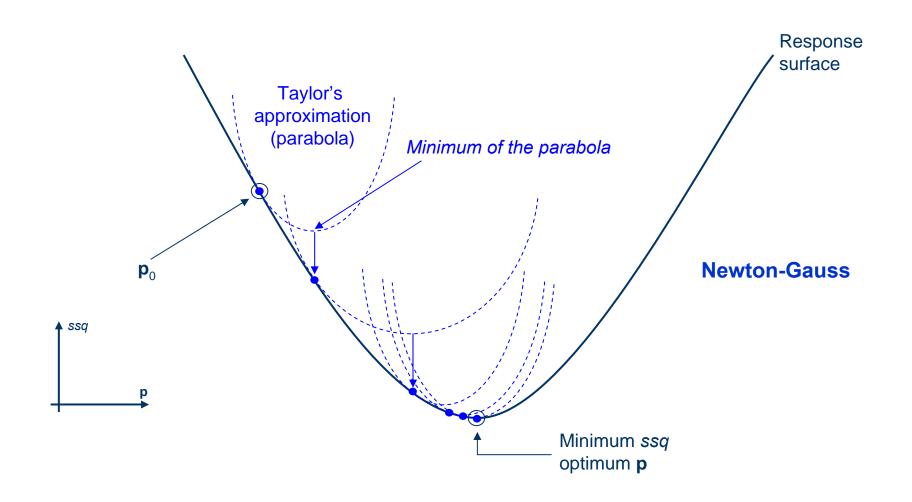




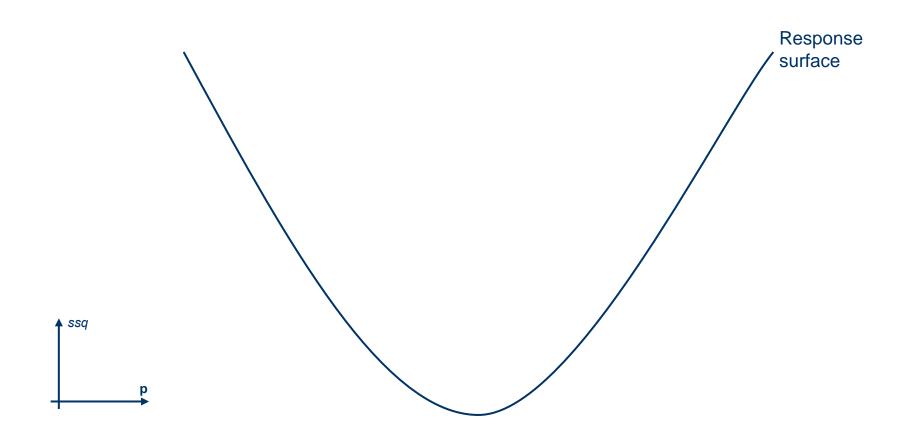




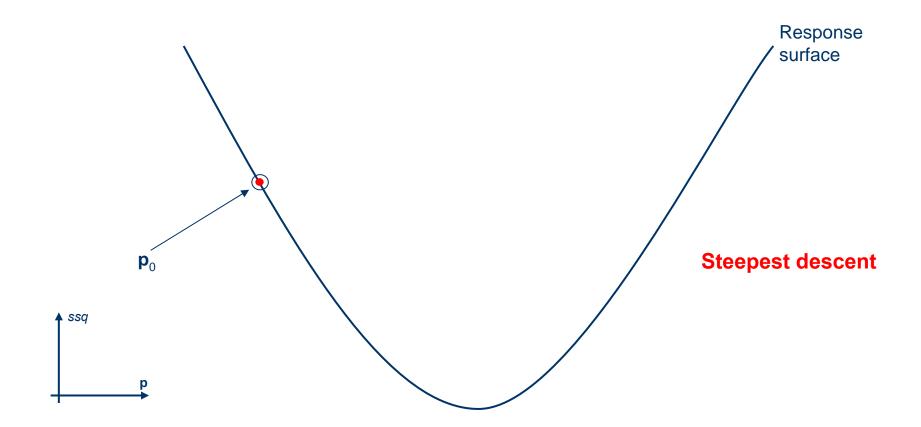




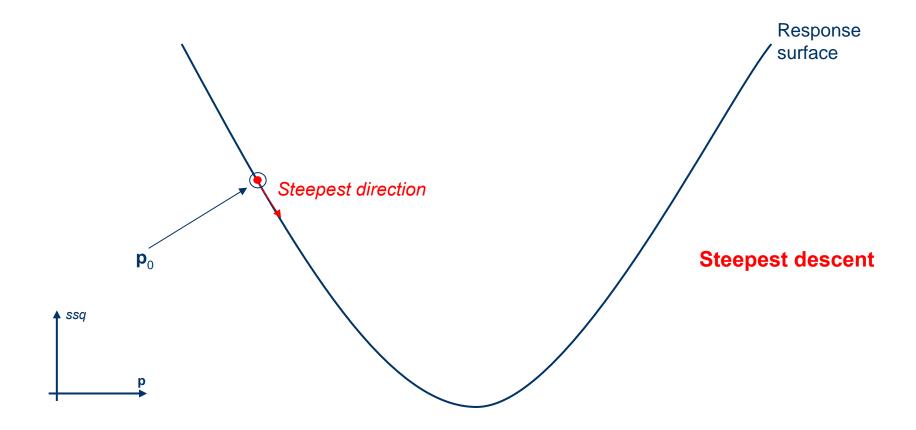




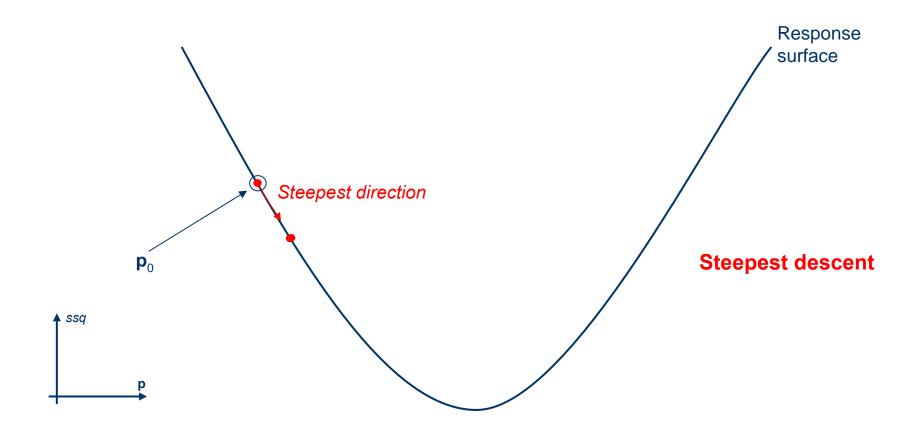




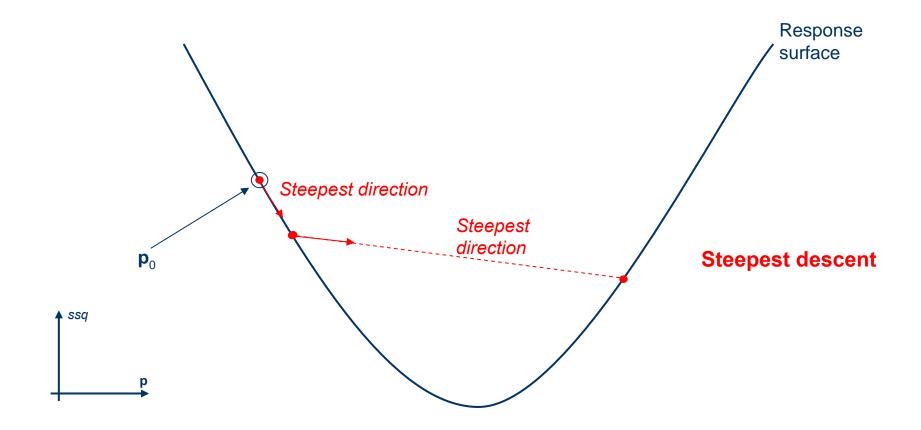




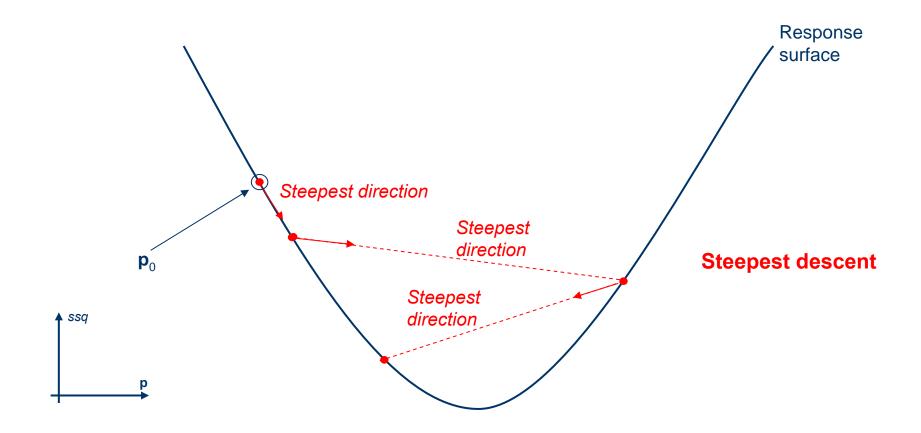




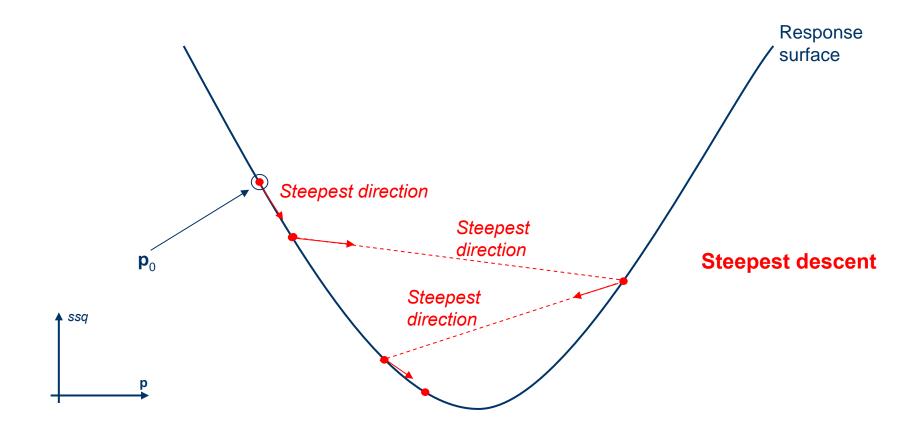




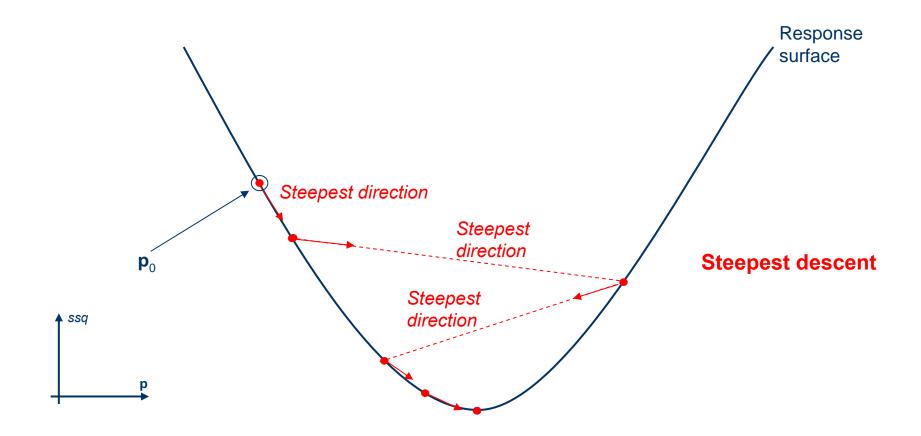




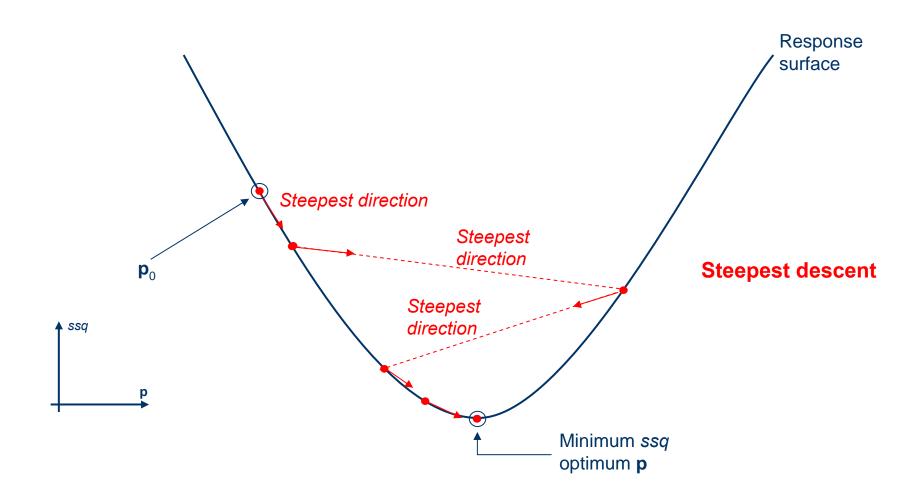




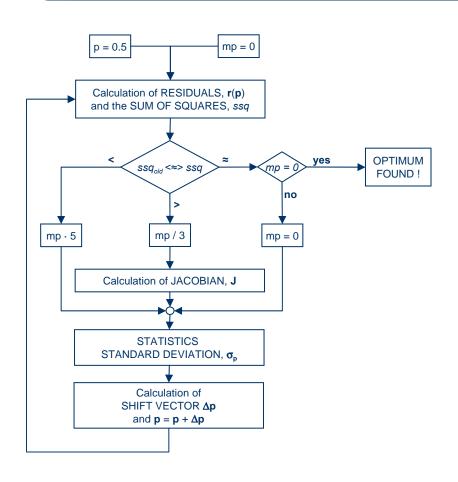




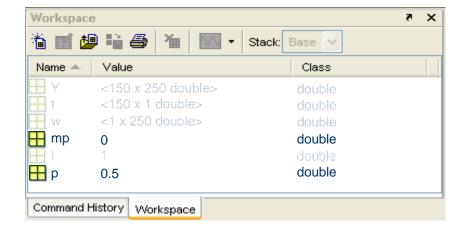


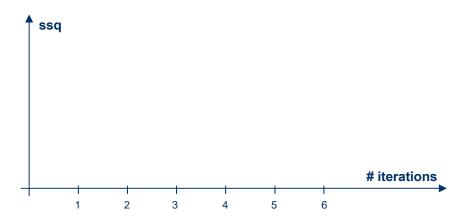




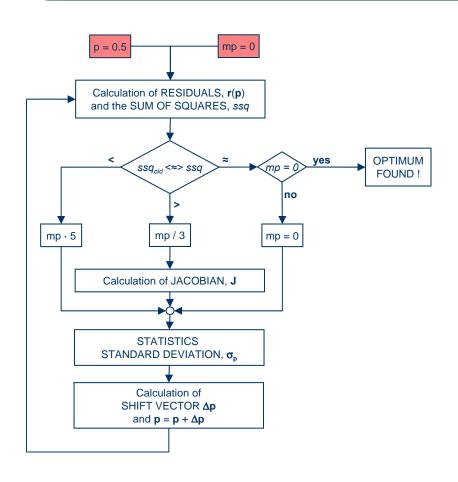


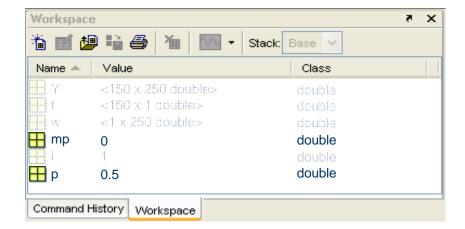
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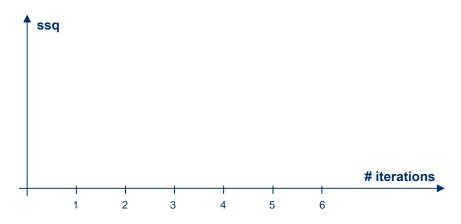




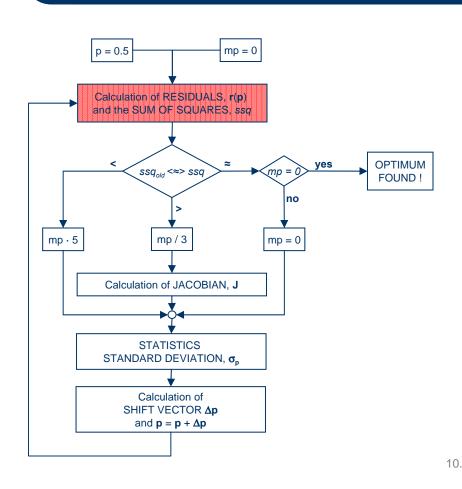


