Co-production of Hydrogen and Electricity from Lignocellulosic Biomass: Process Design and Thermo-economic Optimization

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Abstract:
The thermochemical production of hydrogen from lignocellulosic biomass is systematically analyzed by developing environomic models combining thermodynamics with economic analysis, process integration techniques and optimization strategies for the conceptual process design. H_2 is produced by biomass gasification and subsequent gas treatment by reforming, water gas shift and cold gas cleaning, followed by H_2 purification by CO_2 removal. It is shown how the overall efficiency is improved by including process integration computing the optimal utility integration to allow waste heat valorization and combined production of heat and power. In the conversion process, electricity can be generated in steam and gas turbine cycles using the combustion of the off-gases and a Rankine cycle recovering available process heat. Additional electricity can be produced by burning part of the H_2 -rich intermediate or of the purified H_2 product. The trade-off between H_2 and electricity co-production and H_2 or electricity only generation is assessed with regard to energy, economic and environmental considerations. Based on multi-objective optimization the most promising options for the poly-generation of H_2, power and heat are identified with regard to different process configurations and operating conditions. The best compromise between efficiency, H_2 and/or electricity production cost and CO_2 capture is identified for competitive processes. In a future sustainable energy system biomass based H_2 and electricity reveal to be a competitive alternative.

Keywords:
Biomass, Hydrogen, Polygeneration, Process integration, Thermo-economic optimization.

1. Introduction

In a future clean and abundant energy system, hydrogen is to be considered as an alternative energy carrier. H_2 is a clean fuel that can be used in combustion engines and fuel cells for electricity generation without CO_2 emissions. Being a secondary form of energy, H_2 does not freely exist in nature and consequently has to be manufactured. Today H_2 is produced essentially by steam methane reforming, coal gasification and in a lesser extent by water electrolysis [1–3]. The drawback of these processes is that they are using fossil fuels or electricity from non-renewable sources. Within the worldwide challenge of global warming mitigation and energy supply, alternative H_2 production processes from renewable resources have received considerable attention. Different renewable processes are practical using wind, biomass or solar energy [1, 3]. Biomass-based technologies have a high potential because they emit no or very few net CO_2 emissions, if carefully managed, since the released CO_2 was previously absorbed and fixed by photosynthesis. H_2 production from biomass can be divided into two categories; thermo-chemical processes (i.e. biomass gasification and pyrolysis) and biological processes (i.e. biophotolysis and fermentation). An overview of these H_2 production processes from fossil and renewable resources and its economics can be found in [2].

The economic surveys in [2, 4] among with other studies assessing the energy and exergy efficiency of the biomass conversion into H_2, as well as the influence of operating conditions, show that it is a technical feasible process that could be promising on the future energy market [5–11]. H_2 yields in the range of 80-130$g_{H2}/kg_{Biomass}$ are assessed in [9, 10]. Energy efficiencies between 51 and 60% on lower heating value basis and H_2 production cost ranging from 29 to over 40 \$/MWh_{H2} are computed for biomass based H_2 processes in [5]. The performance of some H_2 processes using fossil or renewable resources are compared in Table 1.

Table 1: Reference H_2 production plants performance.

Process	CO_2 capture [%]	ϵ [%]	COE [\$/MWh_{H2}]	Ref.
Natural gas	0	75	18.9	[12]
Natural gas	71	71	20.2	[12]
Coal (Texaco gasif.)	0	63.7 (HHV)	31.6	[2]
Coal (Texaco gasif.)	87	59 (HHV)	37.8	[2]
Biomass (FICFB, CGC)	-	57.7	-	[10]
Biomass	-	51-60	29-40	[5]

Instead of producing H_2 from biomass, electricity can be generated in an integrated biomass gasification combined cycle (IBGCC) [13] . Even if there are still some technology challenges, this option contributing to the CO_2 emissions reduction is promising compared to other power plants with CO_2 capture using fossil fuels as shown by the performances in Table 2. Carbon capture decreases the efficiency of power plants by around 10% points and increases the electricity cost by nearly one third which yields CO_2 avoidance cost in the range of 13-75\$/t $CO_{2,avoided}$ [14]. Another alternative are polygeneration processes co-producing H_2 and electricity.

Table 2: Reference power plants performance without and with CO_2 capture.

Type	CO_2 capture [%]	ϵ [%]	gCO_2/kWh_e	COE [\$/MWh_e]	\$/t $CO_{2,avoided}$	Ref.
PC	0	41-45	736-811	43-52	-	[14]
PC -CC	85-90	30-35	92-145	62-86	29-51	[14]
IGCC	0	38-47	682-846	41-61	-	[14]
IGCC -CC	85-90	31-40	65-152	54-79	13-57	[14]
NGCC	0	55-58	344-379	31-50	-	[14]
NGCC -CC	85-90	47-50	40-66	43-72	37-74	[14]
IBGCC	0	37(HHV)	-	67.5	-	[15]
IBGCC -CC	80	33.94	178	-	-	[13]

In most of these studies no detailed energy integration is included for maximum heat recovery and valorization. In this paper the thermochemical conversion of biomass into H_2 and electricity will be investigated and optimized with regard to energy, economic and environmental considerations by applying a consistent methodology [16, 17] combining thermodynamics with economic analysis, process integration techniques and optimization strategies for the conceptual process design. The objective is to assess the competition between hydrogen or electricity only production processes and polygeneration with and without CO_2 capture by studying the influence of operating conditions and process configurations. It is focused on the potential process performance improvement by energy recovery and heat valorization for the polygeneration of H_2, heat and power and captured CO_2.

2. Methodology

This paper follows a previously developed methodology for the optimal thermo-economic process design of liquid and gaseous fuel production from biomass [16–18]. Suitable process technologies are first identified and then thermo-economic models are developed. The thermodynamic model computing the chemical and physical transformations and the associated heat requirements is combined with a separate energy integration model representing the heat recovery system. Based on the pinch analysis methodology the optimal thermal process integration is computed after defining the maximal heat recovery potential from the hot and cold streams and their minimum approach temperature ΔT_{min}. The process needs are satisfied by different utilities such as, combustion of waste and producer gas (PG), Rankine cycle for power production, gas turbine and cogeneration by burning either H_2-rich fuel or almost pure H_2. The optimal utility integration is defined by maximizing the combined production of fuel, power and heat with regard to the minimal operating cost by solving a linear programming problem [16, 19, 20]. Using the data from the thermodynamic model the costs are estimated based on equipment sizing and cost correlations from the literature [21, 22]. For the LCA model, the cradle-to-gate LCA approach described in [23] is applied with a functional unit of 1 kJ of biomass at the inlet of the installation and the impact assessment method developed by the Intergovernmental Panel on Climate Change (IPCC) considering a time horizon of 100 years for the global warming potential (GWP). The multi-objective optimization approach [16, 24] identifies the relationship between competing objectives with regard to environomic (i.e. thermodynamic, economic and environmental) criteria and assesses the different trade-offs.

3. Process description

The thermochemical process converting biomass into H_2 fuel consists of wood handling, drying, gasification, gas cleaning and conditioning by reforming and shift conversion, and finally H_2 purification and/or H_2 burning for electricity generation. The general process superstructure represented in Fig.1 summarizes the different technological options for each process step and displays the life cycle inventory (LCI) flows within the system's limits. For the subsequent studies the process layout highlighted in gray is investigated, the other options being not considered at this point. The products are defined by the options chosen at the cross points A and B. Depending on the production purpose and on the fuel which is burnt the process either produces impure or pure H_2, imports or exports electricity, or is self-sufficient in terms of electricity.

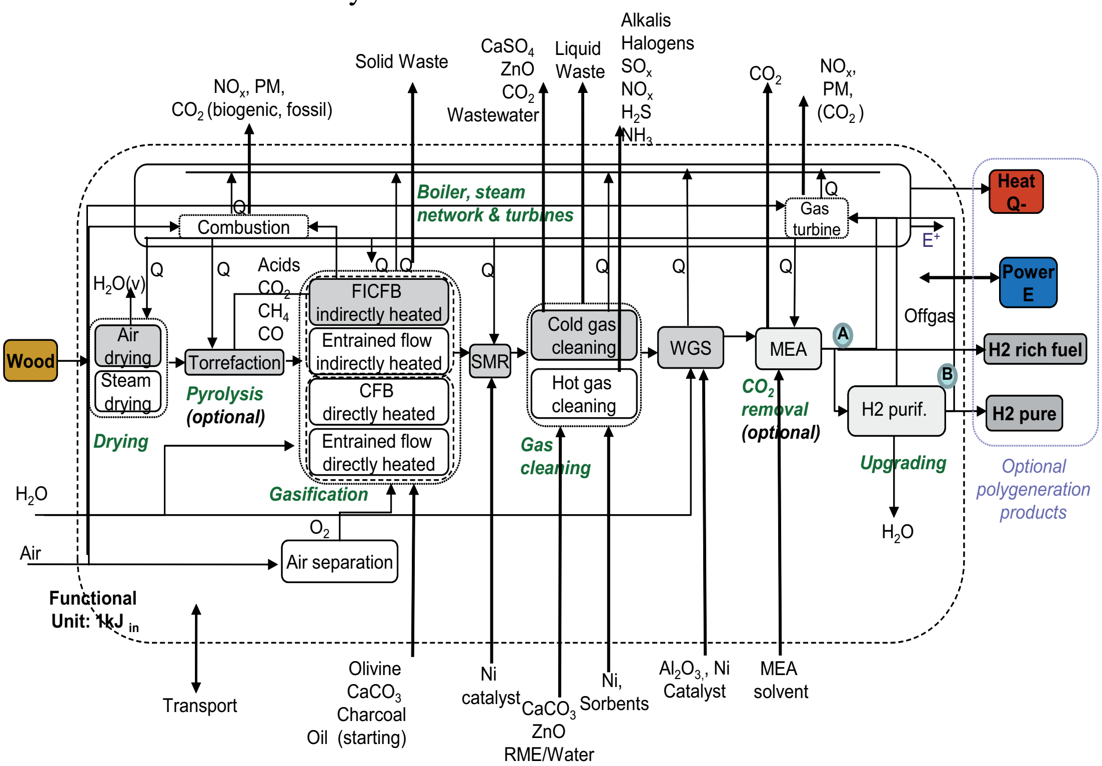

Fig. 1: Superstructure of the biomass conversion processes with recycling options including thermo-economic and LCA model flows. Investigated process options are highlighted in gray. The cross points A and B illustrate the different options with regard to H_2 and/or electricity generation.

3.1. Thermo-economic process model

The thermo-economic models for the drying, gasification and gas cleaning section have been developed in previous work [17, 18] and the same specifications for the biomass and process units are considered in this work. The chemical conversion in the gasifier is modeled by equilibrium relationships with an artificial temperature difference as explained in [18]. After the gasification the syngas is treated in two sequential water gas shift (WGS) reactors (Eq.1) one operating at high (HTS) and one at lower (LTS) temperature, to increase the H_2 and CO_2 concentrations before CO_2 removal reducing the greenhouse gas emissions and producing higher LHV fuel.

$$CO + H_2O \overset{\Delta\tilde{h}_r{}^0=-41\ kJ/mol}{\leftrightarrow} CO_2 + H_2 \tag{1}$$

For the H_2 separation and purification CO_2 capture by chemical absorption with amines and by physical adsorption by pressure swing adsorption (PSA) are considered. To produce pure H_2 and to capture high purity CO_2 for storage a chemical absorption step is introduced before the PSA unit. For the PSA model the approach outlined in [18] is adapted for H_2 / CO_2 separation based on data from [25]. The chemical absorption with MEA is modeled as a blackbox considering the energy demands for the separation given in [26] and summarized in Table 3. PSA yields H_2 purities of over 99%mol. The nominal operating conditions of the main process units are summarized in Table 4.

Table 3: Parameters for the H_2 purification.