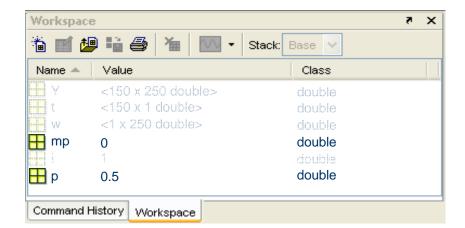


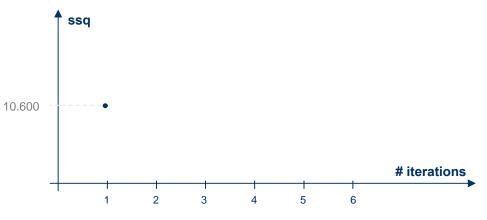




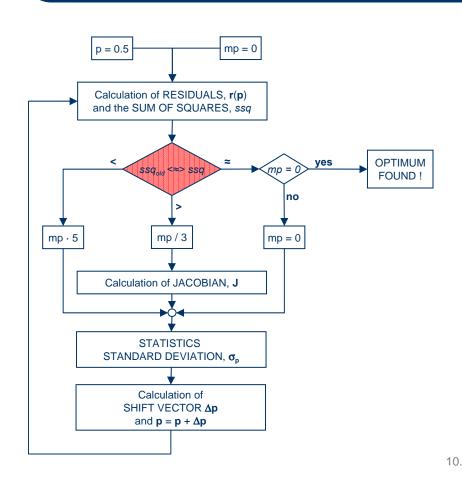


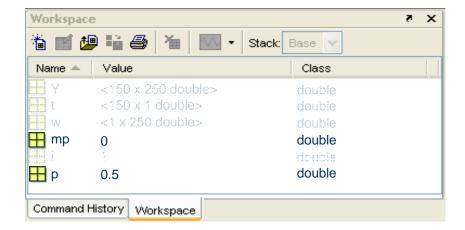


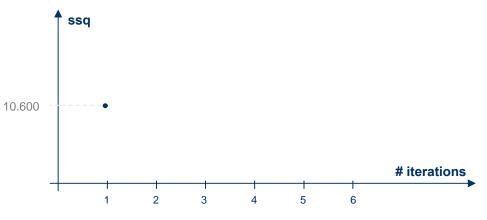




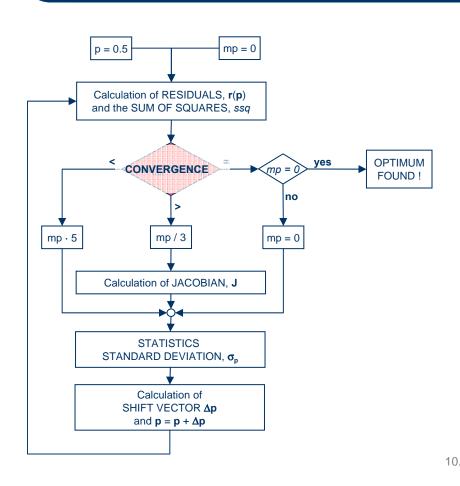


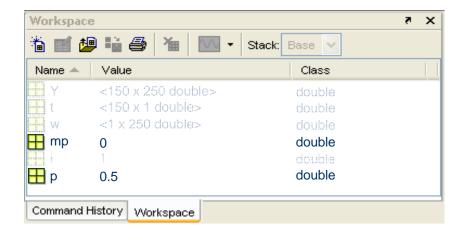


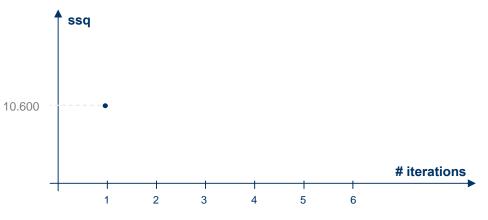




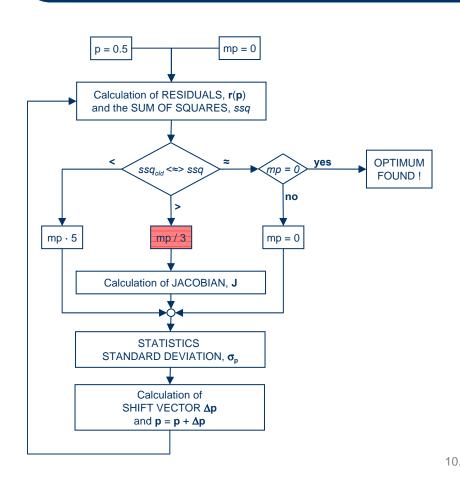


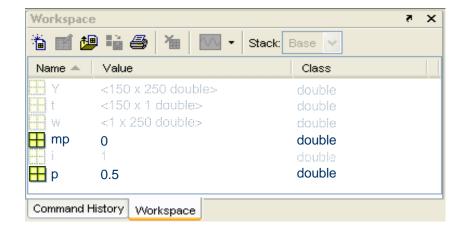


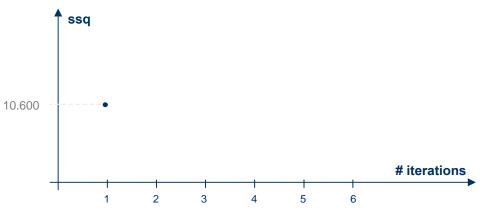




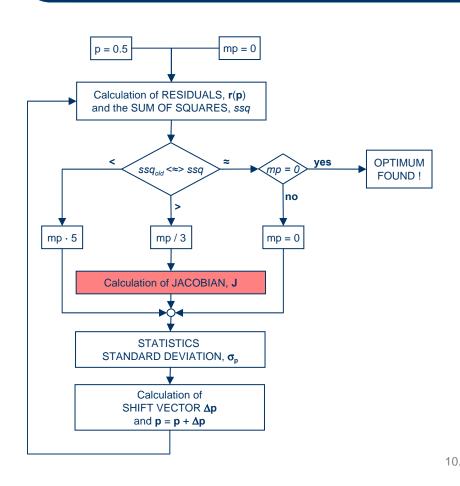


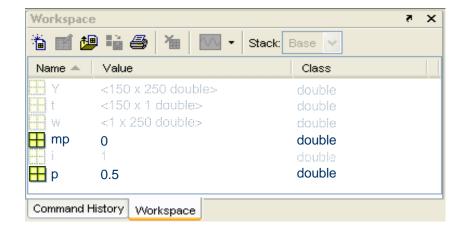


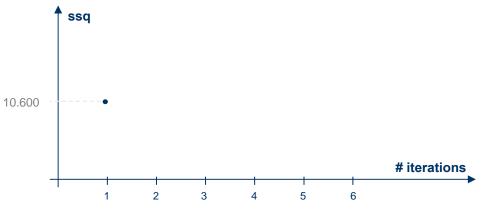




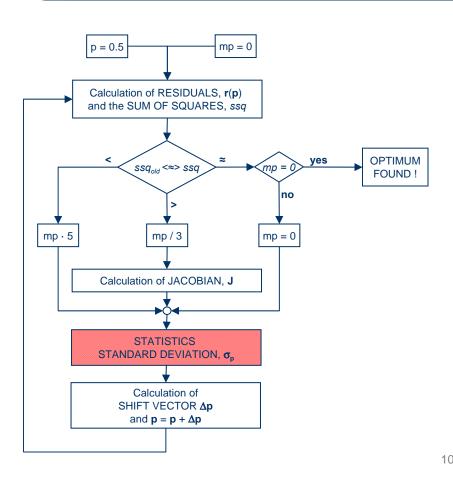






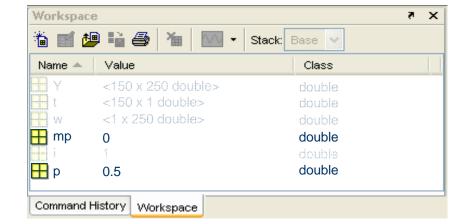


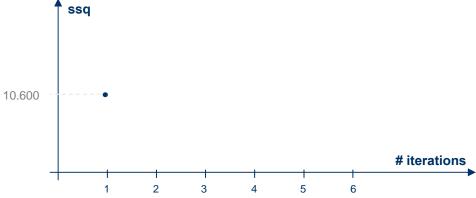




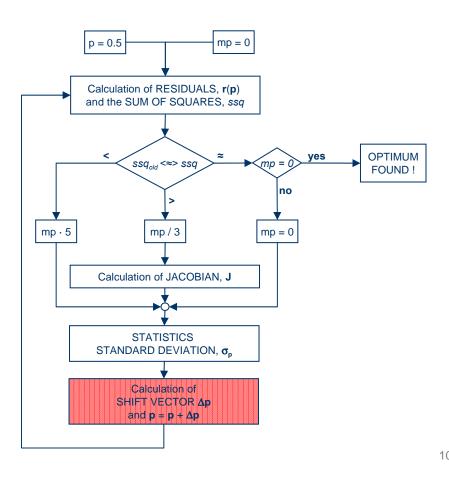
Current method:

Newton-Gauss method



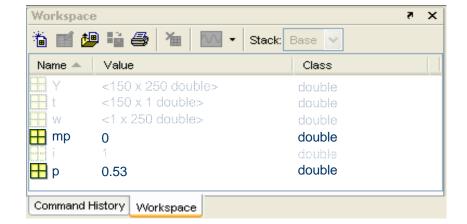


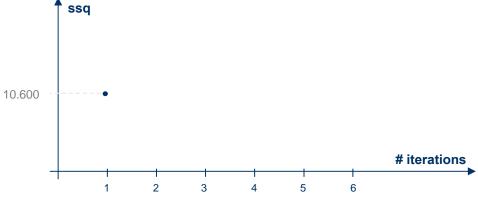




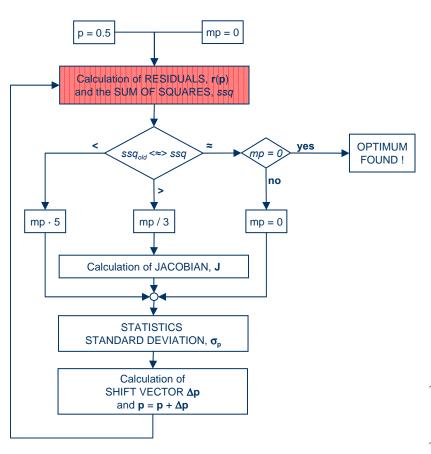
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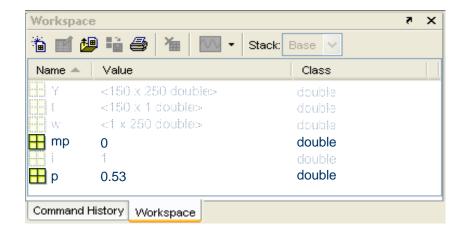
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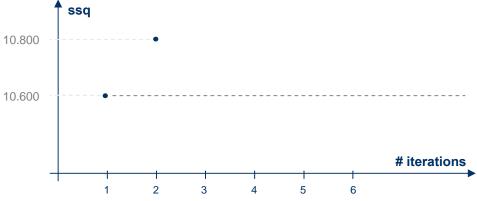




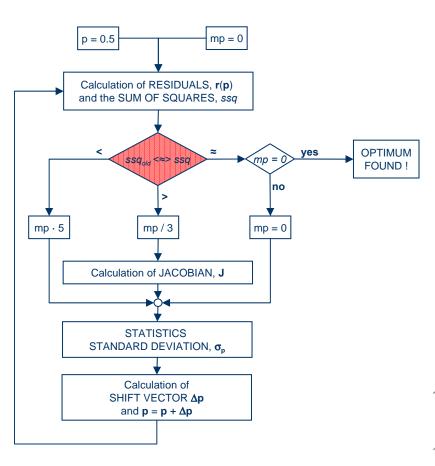


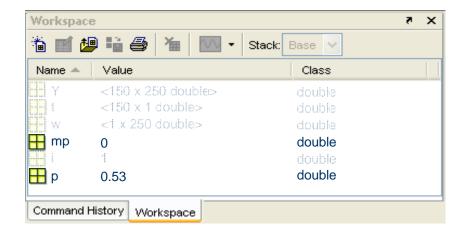


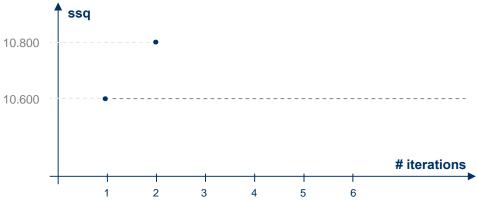




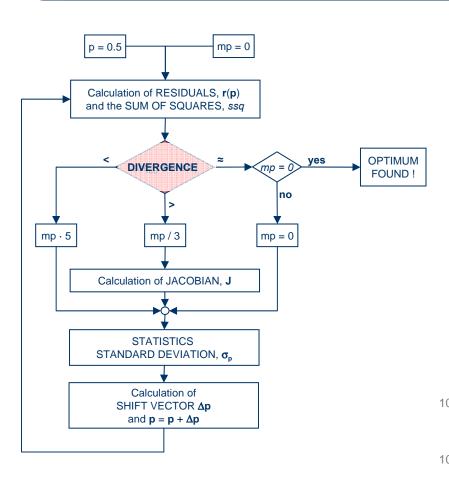


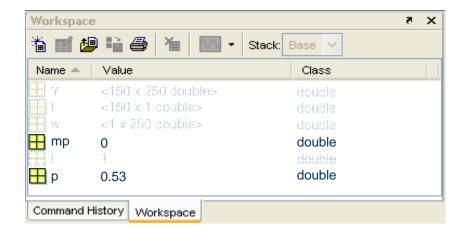


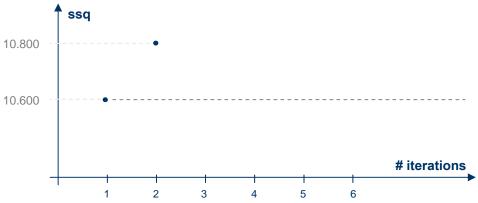




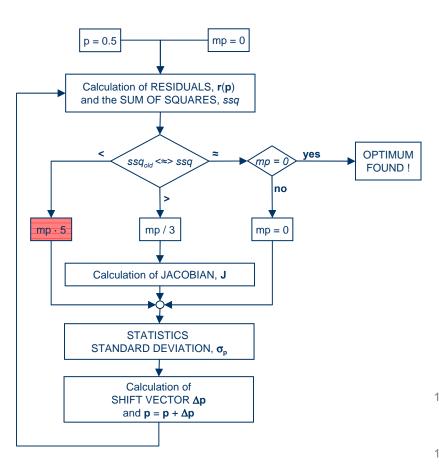


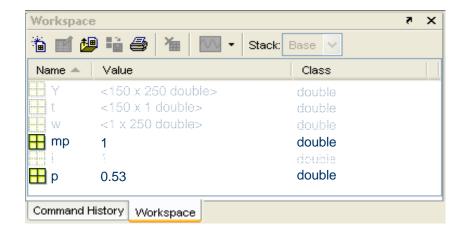


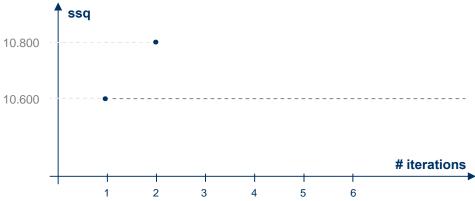




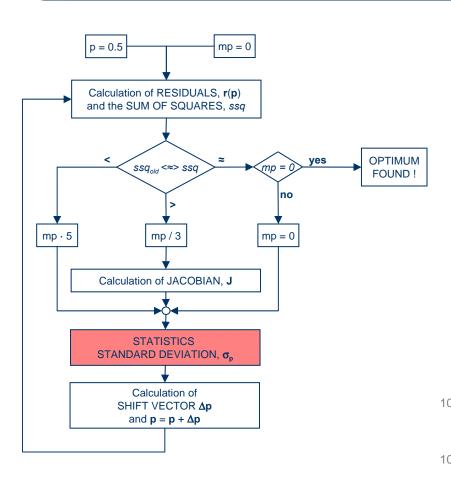


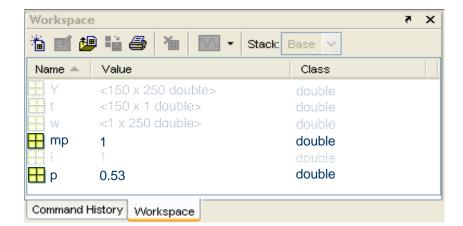


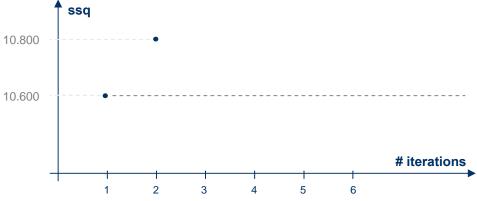




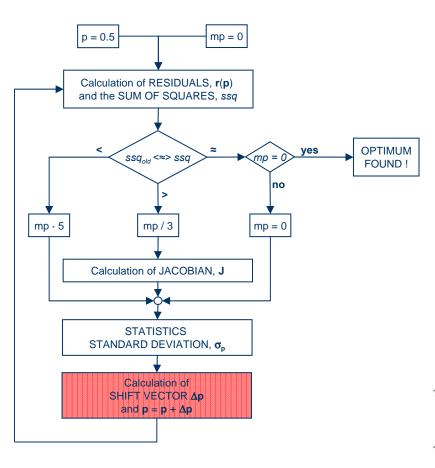






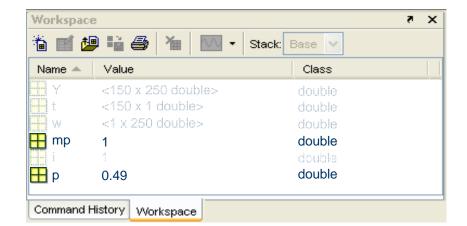


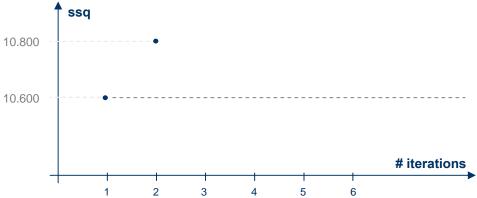




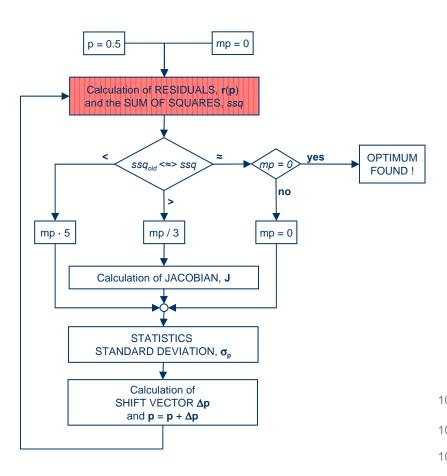
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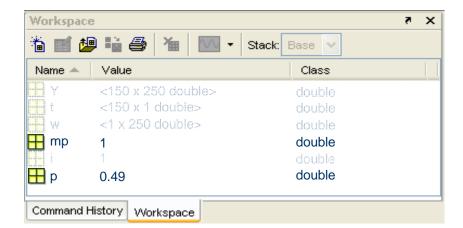
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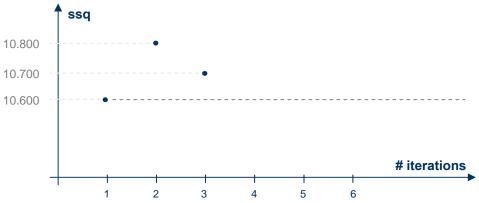