Section	Specification	Value
MEA abs.	Thermal $\dot{Q}$ @ 150^oC	3.7MJ/kg CO_2
	Electric Power	1.0MJ/kg CO_2
PSA	Adsorption P	10bar
	Purging P	0.1bar
	H_2 recovery	90%

Table 4: Operating conditions of the process units and feasible range for optimization.

Operating parameter	Nominal	Range
Drying		
Temperature (in) [K]	473	-
$\theta_{wood,out}$ [wt%]	20	[5-35]
Gasification		
Pressure [bar]	1	[1-15]
Temperature [K]	1123	[1000-1200]
Steam/biomass [%]	50	-
SMR		
Temperature [K]	1138	[950-1200]
WGS		
Pressure [bar]	25	[1-25]
Temperature HTS [K]	623	[573-683]
Temperature LTS [K]	453	[473-573]
H_2O/CO ratio [-]	2	[0.2-4]

4. Process performance

4.1. Performance indicators

The overall energy efficiency ϵ_{tot} defined by Eq.2 characterizes the chemical conversion and the quality of the process integration by taking into account the energy of the products and resources. For the natural gas (NG) equivalent efficiency ϵ_{eq} (Eq. 3) the net electricity that is consumed is substituted by a NG equivalent calculated based on an exergy efficiency of 55%. The H_2 productivity is defined by the H_2 yield (Y_{H2}) (Eq.4) and the conversion efficiency ϵ_{H2} (Eq.5) expressing the production of the H_2 fuel with regard to the biomass resource consumption, without taking into account the electricity import or export. The exergy efficiency ϵ_{ex} is also computed. All the reported efficiencies are expressed on the basis of the lower heating value (Δh^0, LHV) of dry biomass.

$$\epsilon_{tot} = \frac{\Delta h^0_{fuel,out} \cdot \dot{m}_{fuel,out} + \dot{E}^-}{\Delta h^0_{Biomass,in} \cdot \dot{m}_{Biomass,in} + \dot{E}^+} \tag{2}$$

$$\epsilon_{eq} = \frac{\Delta h^0_{Fuel,out} \cdot \dot{m}_{Fuel,out} + \frac{1}{\eta_{NGCC}} \frac{\Delta h^0_{NG}}{\Delta k^o_{NG}} (\frac{1}{\eta_{HP}} \dot{Q}^- + \dot{E}^-)}{\Delta h^0_{Biomass,in} \cdot \dot{m}_{Biomass,in}} \tag{3}$$

$$Y_{H2} = \frac{g_{H_2}}{kg_{biomass}} \tag{4}$$

$$\epsilon_{H2} = \frac{\Delta h^0_{H2fuel} \cdot \dot{m}_{H2fuel}}{\Delta h^0_{Biomass,in} \cdot \dot{m}_{Biomass,in}} \tag{5}$$

The economic performance is defined by the capital investment and the operating cost estimated according to [21, 22] with the assumptions given in Table 5. All the performance analyses are performed for a plant capacity of 380MW$_{th,biomass}$.

Table 5: Assumptions for the economic analysis.

Parameter	Value
Marshall and Swift Index	1473.3
Dollar exchange rate (€_US$)	1.5 US$/€
Expected lifetime	15 years
Interest rate	6%
Yearly operation	8000h/year
Operators [18]	4 p./shift
Operator's salary	91'070 $ /year
Wood costs (θ_{wood}=50%)	50 $ /MWh
Electricity price (green)	270 $ /MWh

Table 6: Feasible range for optimization of the steam network design and the gas turbine.

Operating parameter	Unit	Range
1st Production level	bar	[90-130]
2nd Production level	bar	[70-110]
Superheating temperature	K	[623-823]
1st Utilization level	K	[300-523]
2nd Utilization level	K	510
Condensation level	K	292
Combustion T	K	[700-900]
Turbine T	K	1500

4.2. Energy integration

Heat integration and recovery are important with regard to the process performance since several parts of the system operate at high temperature. The minimum energy requirement is computed from the hot and cold process streams through the heat cascade method accounting for the potential heat recovery. Heat is required by the gasification, the endothermic reforming, the water evaporation for gasification and WGS, and the CO_2 capture. The exothermic WGS and the process and offgas cooling down release heat. The heat demands can be satisfied by different utilities. High temperature heat is delivered by the combustion of waste streams (i.e. unconverted char and gaseous residues of the separation and purification sections) and if necessary additional process streams (i.e. hot or cold PG from the gasifier) and depending on the production scope also by the burning of H_2-rich gas or pure H_2 in a gas turbine to co-produce electricity. In general, the best choice is determined by assembling the potential fuels in a superstructure, integrating the different possibilities and computing the optimal solution by minimizing the operating cost [20]. In the linear programming problem a cost is attributed to the electricity import/export (i.e. [50-270$/MWh]) and to the CO_2 emissions (i.e. 36$/to$_{CO2}$, [15-90$/to$_{CO2}$]). Surplus heat can be recovered in a Rankine cycle with an extraction steam turbine/generator to generate additional electricity and supply steam for gasification, steam methane reforming and shift conversion. A cycle with two production, two usage and one condensation level is considered and adapted to the different process configurations with regard to the parameters given in Table 6. The remaining excess heat is removed by cooling water. The process integration including hot and cold utilities for two different configurations (Table 7:A&B) producing H_2 is represented in Fig.2 and discussed in detail in Section 4.3..

4.3. Process integration analysis

The influence of the heat recovery and the cogeneration systems including the introduction of a steam network, gas turbines or heat pumps is analyzed with regard to H_2 and electricity production and captured CO_2. Table 7 summarizes the different process scenarios and the computed performances.