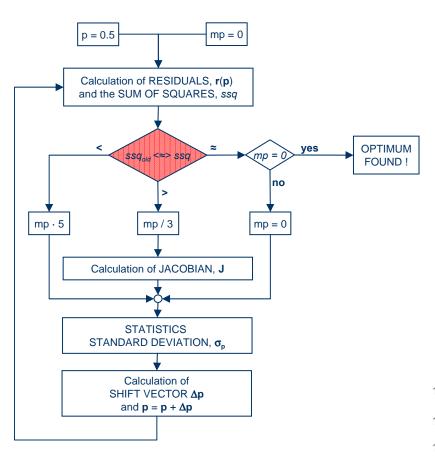


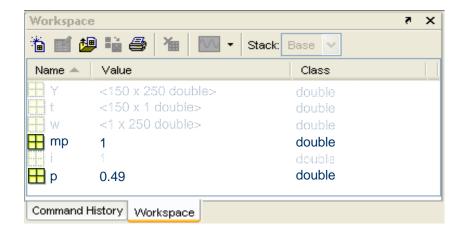


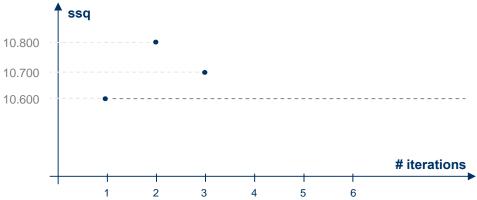




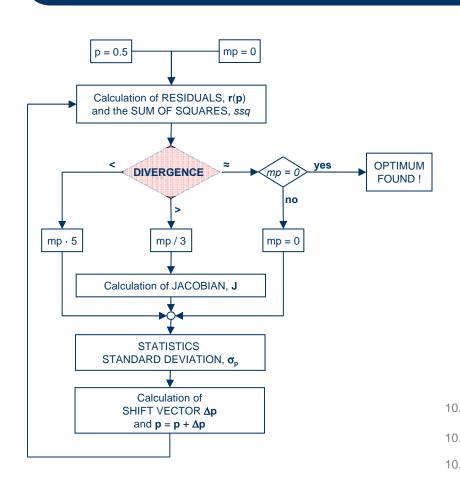


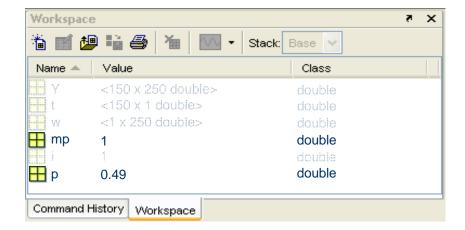


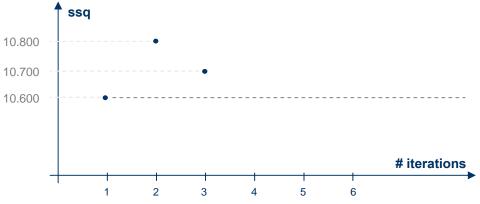




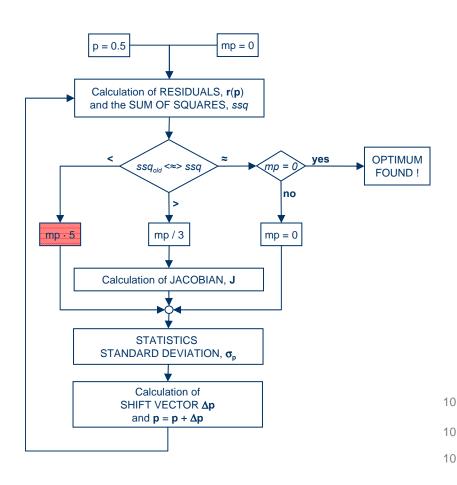


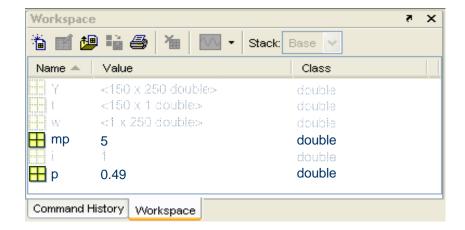


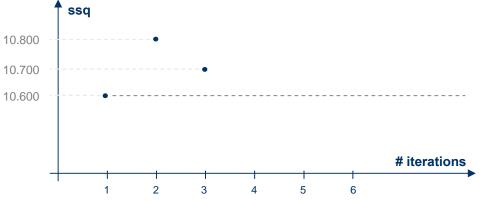




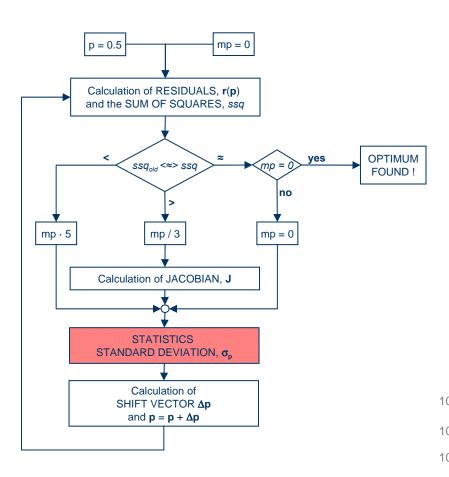


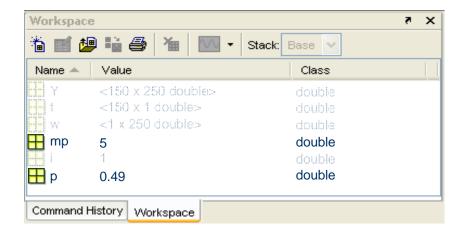


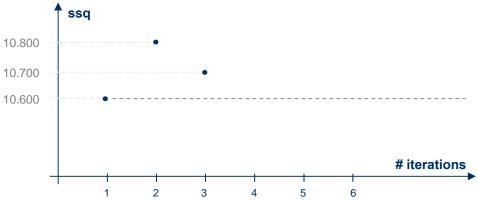




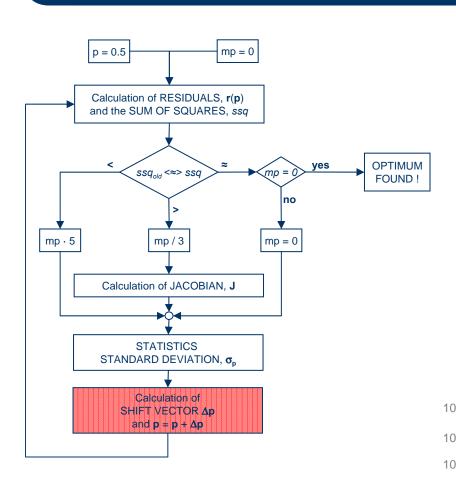


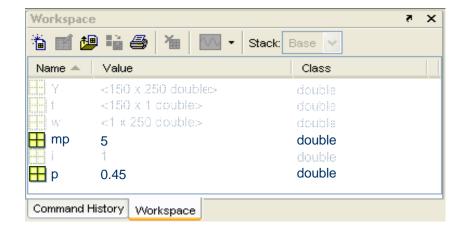


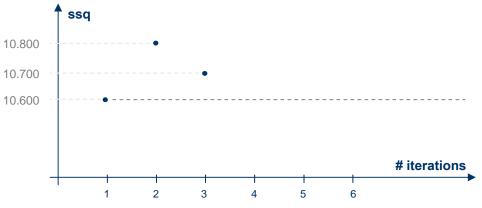




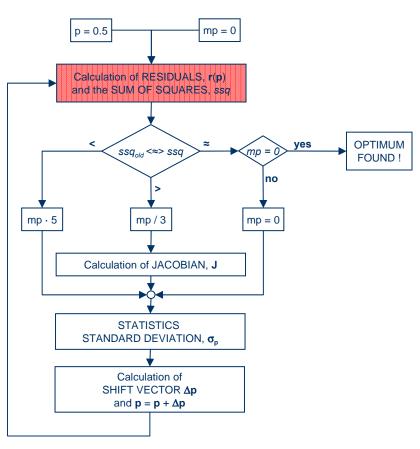


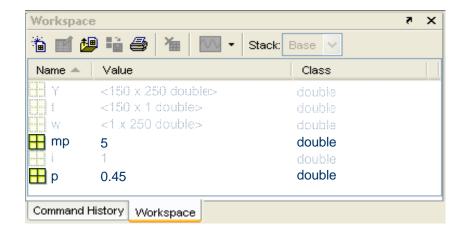


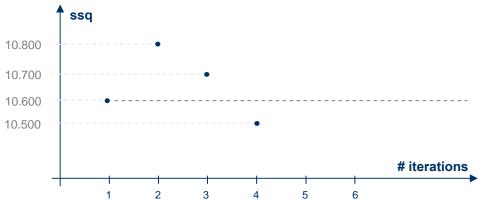




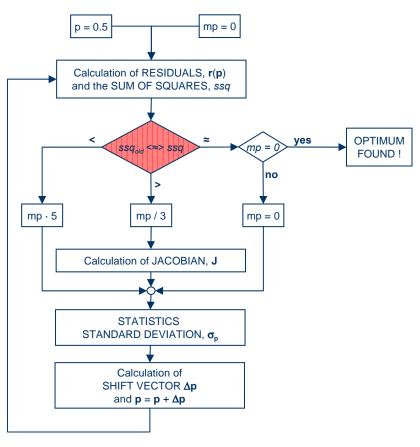


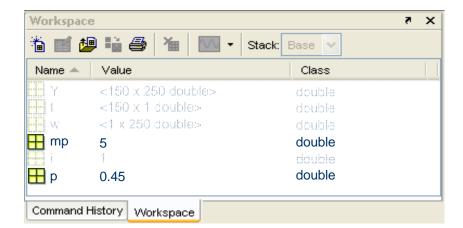


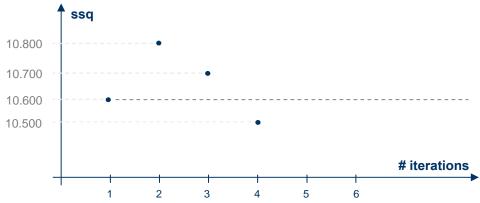




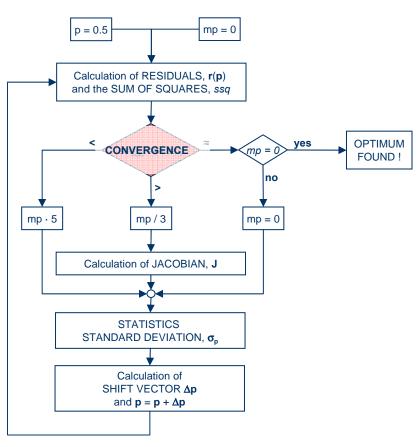


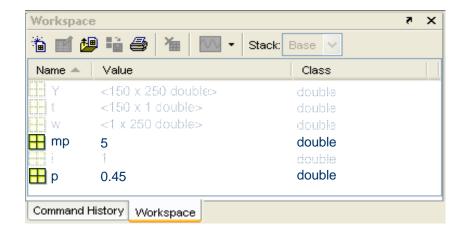


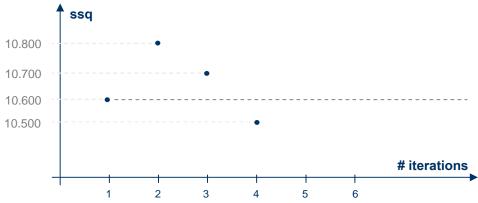




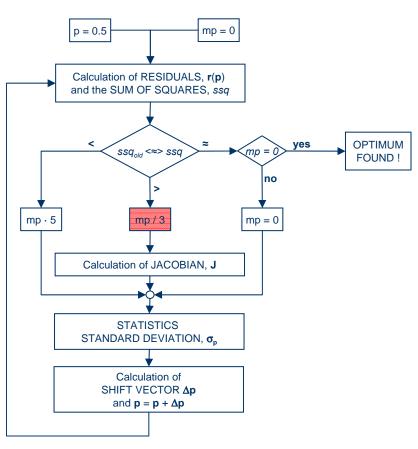


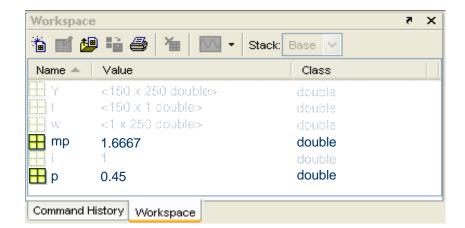


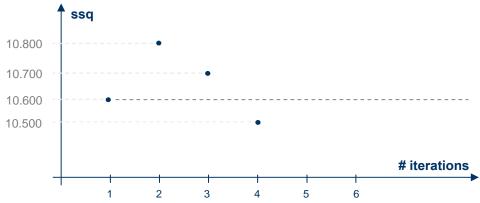




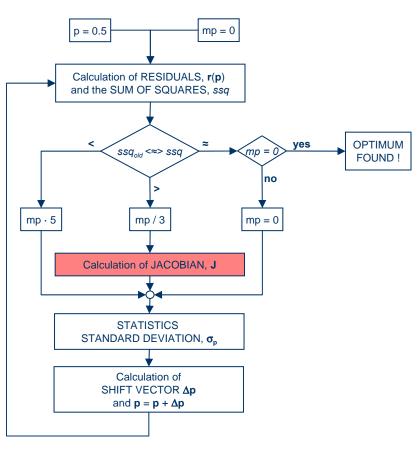


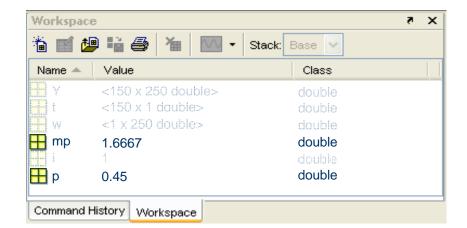


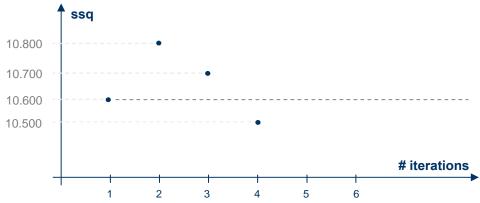




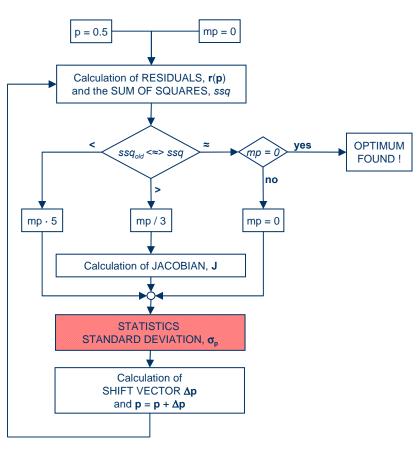


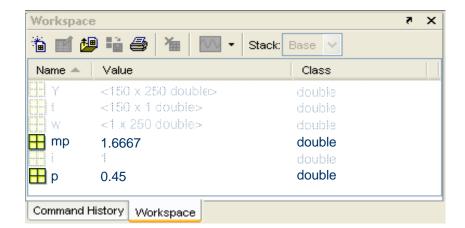


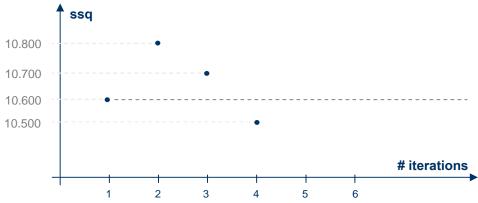




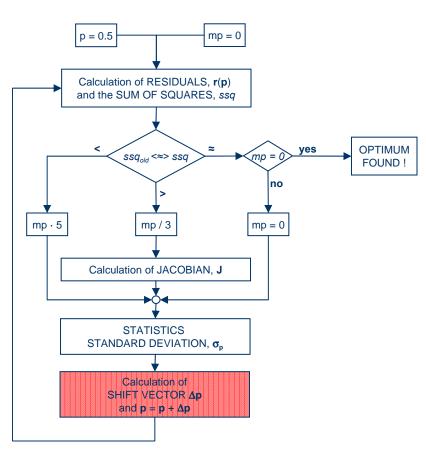




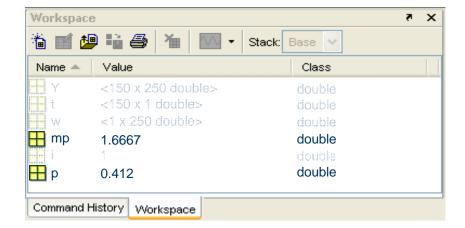


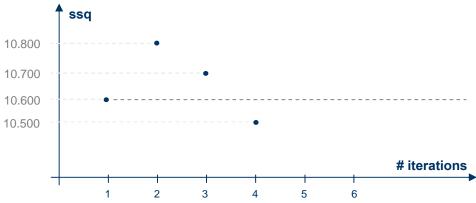




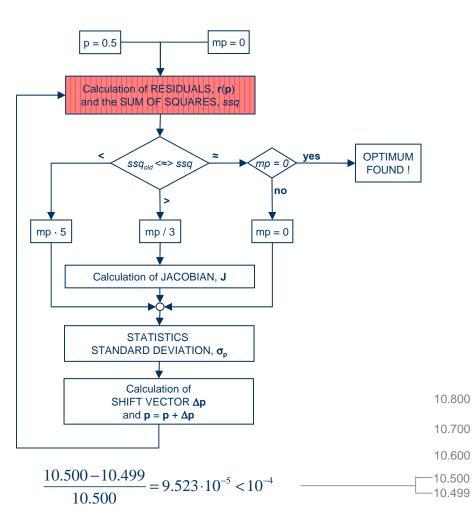


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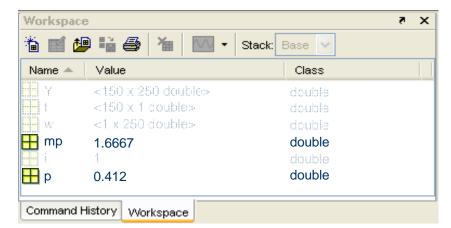


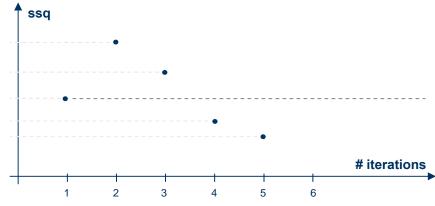




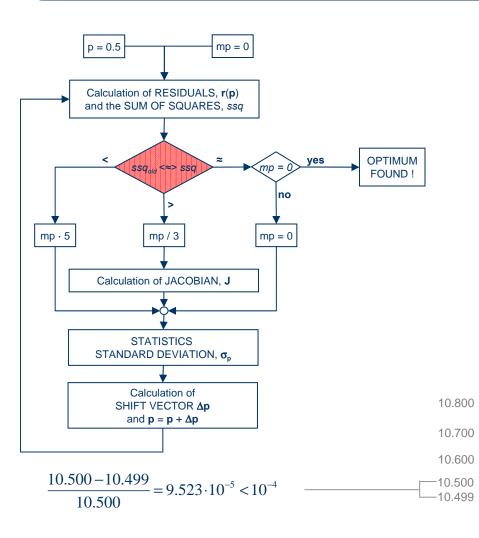


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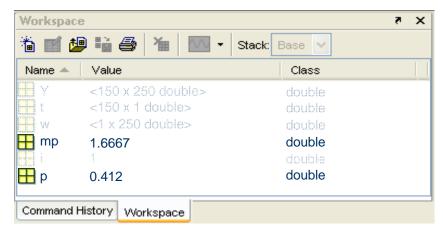


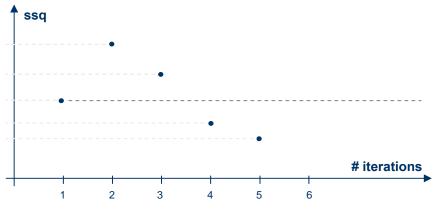




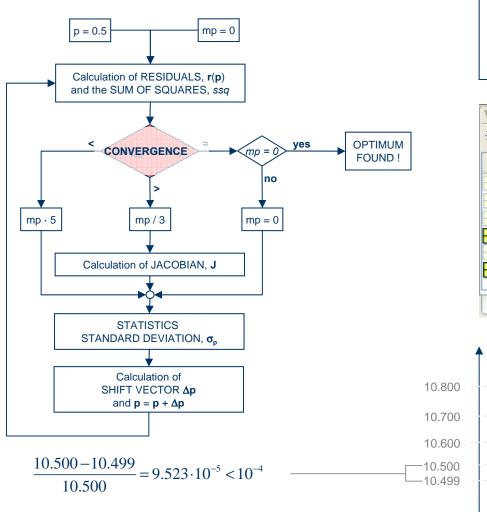


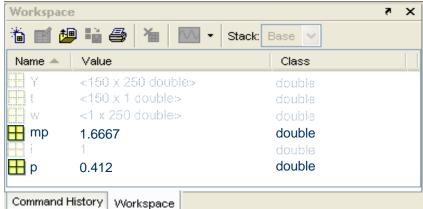
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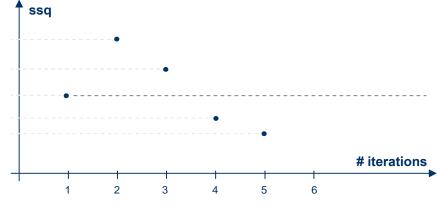




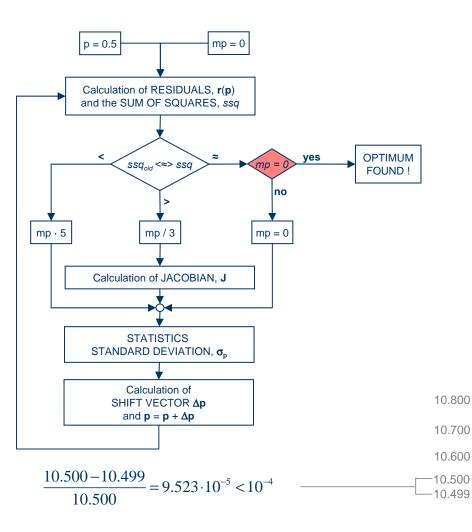




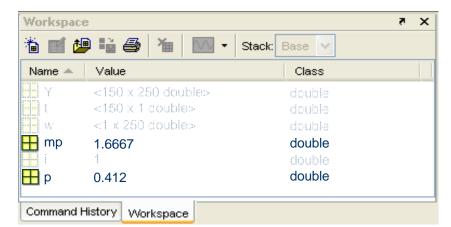


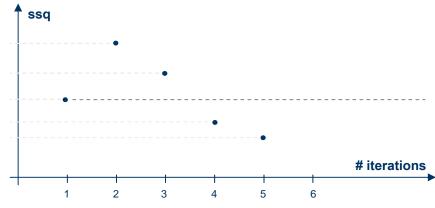




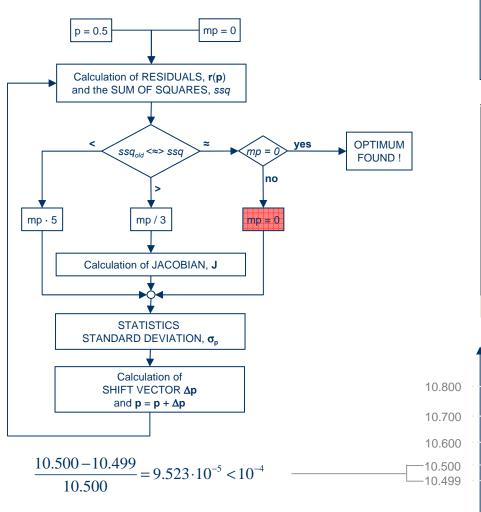


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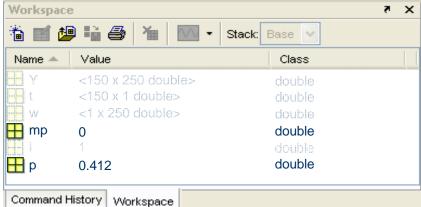