4.3.1. H_2 production processes

For the process configurations producing H_2 by biomass conversion different options with H_2 purification and/or carbon capture are considered. The performances are reported by scenarios A-F (Table

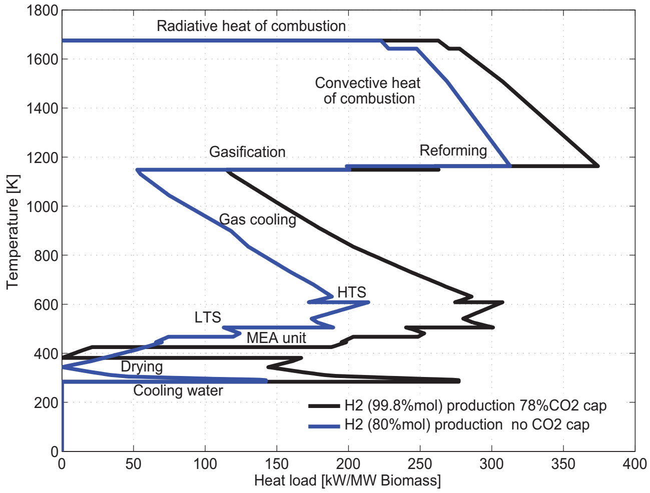

Fig. 2: Integrated composite curves for H_2 process with and without CO_2 capture (Table 7:A& B).

Table 7: Investigated process scenarios characteristics. For the different technology options: n=not included, y=yes included. The net electricity output expressed in kW of electricity per MW of biomass is negative when the integrated process requires electricity importation and positive when it generates electricity. For H_2 processes the costs are expressed in $/MWh$_{H2}$ while for electricity generation they are expressed in $/MWh$_e$.

Scenario	A	B	C	C_{opt}	D	D_{opt}	E	F	G	H	H_{opt}	I	J	J_{opt}
	H_2 Process								Electricity generation					
	Process Parameters								Process Parameters					
Products	H_2	H_2	H_2	H_2	H_2	H_2	H_2	H_2	$\dot{E}$	$\dot{E}$	$\dot{E}$	$\dot{E}$	$\dot{E}$	$\dot{E}$
Carbon capture [%]	y	n	y	y	y	y	y	y	n	y	y	n	y	y
PSA	y	y	y	y	y	y	n	n	y	y	y	n	n	n
PG burning	y	y	y	y	y	n	y	y	n	n	n	n	n	n
GT H_2 impure	n	n	n	n	n	y	n	n	n	n	n	y	y	y
GT H_2 pure	n	n	n	n	n	n	n	n	y	y	y	n	n	n
HP	n	n	387/478K	387/478K	387/478K	387/478K	n	387/478K	n	387/478K	387/478K	n	387/478K	n
Steam network:	n	n	y	y	y	y	y	y	y	y	y	y	y	y
Production levels [bar]	-	-	140	135&95	125	128	93	125&93	125&93	125&93	105&60	125&93	125&93	128&60
Consumption levels [K]	-	-	513&473	505&434	473&300	483&430	300	513&300	513&300	513&300	428&300	513&300	510&300	431&300
	Power Balance								Power Balance					
Consumption [kW/MW]	136.7	72.5	169.7	153.3	120.6	119.6	127.5	100.8	91.8	221.5	102.8	89.5	176.6	77.4
HP [kW/MW]	0	0	40.4	35.9	27.6	8.1	35.9	28.1	0	53.1	0.3	0	53.3	0
Steam network [kW/MW]	0	0	25.7	10.1	37.7	29.3	31.2	28.1	115.6	132.6	108.2	100.4	113.9	105.7
Gas turbine [kW/MW]	9.1	28.9	9.9	30.4	110.5	98.4	6.0	100.8	425.5	414.7	389.3	338.8	307.9	296.2
Net electricity [kW/MW]	-127.6	-43.6	-174.5	-148.7	0	0	-126.2	0	449.3	272.7	394.4	349.7	191.9	324.5
	Performance								Performance					
H_2 yield [g/kg$_{Biomass}$]	79.8	92.4	102.9	107.1	68.7	83.8	96.7	72.2	0	0	0	0	0	0
H_2 purity [mol%]	99.8	80.7	99.8	99.3	99.8	98.7	97.4	97.4	80.7	99.8	98.7	69.1	97.4	63.2
H_2 production [t/d]	140.7	162.8	181.4	188.7	121.1	147.7	170.5	127.3	0	0	0	0	0	0
Energy H_2 [kW/MW]	514.3	596.9	663	696.5	442.2	550.1	626.9	468.1	0	0	0	0	0	0
CO_2 capture [%]	44.9	0	57.9	52.3	38.6	25	53.3	39.8	0	78.2	22.4	0	78.2	24.9
gCO_2 captured/kWh	316	0	316	271	316	164	308	307	0	1037	205	0	1474	278
ϵ_{tot} [%]	45.6	57.2	56.4	60.6	44.2	55	55.6	46.8	44.9	27.3	39.4	34.9	19.2	32.4
ϵ_{eq} [%]	29.1	52.1	35.8	43.7	44.2	55	40.1	46.8	-	-	-	-	-	-
ϵ_{H2} [%]	51.4	59.7	66.3	69.6	44.2	55	62.7	46.8	-	-	-	-	-	-
ϵ_{ex} [%]	39.9	49.7	49.6	53.1	38.2	47.5	48.7	40.4	39.9	24.3	35.1	31.1	17.1	28.9
	Economics								Economics					
Investment [M$]	424	421	525	401	555	361	461	511	521	600	416	446	529	333
Annualized Inv. [$/MWh]	27.9	23.9	26.8	19.5	42.5	22.2	24.9	36.9	39.2	74.5	35.7	43.2	93.4	34.7
Maintenance [$/MWh]	21.7	18.7	19.4	15.5	30.2	18.5	18.8	26.9	28.5	51.6	28.0	33.1	67.4	29.8
Wood cost [$/MWh]	95.7	82.4	74.2	70.6	111.3	89.4	78.5	105.1	109.5	180.4	124.8	140.7	256.3	151.6
Electricity cost [$/MWh]	65.9	19.4	69.9	42.5	0	0	53.5	0	0	0	0	0	0	0
Production cost [$/MWh]	211.2	144.4	190.3	148.1	184	130.1	175.7	169	177.2	306.5	188.5	217	417	216.1
	Environmental Impact (GWP 100)								Environmental Impact (GWP 100)					
10^{-5} kg CO2$_{eq}$/kJ$_{BM}$	-4.2	0.6	-5.6	-5.1	-3.6	-2.3	-5.2	-3.8	0.8	-6.9	-1.44	0.8	-6.8	-1.74

7). The energy integration of the process with H_2 separation by PSA and without or with carbon capture by chemical absorption with amines is illustrated in Fig.2. Since the pinch point is located at low temperature there is no excess heat that can be used in a Rankine cycle. By introducing a heat pump, heat can be transfered to a higher temperature for valorization in a Rankine cycle and consequently the energy integration of the CO_2 capture is improved as shown in Fig.3 (Table 7:C).