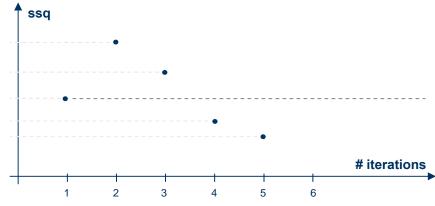




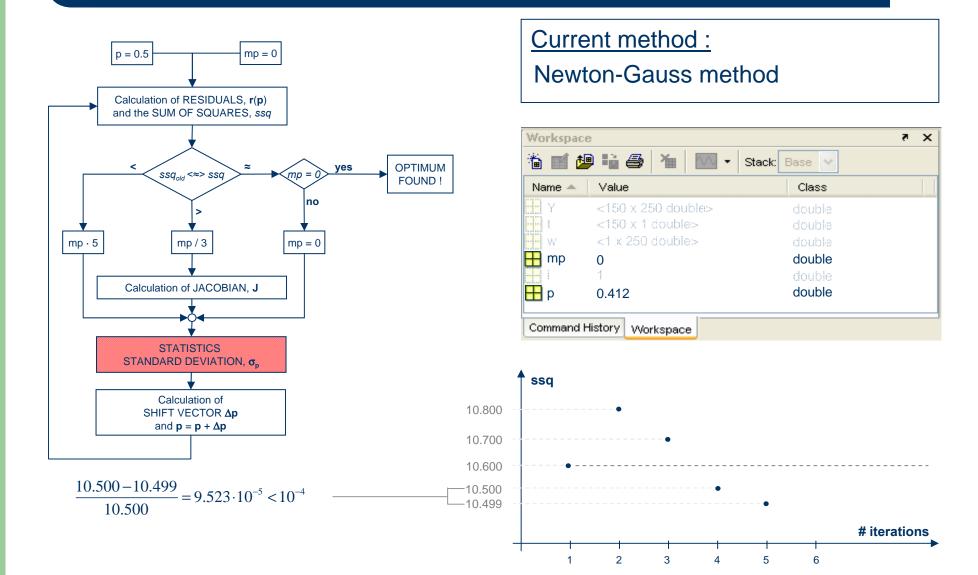


<u>Current method :</u> Newton-Gauss method

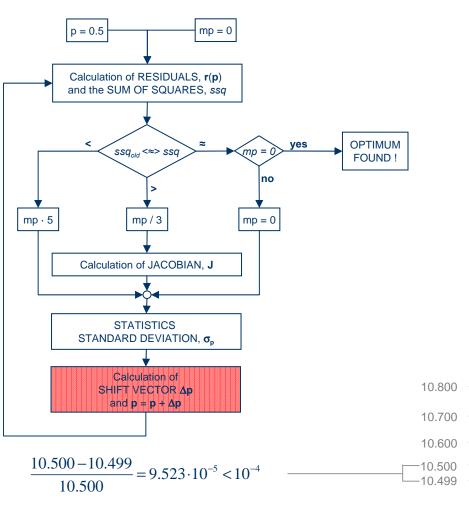






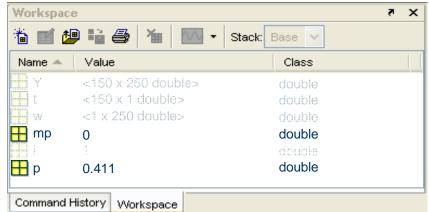


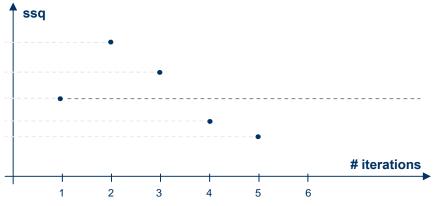




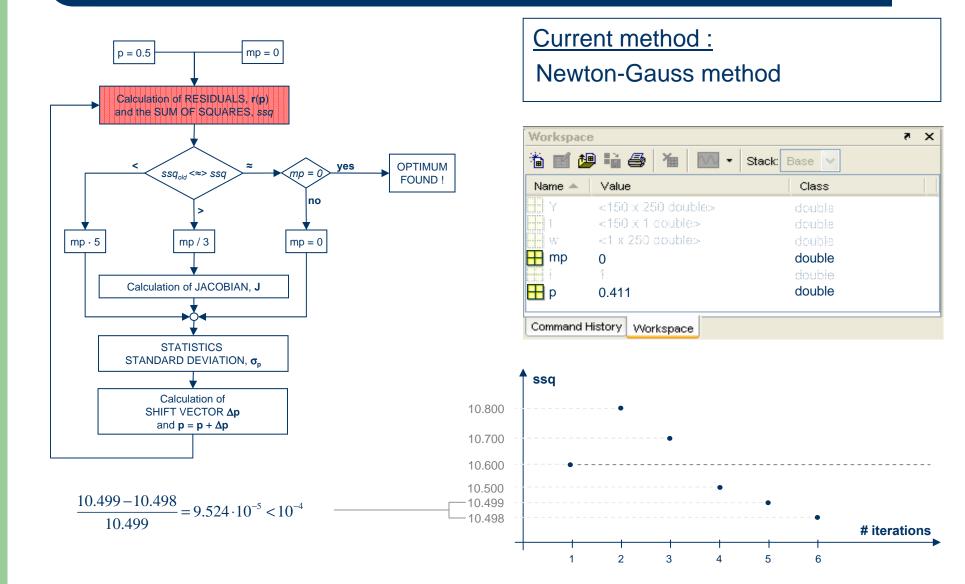
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Newton-Gauss method

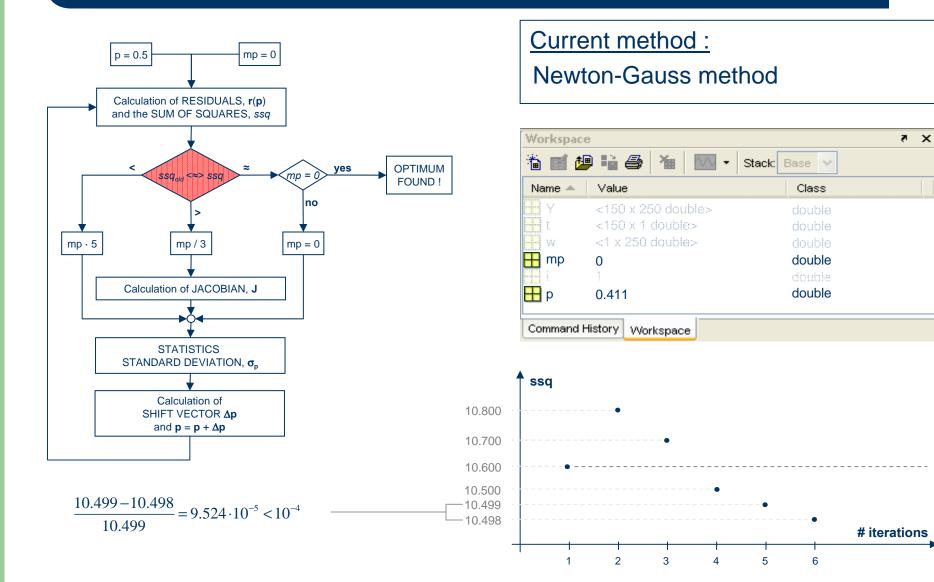




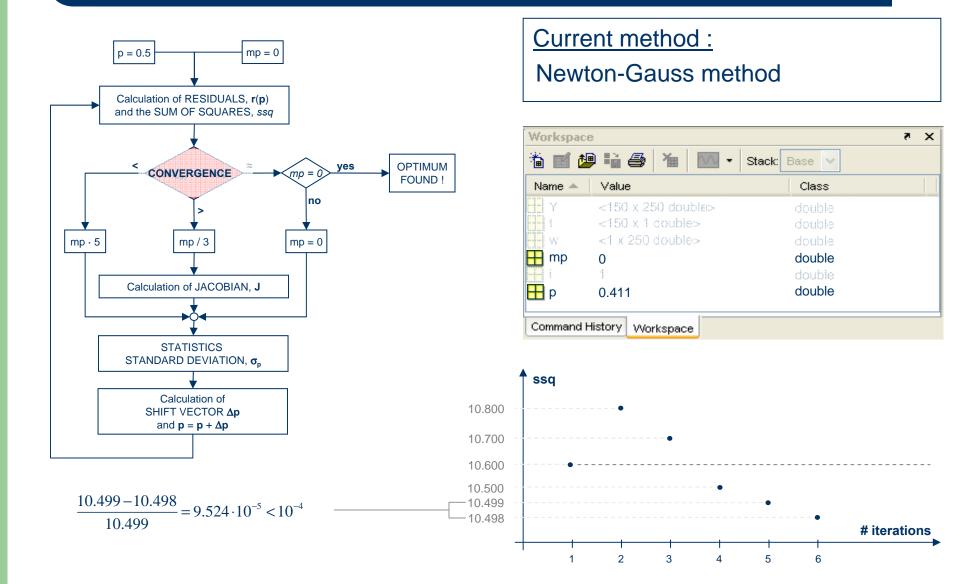




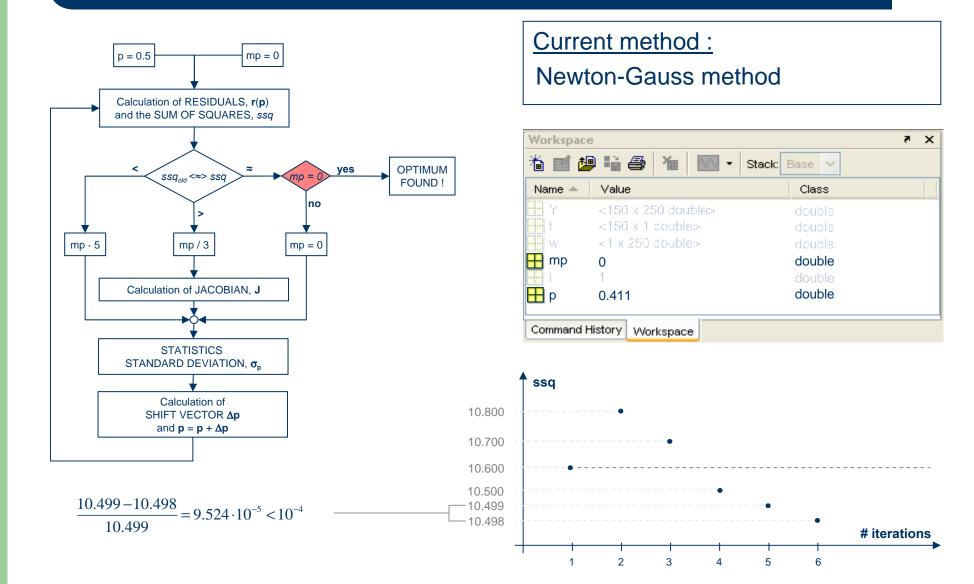




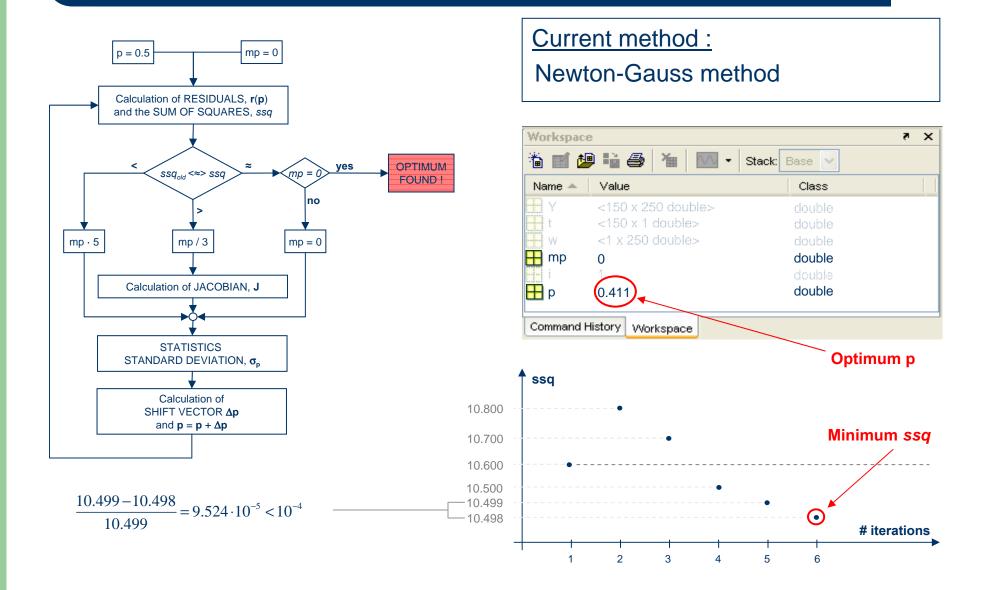








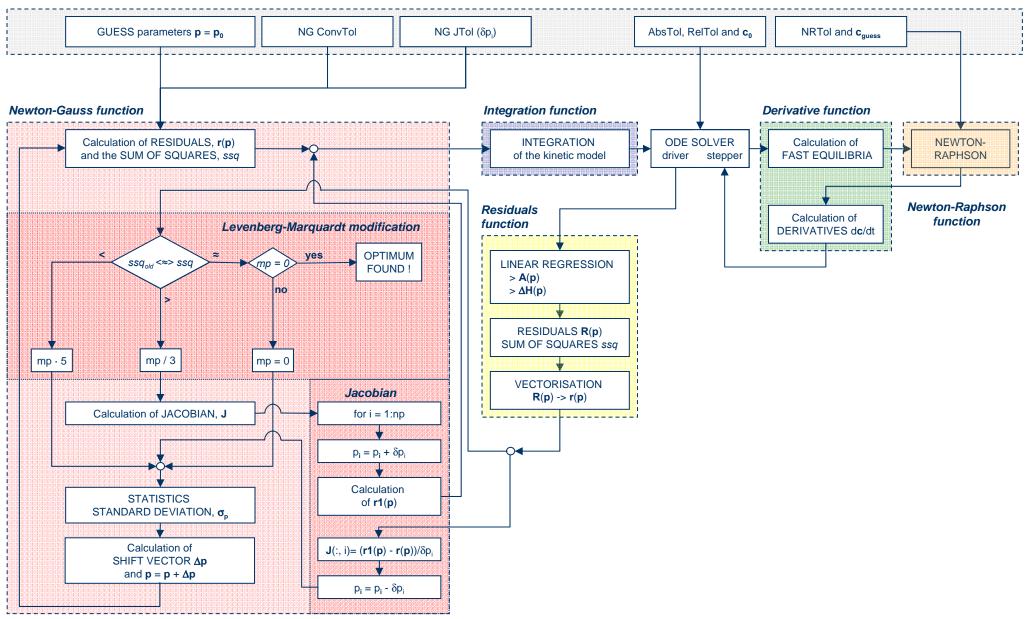




Kinetic modeling algorithm

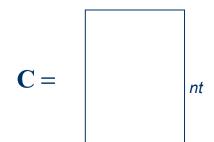


Settings





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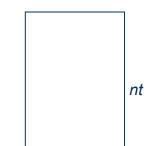


The maximum rank of C is:

$$|rank_{max}(\mathbf{C}) = \min(nt, nc)|$$



nc



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$$rank_{max}(\mathbf{C}) = \min(nt, nc)$$

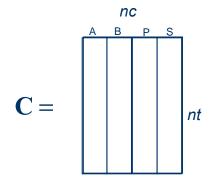
The pseudo inverse (\mathbf{C}^+) only exists if : $rank(\mathbf{C}) = rank_{max}(\mathbf{C})$



 $\mathit{rank}_{\mathit{max}}(\mathbf{C})$ columns or rows are linearly independant

-AL

Rank Deficiency of the concentration profile



The maximum rank of C is:

$$rank_{max}(\mathbf{C}) = \min(nt, nc)$$

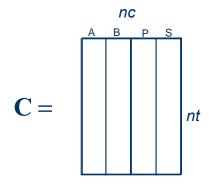
The pseudo inverse
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 \iff

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Example:
$$A + B \xrightarrow{k} P + S$$
 (in batch conditions)





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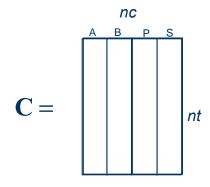


 $rank_{max}(\mathbf{C})$ columns or rows are linearly independent

Example:
$$A + B \xrightarrow{k} P + S$$
 (in batch conditions)

- Maximum possible rank?
- Number of independent species in stoichiometric conditions $(A_0 = B_0 = 1)$?
- And in non-stoichiometric conditions $(A_0 = 1, B_0 = 0.5)$?