The influence of CO_2 capture is studied by the comparison of scenarios B and C (Table 7). CO_2 capture increases the power consumption considerably by the requirement for the solvent regeneration and the CO_2 compression. The purchase of the capture unit equipments increases the capital investment and consequently the production cost are increased by around one third. Through H_2 purification the H_2 yield is increased by over 10% and the environmental impact is decreased through CO_2 storage. By performing a multi-objective optimization it is shown in Section 4.4. how the performance can be improved further to reach an overall energy efficiency of around 60% with CO_2 capture (Table 7:C_{opt}) by changing the operating conditions.

For these configurations electricity is imported to satisfy the overall process demands. Alternatively, part of the H_2 rich gas and/or H_2 product could be burnt in a gas turbine to cover the power demand and yield a self-sufficient process in terms of heat and power (Table 7:D). The energy integration of such a scenario is represented in Fig.4. The self-sufficient H_2 process has a lower H_2 yield since part of the product is used for electricity production which leads to an energy efficiency decrease of more than 10% points. The equivalent efficiency ϵ_{eq} is however increased by around 10% points which shows that the internal electricity production is more efficient than an NGCC. Due to the reduced electricity cost the production cost are slightly reduced, even if the H_2 yield is reduced and the capital investment increased. However, for keeping a higher level of CO_2 capture in the process the production cost would be larger (Table 8). In Sections 4.4.&4.5. it is shown that the process can become more attractive by changing the operating conditions and that the economic competitiveness of this option depends highly on the electricity and fuel market prices and the CO_2 taxes.

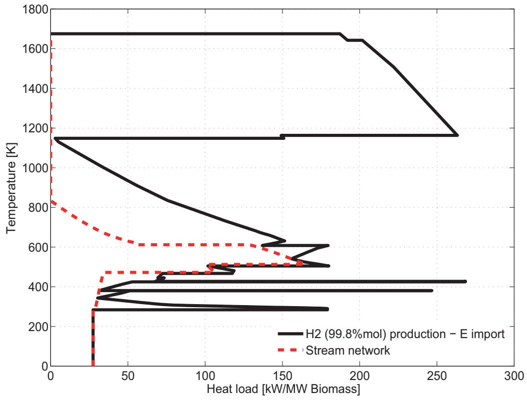

Fig. 3: Integrated composite curve for a base case H_2 process with net $\dot{E}$ import and with steam network integration (scenario C).

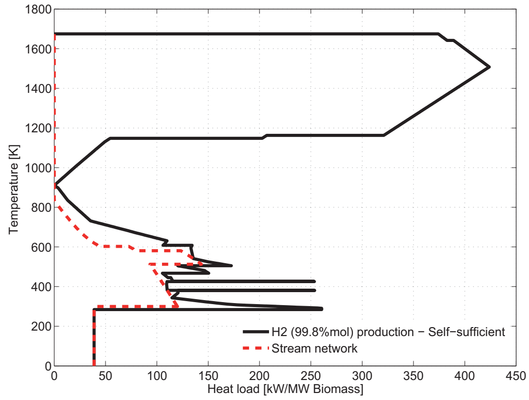

Fig. 4: Integrated composite curve for a self-sufficient H_2 process with steam network integration (scenario D).

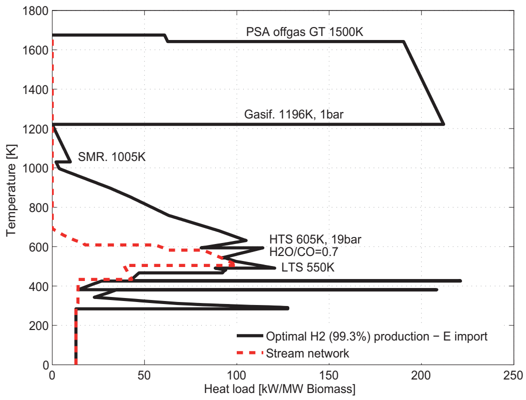

Fig. 5: Integrated composite curve for an optimized H_2 process with net $\dot{E}$ import and steam network integration (scenario C_{opt}).

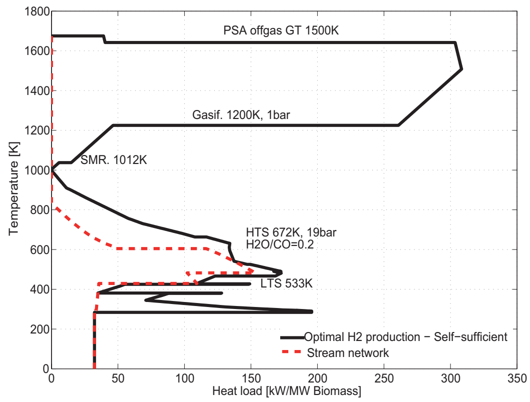

Fig. 6: Integrated composite curve for an optimized self-sufficient H_2 process with steam network integration (scenario D_{opt}).

The H_2 purification by PSA (Table 7:C) increases the H_2 purity by around 2.5% compared to the process without PSA (Table 7:E). The electricity demand and the investment are increased, however the overall impact on the performance is relatively low since the H_2 yield is increased.

4.3.2. Electricity only production processes

Instead of generating H_2 as a final product, electricity can also by produced by burning the H_2 gas products in a combustion engine. Different configurations producing electricity as a final product are assessed (Table 7:G-J): electricity generation from nearly pure H_2 and electricity generation by the combustion of the H_2-rich stream after WGS without (scenarios G&I) and with carbon capture (scenarios H&J). H_2 purification and carbon capture adding additional cost, the configuration burning impure H_2 (lower LHV fuel) without CO_2 capture (scenario I) yields the lowest investment cost. The burning of pure H_2 (higher LHV fuel) generates more electricity in the gas turbine which outweighs the additional power consumption for H_2 purification and consequently yields a higher energy efficiency. However, there are still some concerns with regard to flame stability which have to be addressed for high purity H_2 combustion. CO_2 capture leading to a negative CO_2 balance in biomass based processes, reduces the efficiency by around 10% and increases the production cost considerably. The difference in the energy integration for the electricity generation without and with CO_2 capture is reported in Fig.7&8 respectively. In these scenarios the hot utility is satisfied by the heat generated from the gas turbine and by the combustion of waste streams. The computed efficiencies are in the range of the IBGCC power plant efficiency of 33.9% reported in [13].

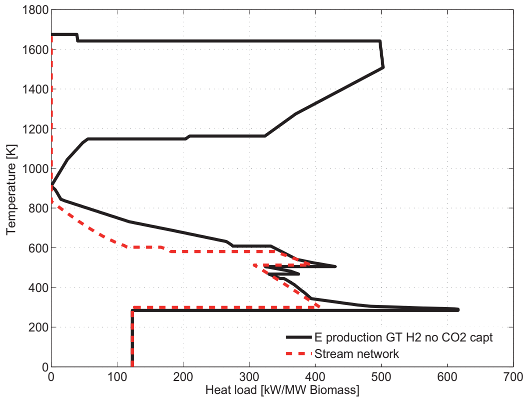

Fig. 7: Integrated composite curve for the $\dot{E}$ production without CO_2 capture and with steam network integration (scenario G).

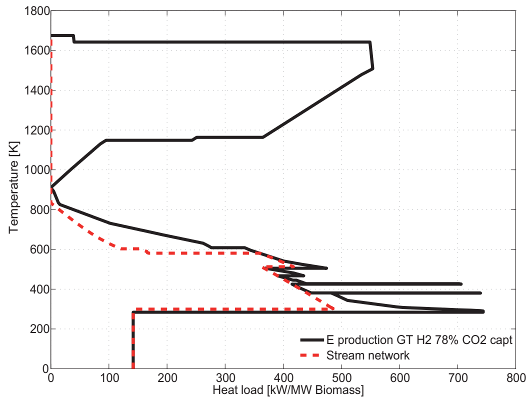

Fig. 8: Integrated composite curve for the $\dot{E}$ production with CO_2 capture and with steam network integration (scenario H).

4.4. Process optimization

To investigate the trade-off between several competing factors defining the process performance, multi-objective optimization is performed by applying an evolutionary algorithm. The decision variables and their variation range are chosen according to the key process operating conditions and the steam network characteristics reported in Tables 4 and 6, respectively.

Four scenarios are optimized: H_2 production with electricity import (scenario C), self-sufficient H_2 production (scenario D), electricity generation from nearly pure H_2 (scenario H) and electricity generation from H_2-rich gas (scenario J). First the maximization of the energy efficiency ϵ_{tot} and the minimization of the capital investment are chosen as objectives. The optimal Pareto frontiers are presented in Fig.9 (left). The energy efficiency increase goes in pair with the investment increase. For each scenario the performance of an optimal configuration yielding a high ϵ_{tot} is reported in Table 7 (C_{opt}/D_{opt}/H_{opt}/J_{opt}). The energy integration and the main operating conditions of the optimal H_2 process designs are represented in Fig.5& 6, respectively. Looking at the equivalent efficiency instead of ϵ_{tot}, the self-sufficient scenario (D_{opt}) performs better than the one with electricity import (C_{opt}). Through the optimization the energy efficiency is increased and the cost are decreased compared to the base case scenarios, however the CO_2 capture rate is lower and consequently the environmental benefit is less important. The trade-off between the energy efficiency and the CO_2 capture rate is highlighted by the optimal Pareto frontier resulting from the maximization of the energy efficiency and the CO_2 capture rate (Fig.9(right)). With regard to competitiveness a compromise between the different objectives has to be found. The performance of selected optimal configurations yielding relative high efficiency and capture rates are reported in Table 8. Depending on the biomass and the electricity import/export prices, production cost can become lower as shown in section 4.5.. Compared to fossil power plants (Tables 1& 2) with carbon capture the biomass conversion into electricity and H_2 reveals to be competitive.

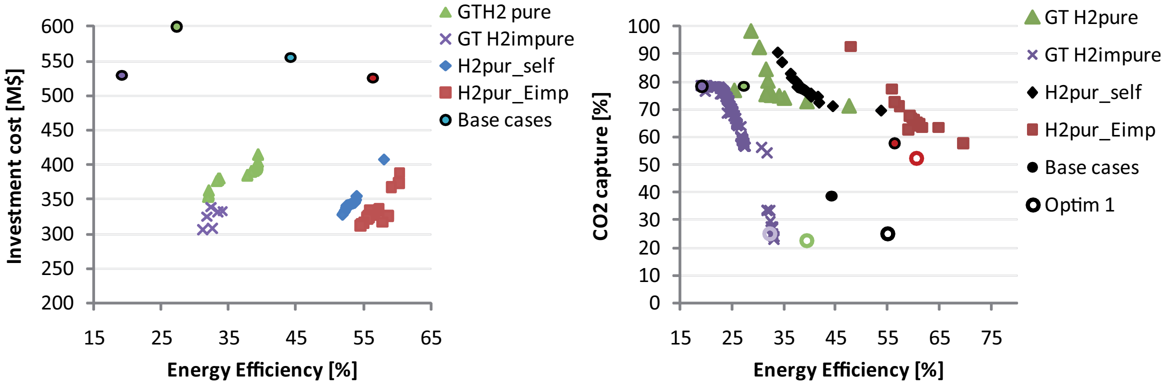

Fig. 9: Optimal solutions in the Pareto domain for different objectives for H_2 processes (scenario C& D) and $\dot{E}$ generation processes (scenario I& H).