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 \Leftrightarrow

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$$A + B \xrightarrow{k} P + S$$
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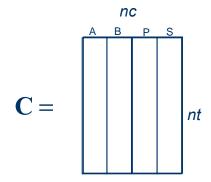
Maximum possible rank?

$$4 \text{ species } \Rightarrow \text{ rank}_{max}(\mathbb{C}) = 4$$

Number of independent species in stoichiometric conditions $(A_0 = B_0 = 1)$?

• And in non-stoichiometric conditions $(A_0 = 1, B_0 = 0.5)$?





The maximum rank of C is:

The pseudo inverse (\mathbf{C}^+) only exists if : $rank(\mathbf{C}) = rank_{max}(\mathbf{C})$



 $rank_{max}(\mathbf{C}) = \min(nt, nc)$

 $rank_{max}(\mathbf{C})$ columns or rows are linearly independent

Example: $A + B \xrightarrow{k} P + S$ (in batch conditions)

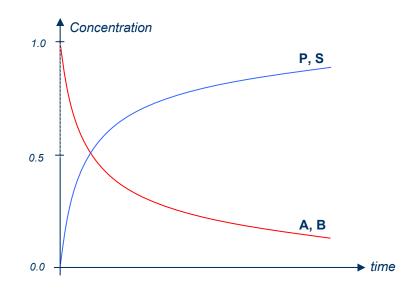
Maximum possible rank?

$$4 \text{ species } \Rightarrow \text{ rank}_{max}(\mathbb{C}) = 4$$

• Number of independent species in stoichiometric conditions $(A_0 = B_0 = 1)$?

$$rank(\mathbf{C}) = 2 \quad (only!)$$

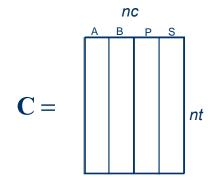
• And in non-stoichiometric conditions $(A_0 = 1, B_0 = 0.5)$?



[A]_t and [B]_t are identical [P]_t and [S]_t are identical

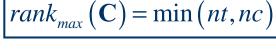






The maximum rank of C is:

The pseudo inverse
$$(\mathbf{C}^+)$$
 only exists if : $rank(\mathbf{C}) = rank_{max}(\mathbf{C})$



 $rank_{max}(\mathbf{C})$ columns or rows are linearly independent

$$\underline{\mathsf{Example}}: \quad A+B \xrightarrow{\ k \ } P+S \quad \left(in \ batch \ conditions\right)$$

Maximum possible rank?

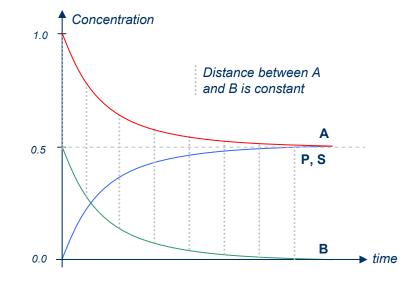
$$4 \text{ species } \Rightarrow \text{ rank}_{max}(\mathbf{C}) = 4$$

• Number of independent species in stoichiometric conditions $(A_0 = B_0 = 1)$?

$$rank(\mathbf{C}) = 2 \quad (only!)$$

• And in non-stoichiometric conditions $(A_0 = 1, B_0 = 0.5)$?

$$rank(\mathbf{C}) = 2 \quad (still!)$$



[A]_t and [B]_t disappear at the same rate $[P]_t$ and $[S]_t$ are identical

 \iff

1 species 1 species

2 independant species





- Model Reduction : set the dependant species as colorless (non-absorbing)
 - ⇒ Rates constants will be correct
 Absorption spectra will be wrong (mixed pure spectra)



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 Absorption spectra will be wrong (mixed pure spectra)
- Provide **Known Spectra**
- Work under Semi-Batch Conditions



Annihilation of Rank Deficiency

5 ways to break the rank deficiency:

- Model Reduction : set the dependant species as colorless (non-absorbing)
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- Use concentration dependant measurements (Second Order Global Analysis)



Annihilation of Rank Deficiency

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- Provide Known Spectra
- Work under Semi-Batch Conditions
- Use concentration dependant measurements (Second Order Global Analysis)
- Extend the wavelength-time domain to resolve linear dependencies (**Tri-linear Measurements**)

Example: Coupling chromatrography to UV



Annihilation of Rank Deficiency

5 ways to break the rank deficiency:

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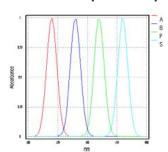
 Example: Couniethed is not addressed to UV

 This last highly complex because it is highly acomplex because it is highly acomplex.



Reduced model

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$

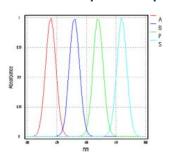




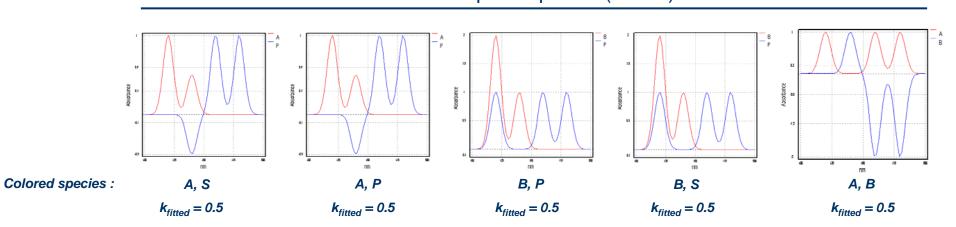
Reduced model

Simulated absorption spectra

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$



Fitted absorption spectra (mixed)

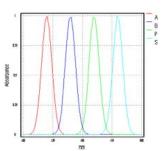




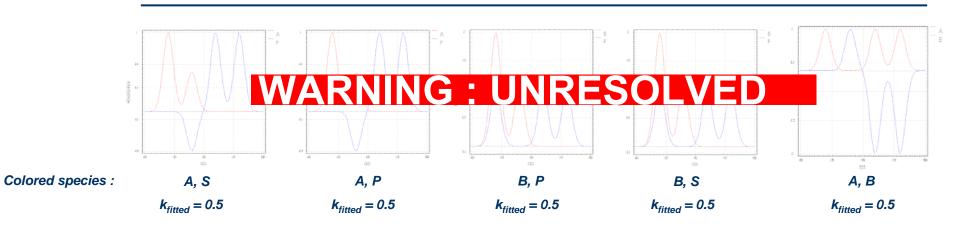
Reduced model

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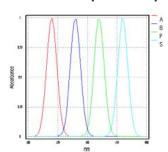


Fitted absorption spectra (mixed)





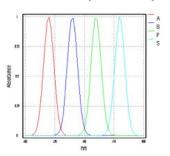
$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$





Simulated absorption spectra

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$

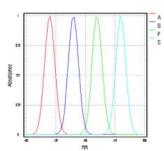


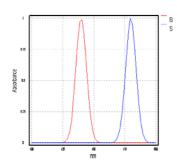
2 species are dependent



Simulated absorption spectra

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$





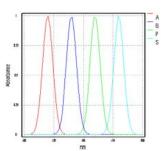
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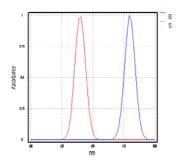
Let's provide 2 pure spectra : those of B and S



Simulated absorption spectra

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$





2 species are dependent

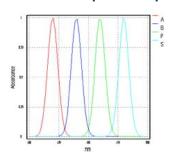
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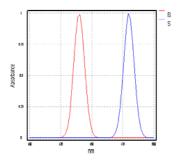
All species are set colored



Simulated absorption spectra

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$



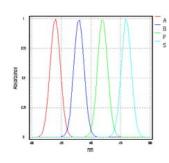


2 species are dependent

Let's provide 2 pure spectra : those of B and S

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Fitted absorption spectra:

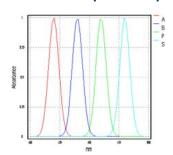


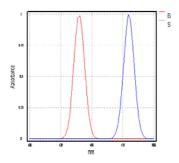
 $k_{\text{fitted}} = 0.5$



Simulated absorption spectra

$$A(1)+B(0.5) \xrightarrow{k=0.5} P+S$$



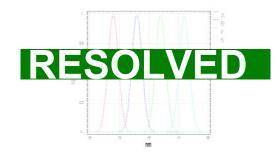


2 species are dependent

Let's provide 2 pure spectra : those of B and S

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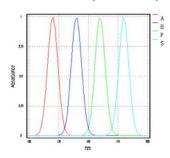
Fitted absorption spectra:



 $k_{\text{fitted}} = 0.5$



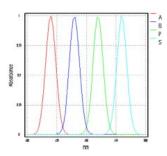
$$A+B \xrightarrow{k=0.5} P+S$$





$$A+B \xrightarrow{k=0.5} P+S$$

Dose A into B will break the rank deficiency between A and B but not between P and S !!!





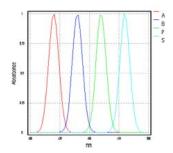
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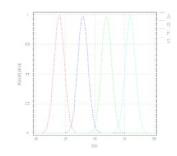
To break both rank deficiencies, one has to dose :

- A and P into B or
- A and S into B or
- B and P into A or
- B and S into A

Simulated absorption spectra



Fitted absorption spectra:



 $k_{\text{fitted}} = 0.5$



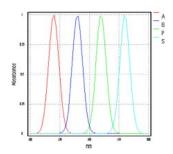
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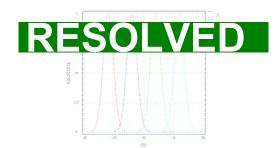
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Simulated absorption spectra



Fitted absorption spectra:



 $k_{\text{fitted}} = 0.5$



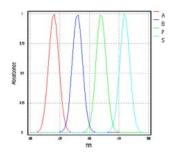
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Dose A into B will break the rank deficiency between A and B but not between P and S !!!