Table 8: Process performance of selected optimal configurations.

Process	H_2 $\dot{E}$ import	H_2 self-sufficient	$\dot{E}$ GT H2 pure	$\dot{E}$ GT H2 impure
ϵ_{tot} [%]	60.6	40.2	32.5	27.5
CO_2 capture [%]	65.1	74.4	75.2	56.4
gCO_2 captured/kWh	324	668	835	741
10^{-5} kg $CO2_{eq}$/kJ$_{BM}$	-6.5	-7.0	-6.6	-4.8
Investment [M$]	509	651	777	532
Production cost [$/MWh]	129.7	214.1	284.3	291.3

4.5. Economic evaluation

The H_2 production cost assessed previously depend strongly on the economic assumptions made in Table 5. The sensitivity analysis varying the wood cost [10-70 $ /MWh$_{BM}$] and the green electricity cost [40-270 $ /MWh$_e$] shows the influence on the competitiveness of the H_2 production in Fig.10 for the scenarios yielding a compromise between efficiency and CO_2 capture (Table 8) and the base case without capture (Table 7:B). With the initial assumption of 50$/MWh$_{BM}$ up to 60% of the production cost are attributed to wood purchase, whereas a decrease of the resource cost can reduce this fraction to around 20% and reduce the H_2 production cost by nearly 50%. These costs are still slightly higher than the one reported in [5] because of the higher investment cost, especially for the gasifier purchase. Contrary to their approach, the investment estimation method applied here rates the equipment with conventional design heuristics that take the operating conditions into account. As pilot plant data are used as reference for the design parameters of the gasifier, it can be expected to yield realistic figures. The conservative cost estimation might however overestimate the investment and consequently lead to higher production cost. Nevertheless, these biomass based H_2 processes yielding efficiencies of 40-60% and production costs in the range of 65-262$/MWh$_{H2}$ can become a competitive option with regard to fossil resource depletion and climate change compared to conventional processes using fossil resources (Table 1). Considering a new hydrogen plant based on fossil resources [14] producing H_2 with an efficiency of 60%, production costs of 28$/MWh$_{H2}$ and CO_2 emissions of 493kg/MWh$_{H2}$ as a reference, CO_2 avoidance cost [1] in the range of 45-220$/t$_{CO2}$ are assessed for the analyzed biomass based processes. In comparison, CO_2 avoidance cost in the range of 2-56$//t$_{CO2}$ are assessed for fossil H_2 production processes with CO_2 capture in [14] .

[1] CO_2 avoidance cost expressed in $/t$_{CO2,avoided}$ are defined by the ratio of the difference of the production cost and the CO_2 emissions for a plant with capture and a reference plant without capture: $\frac{COE_{CC}-COE_{ref}[\$/MWh]}{CO2_{emit,ref}-CO2_{emit,CC}[kgCO2/MWh]}$. For the biomass based plants the CO_2 emissions equal to the negative value of the CO_2 captured since it is removed from the atmosphere.

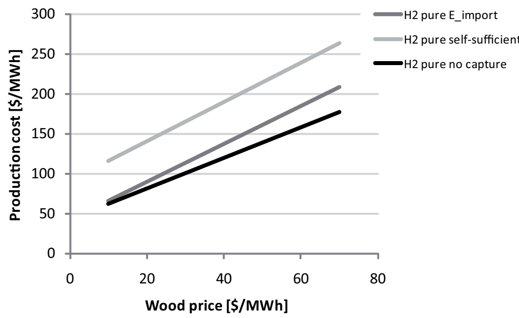

Fig. 10: Sensitivity analysis of the wood cost on the hydrogen production cost [\$/MWh$_{H2}$] for different H_2 scenarios (Table 7:B & Table 8).

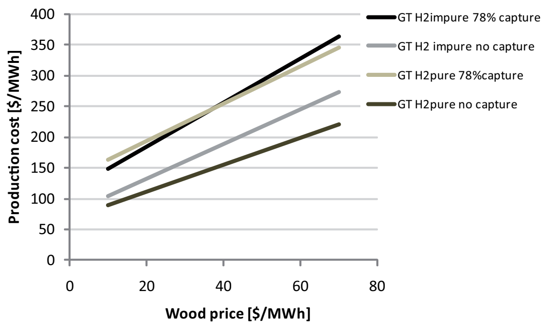

Fig. 11: Sensitivity analysis of the wood cost on the electricity generation cost [\$/MWh$_e$] for different scenarios (Table 7:G/I & Table 8).

For the electricity production processes without CO_2 capture (Table 7:G/I) and with CO_2 capture (Table 8) a sensitivity analysis on the wood cost [10-70 \$ /MWh$_{BM}$] yields electricity production cost in the range of 89-362\$/MWh$_e$. Compared to fossil power plants (Table 2) some scenarios with CO_2 capture are promising regarding the future energy market, especially when high CO_2 taxes are imposed. Considering a NGCC plant [14] with an efficiency of 57%, production costs of 40\$/MWh$_e$ and CO_2 emissions of 360kg/MWh$_e$ as a reference, CO_2 avoidance cost in the range of 98-254\$/t$_{CO2}$ are assessed for the analyzed biomass based processes. In comparison, CO_2 avoidance cost in the range of 37-74\$//t$_{CO2}$ are assessed for an NGCC with CO_2 capture in [14].

The market price of electricity, fuel, biomass and CO_2 taxes will define if it is more advantageous to produce H_2 with or without electricity import as final product or to convert the H_2 fuel directly into electricity with or without CO_2 capture.

4.6. Environmental impacts

For the life cycle inventory the method from the IPCC (IPCC07) is applied based on the LCI flows identified in Fig.1. As functional unit 1kJ of biomass is considered in order to make a consistent comparison of H_2 and electricity production scenarios. For the H_2 processes the produced H_2 is substituted with H_2 produced from cracking (95%) and electrolysis (5%) based on the data available from the ecoinvent database [27]. For the electricity impact contribution the Swiss mix for medium voltage electricity production at grid is considered. The amount of CO_2 that is stored is accounted as negative contribution of fossil CO_2.