To break both rank deficiencies, one has to dose :

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Simulated absorption spectra



Fitted absorption spectra:

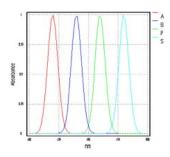


 $k_{\text{fitted}} = 0.5$

NB: in practice, one dose A in B or B in A and set one of the two products (P or S) as uncolored. In such case, one spectrum of the two products is unresolved



$$A+B \xrightarrow{k=0.5} P+S$$

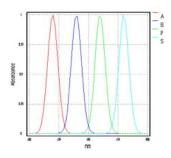




$$A+B \xrightarrow{k=0.5} P+S$$

Let's make 3 Concentration dependent measurements

	A ₀	B ₀		
# 1	1	1		
# 2	0.5	1		
# 3	1	0.5		





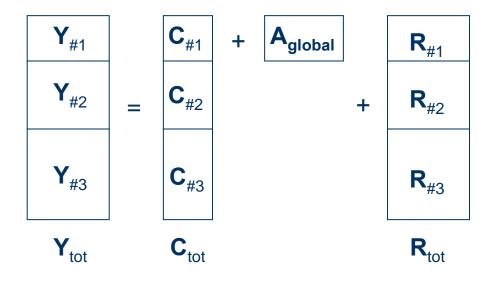
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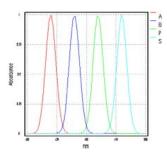
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Hypothesis of Global Spectra:

The 3 sets of experiment share the same pure spectra







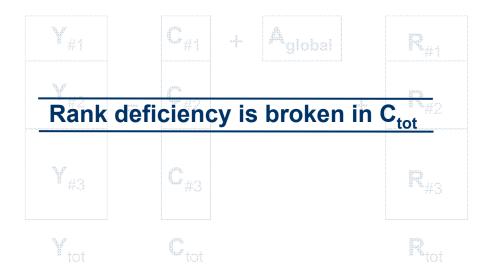
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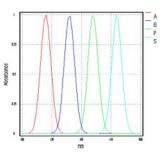
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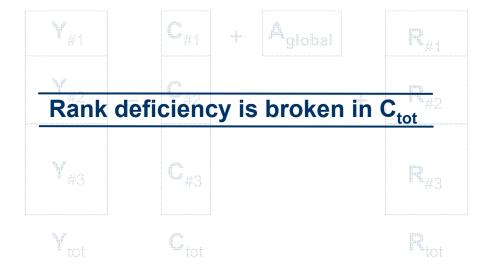
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Let's make 3 Concentration dependent measurements

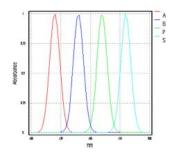
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Hypothesis of Global Spectra :

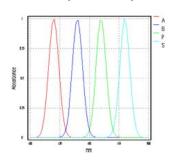
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Simulated absorption spectra



Fitted absorption spectra:



$$k_{titted} = 0.5$$



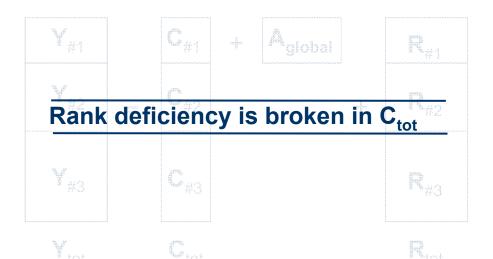
$$A + B \xrightarrow{k=0.5} P + S$$

Let's make 3 Concentration dependent measurements

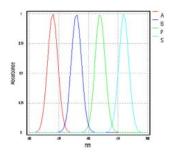
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Hypothesis of Global Spectra:

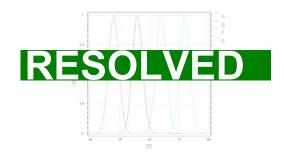
The 3 sets of experiment share the same pure spectra



Simulated absorption spectra



Fitted absorption spectra:



$$k_{\text{fitted}} = 0.5$$



End of the Tutorial

That is « already » the end of this Tutorial

Thank you for your attention!



Case study overview

The aims of these case studies are:

- Identify the number of detectable species
- Know the phenomenon of parameter interchange
- Identify and break rank deficiency
- Use residuals for model validation

Using the following techniques:

- PCA
- EFA
- ALS
- Hard-modeling

On simulated data from different types:

- Spectroscopy
- Calorimetry

Under batch and semi-batch conditions

$$\bullet A \xrightarrow{k=0.5} P$$

$$\bullet A \xrightarrow{k_1=0.5} B \xrightarrow{k_2=0.3} P$$

•
$$A + B \xrightarrow{k=0.5} P$$

•
$$A + B(dosed) \xrightarrow{k=0.5} P$$

•
$$A + B(dosed) \xrightarrow{k_1=10} C$$

 $B(dosed) + C \xrightarrow{k_2=5} P$



Mechanism : $A \xrightarrow{k=0.5} P$

Signal : Spectroscopy

Process : Batch

Conversion: 99%

PCA/EFA : 2 species ⇒ Full rank

ALS : Easily resolved

with non-negativity constraint

Hard-modeling : k does not depend on c₀(A) for a 1st order reaction



Mechanism : $A \xrightarrow{k=0.5} P$

Signal : Spectroscopy

Process : Batch

Conversion: 63%

PCA/EFA : 2 species ⇒ Full rank

ALS : Resolved under constraints

with non-negativity constraint and known spectrum of P

• Hard-modeling : k does not depend on $c_0(A)$ for a 1st order reaction



Mechanism : $A \xrightarrow{k=0.5} P$

Signal : Calorimetry

Process : Batch

Conversion: 99%

PCA/EFA/ALS : NA

Hard-modeling : k does not depend on c₀(A)

for a 1st order reaction



Mechanism : $A + B \xrightarrow{k=0.5} P$

Signal : Spectroscopy

Process : Batch

Fitted mechanism: $A \longrightarrow P$

PCA/EFA : 2 species ⇒ Full rank

ALS : Apparently resolved under constraints

with non-negativity constraint and known spectrum of P

Hard-modeling : 1st order mechanism is wrong!



Mechanism : $A \xrightarrow{k_1=0.5} B \xrightarrow{k_2=0.3} P$

Signal : Spectroscopy

Process : Batch

Conversion: 99%

PCA/EFA : 3 species ⇒ Full rank

ALS : Resolved under constraints
 with non-negativity constraint and known spectrum of B

Hard-modeling : Parameter interchange
 k₁ and k₂ swap depending on the initial guess



Mechanism : $A \xrightarrow{k_1=0.5} B \xrightarrow{k_2=0.3} P$

Signal : Spectroscopy

Process : Batch

Conversion: 77%

PCA/EFA : 3 species ⇒ Full rank

ALS : Hardly resolved

with non-negativity constraint and known spectrum of B and P

• Hard-modeling : Parameter interchange

 k_1 and k_2 swap depending on the initial guess



Mechanism : $A \xrightarrow{k_1=0.5} B \xrightarrow{k_2=0.3} P$

Signal : Calorimetry

Process : Batch

Conversion: 99%

PCA/EFA/ALS : NA

Hard-modeling : 1. Less robust than multivariate fitting

2. Parameter interchange



Mechanism : $A \xrightarrow{k_1=0.5} B \xrightarrow{k_2=0.3} P$

Signal : Spectroscopy

Process : Batch

Fitting : Univariate ($\lambda = 400$)

PCA/EFA/ALS : NA

Hard-modeling : 1. Less robust than multivariate fitting

2. Parameter interchange



Mechanism : $A \xrightarrow{k_1=0.5} B \xrightarrow{k_2=0.3} P$

Signal : Spectroscopy

Fitting : Univariate ($\lambda = 400$)

Fitted mechanism: $A \longrightarrow P$

PCA/EFA/ALS : NA

Hard-modeling : 1. Less robust than multivariate fitting

2. Parameter interchange

3. Structured residuals

⇒ The model is slightly wrong but hard to validate at this single wavelength



Mechanism : $A + B \xrightarrow{k=0.5} P$

Signal : Spectroscopy

Process : Batch

Colored species: A and P (model reduction)

PCA/EFA : 2 species ⇒ Rank deficiency

• ALS : NA

Hard-modeling : Species B set as non-absorbing

 \Rightarrow 1. k is correct

2. The fitted pure spectra are wrong (linear combinations of the true pure spectra)



Mechanism : $A+B \xrightarrow{k=0.5} P$

Signal : Spectroscopy

Process : Batch

Known spectrum : Species B

PCA/EFA : 2 species ⇒ Rank deficiency

• ALS : NA

Hard-modeling : The pure spectrum of B is provided

 \Rightarrow 1. k is correct

2. The fitted pure spectra are resolved



Mechanism : $A + B(dosed) \xrightarrow{k=0.5} P$

Signal : Spectroscopy

Process : Semibatch

Conversion: 68%

PCA/EFA : 3 species ⇒ Full rank

ALS : Resolved under strong constraints

non-negativity constraint and known spectrum of B and P!

• Hard-modeling : The pure spectra are resolved



Mechanism : $A + B(dosed) \xrightarrow{k=0.5} P$

Signal : Calorimetry

Process : Semibatch

Conversion: 68%

PCA/EFA/ALS : NA

 Hard-modeling : Fitting calorimetric data is more robust in semibatch than in batch conditions!



Mechanism :
$$A + B(dosed) \xrightarrow{k_1=10} C$$

$$B(dosed) + C \xrightarrow{k_2=5} P$$

Signal : Spectroscopy

Process : Semibatch

PCA/EFA : 4 species ⇒ Full rank

ALS
 : Resolved under very strong constraints
 non-negativity constraint and known spectrum of B, C and P!

Hard-modeling : The pure spectra are resolved



Mechanism : $A + B(dosed) \xrightarrow{k_1=10} C$

 $B(dosed) + C \xrightarrow{k_2=5} P$

Signal : Calorimetry

Process : Semibatch

PCA/EFA/ALS : NA

Hard-modeling : Fitting calorimetric data conditions is

more robust in semibatch than

in batch conditions!



Summary on the Case studies (1)

PCA/EFA

 These two techniques provide information on the number of observable species and therefore the maximum rank of Y

ALS

- Non-negativity constraint alone only resolves $A \rightarrow P$
- Pure spectra of the products are required if they are not fully formed
- Pure spectra of the intermediates are generally required for complete resolution
- Without a priori knowledge on mechanisms and/or spectra, rank deficiency is undetectable



Summary on the Case studies (2)

HARD-MODELING

BATCH CONDITIONS

- Multivariate fitting of spectrocopy data is more reliable than univariate fitting
- Fitting of calorimetric data is not very stable in batch conditions
- Rank deficiency due to the model can be easily broken by :
 - Model reduction (some species are set non-absorbing)
 Fitted pure spectra are wrong (linear combination of the true ones)
 but nonlinear parameters are correct!
 - Known spectra provided
 Fitted pure spectra and nonlinear parameters are in this case both correct

SEMIBATCH CONDITIONS

- Fitting of calorimetric data is more robust in semibatch conditions
- The dosing completely breaks simple rank deficient problems and partially highly complex mechanisms (eg. 2 intermediates, 2 products ...)

FIRST ORDER MECHANISMS

 With 1st order mechanisms, rates are independent on initial concentrations and rate constants can swap without differences in fitting (*Parameter Interchange*)



Appendix 1: List of the Matlab files

#	Simulated Mechanism	Fitted mechanism	Process	Model rank	Rank deficiency	Conversion	Fitted signal	Fitting	PCA / EFA	ALS	Hard-modeling	File
1	A -> P	same	Batch	2	No	99.3%	Spec	Multivariate	2	[>0]	C ₀ (A) = 1 and 10	main_AtoP_X99
2	A -> P	same	Batch	2	No	63.2%	Spec	Multivariate	2	[>0,P]	NA	main_AtoP_X60
3	A -> P	same	Batch	2	No	99.3%	Cal	Univariate	NA	NA	NA	main_AtoP_cal
4	A + B -> P	A -> P	Batch	2	Yes	90.9%	Spec	Multivariate	2	NA	Structured residuals	main_ApBtoP_1st_order
5	A -> B -> P	same	Batch	3	No	99.9%	Spec	Multivariate	3	[> 0 , B]	Swap of k's	main_AtoBtoP_X99
6	A -> B -> P	same	Batch	3	No	77.7%	Spec	Multivariate	3	[>0,B,P]	NA	main_AtoBtoP_X75
7	A -> B -> P	same	Batch	3	No	99.9%	Cal	Univariate	NA	NA	Less robust than Case 5	main_AtoBtoP_cal
8	A -> B -> P	same	Batch	3	No	99.9%	Spec	Univariate	NA	NA	Less robust than Case 5	main_AtoBtoP_univar1
9	A -> B -> P	A -> B	Batch	3	No	99.9%	Spec	Univariate	NA	NA	Structure in the residuals	main_AtoBtoP_univar2
10	A + B -> P	same	Batch	2	Yes	90.9%	Spec	Multivariate	2	NA	B not absorbing	main_ApBtoP_batch
11	A + B -> P	same	Batch	2	Yes	90.9%	Spec	Multivariate	2	NA	Pure spectrum of B provided	main_ApBtoP_batch_Bknown
12	A + B(dosed) -> P	same	Semibatch	3	No	68.2%	Spec	Multivariate	3	[>0,B,P]	NA	main_ApBtoP_semi_Y
13	A + B(dosed) -> P	same	Semibatch	3	No	68.2%	Cal	Univariate	3	NA	NA	main_ApBtoP_semi_cal
14	A + B(dosed) -> C B(dosed) + C -> P	same	Semibatch	4	No	99.8%	Spec	Multivariate	4	[>0,B,C,P]	NA	main_ApBtoC_BpCtoP_semi_Y
15	A + B(dosed) -> C B(dosed) + C -> P	same	Semibatch	4	No	99.8%	Cal	Univariate	4	NA	NA	main_ApBtoC_BpCtoP_semi_cal