Regarding the climate change impact of H_2 processes, Fig.12 shows the advantage of CO_2 capture. H_2 production from biomass and CO_2 capture for storage have a negative contribution (n) to the climate change impact which largely outweighs all the other positive contributions (p).

For the electricity generation processes the benefit of CO_2 capture on the climate change is highlighted in Fig.13. A large impact is attributed to the use of rape methyl ester (RME) produced from colza cultivated with insecticides and consumed for the cold gas cleaning, consequently alternative colza cultivation methods and the development of alternative cleaning technologies such as hot gas cleaning have to be analyzed.

With regard to CO_2 emissions mitigation, processes based on renewable biomass have a huge potential, especially if CO_2 capture and storage is implemented since this leads to a negative CO_2 balance.

5. Conclusion

A systematic methodology based on thermo-economic and LCA models coupled with a multi-objective optimization algorithm has been applied to the conceptual design of integrated plants for H_2 fuel, power and heat production. The competitiveness of H_2 and electricity production and co-production process options are evaluated consistently with respect to energy efficiency, cost and environmental impacts. It is highlighted in particular, how appropriate energy integration and operating

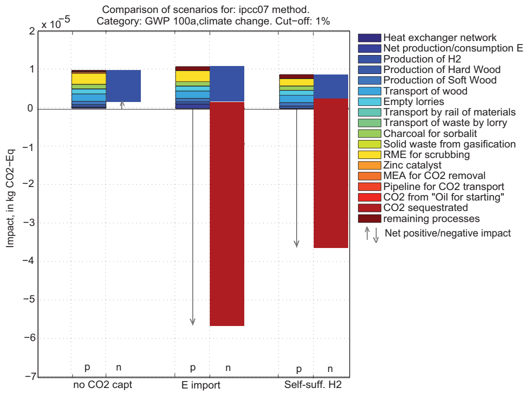

Fig. 12: Comparison of the climate change impact of the H_2 generation processes (Table 7:B/C/D) based on impact method IPCC07 for 1kJ of biomass.

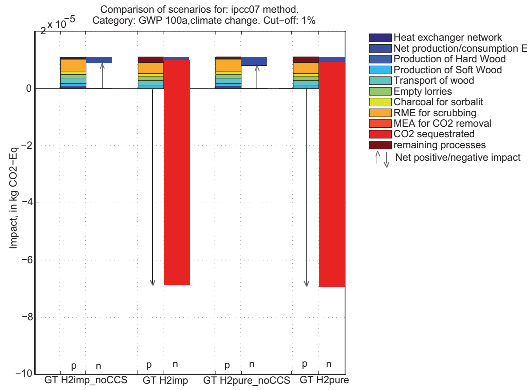

Fig. 13: Comparison of the climate change impact of the electricity generation processes (Table 7:G-J) based on impact method IPCC07 for 1kJ of biomass.

conditions improve the process performance by maximizing the combined production of fuel, heat and power. Based on multi-objective optimizations with regard to energy efficiency and capital investment or CO_2 capture rate, the trade-off between H_2 and electricity generation and CO_2 capture are assessed. LCA analysis underlined the climate change benefit of using renewable resources and capturing CO_2. Overall energy efficiencies in the range of 60% are reached for H_2 production and around 39% for electricity production with CO_2 capture. Depending on the biomass price evolution H_2 production costs in the range of 65-262\$/MWh$_{H2}$ and electricity production costs in the range of 89-362\$/MWh$_e$ are assessed. With regard to conventional H_2 and electricity production processes based on fossil resources, CO_2 avoidance costs of 45-220\$/t$_{CO2,avoided}$ and 98-254\$/t$_{CO2,avoided}$ respectively, are computed. In comparison, the performances assessed in [14] for processes using fossil resources are for a NGCC plant 43-72\$/MWh$_e$ and 37-74\$/t$_{CO2,avoided}$, and for H_2 plants 27-48\$/MWh$_{H2}$ and 2-56\$/t$_{CO2,avoided}$. The market price of electricity, fuel, biomass and CO_2 taxes will consequently define the competitiveness of biomass conversion into H_2 or electricity with or without CO_2 capture. With regard to a future energy system promoting renewable resources and reduced greenhouse gas emissions biomass based H_2 and electricity production have to be considered as a competitive alternative.

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Nomenclature

Abbreviations

BM Biomass
CC Carbon Capture
CFB Circulating Fluidized Bed
COE Cost Of Electricity
GWP Global Warming Potential
HHV Higher heating value
HTS High temperature shift
IBGCC Integrated Biomass Gasification Combined Cycle
IGCC Integrated Gasification Combined Cycle
IPCC Intergovernmental Panel on Climate Change
LCA Life Cycle Assessment
LCI Life Cycle Inventory

LHV Lower Heating Value
LTS Low temperature shift
MEA Monoethanolamine
MOO Multi-Objective Optimization
NG Natural Gas
NGCC Natural Gas Combined Cycle
PC Pulverized Coal
PG Producer Gas
PSA Pressure Swing Adsorption
RME Rape Methyl Ester
SMR Steam Methane Reforming
WGS Water-Gas Shift

Greek letters

Δh^o Lower heating value, kJ/kg
$\Delta \tilde{h}_r{}^0$ Standard heat of reaction, kJ/mol
ϵ_{eq} Natural gas equivalent efficiency, %
ϵ_{H2} H_2 efficiency, %
ϵ_{ex} Exergy efficiency, %
ϵ_{tot} Energy efficiency, %
Y_{H2} H_2 Yield, g_{H2}/kg_{BM}

Roman letters

$\dot{E}$ Mechanical/electrical power, kW
$\dot{m}$ Mass flow, kg/s
P Pressure, bar
$\dot{Q}$ Heat, kW
T Temperature, ^oC or K

Superscripts

$^+$ Material/energy stream entering the system
$^-$ Material/energy stream leaving the system

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