

Simulating viscoplastic avalanches

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Viscoplastic material

- ▶ Occurrence of a yield-stress:
Threshold τ_0 , for the
stress to shear the material.
- ▶ Examples:
 - ▶ Concrete
 - ▶ Clay, Mudflow
 - ▶ Snow, Avalanche
 - ▶ Nutrients, Cosmetics
- ▶ Focus:
Rapid flows.



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Flow down an inclined plane

Outline

Introduction

Modeling

- Contiuum mechanical approach

- Rheology

- Governing equations

- Two phase flow

Numerical Scheme

- The Inter-phase

- Projection scheme

Results

- Convergence

- Down a channel

- On an inclined plane

Results

- Looking into the flow

Conclusion

Stress Tensor

“Stress”

$$\boldsymbol{\tau} = \mu \dot{\boldsymbol{\gamma}}$$

“Shear-rate”

$$\dot{\boldsymbol{\gamma}} = \left(\nabla \vec{u} + (\nabla \vec{u})^T \right)$$

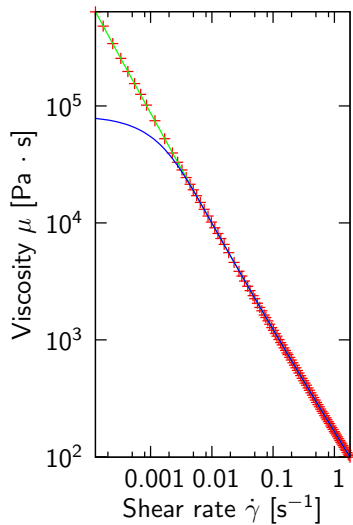
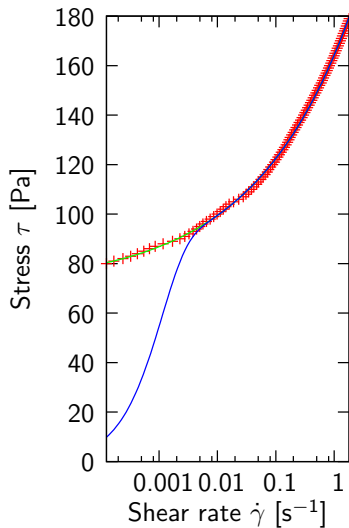
- ▶ Herschel-Bulkley fluid

$$\mu(\dot{\boldsymbol{\gamma}}) = \frac{\tau_0 + K \dot{\boldsymbol{\gamma}}^\alpha}{\dot{\boldsymbol{\gamma}}}$$

- ▶ isotrope
- ▶ no thinxotropy
- ▶ measurable quantity

Viscosity function

data +
fitted HB-modell — (green)
smoothed modell — (blue)



Governing equations

Momentum equation:

$$\frac{\partial \vec{u}}{\partial t} = -\nabla p + \frac{1}{\rho} \nabla \cdot \boldsymbol{\tau} \quad (1)$$

Continuity/Incompressibility:

$$\nabla \cdot \vec{u} = 0 \quad (2)$$

Equation of state:

$$\boldsymbol{\tau} = \nu(\dot{\gamma}) \dot{\boldsymbol{\gamma}} \quad (3)$$

$$(4)$$

Level-Set formulation

- ▶ Signed distance function: $\Phi(\vec{x}, t)$

$\Rightarrow \Phi = 0$ Location of the interface

$\Phi > 0$ Liquid phase

$\Phi < 0$ Gas phase

- ▶ Advected by the Velocity field:

$$\frac{\partial \Phi}{\partial t} + \vec{u} \cdot \nabla \Phi = 0 \quad (5)$$

- ▶ Reinitialisation

$$|\nabla \Phi| = \text{sgn}(\Phi) \quad (6)$$

Smoothing

$$H_\epsilon(\Phi) = \begin{cases} 1 & , \Phi > \epsilon \\ 0 & , \Phi < -\epsilon \\ 1 + \sin\left(\frac{\Phi}{\epsilon}\pi\right) & \text{else.} \end{cases}$$

$H_{dx}(\Phi) \approx$ Volume of fluid

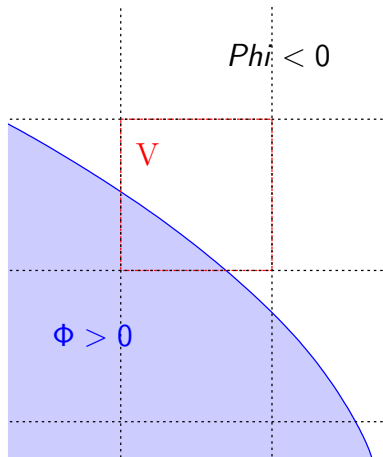
Density:

$$\frac{d\vec{u}}{d\vec{n}} = 0$$

↓

$$\bar{\rho} = H(\Phi)\rho_l + (1 - H(\Phi))\rho_g$$

proof



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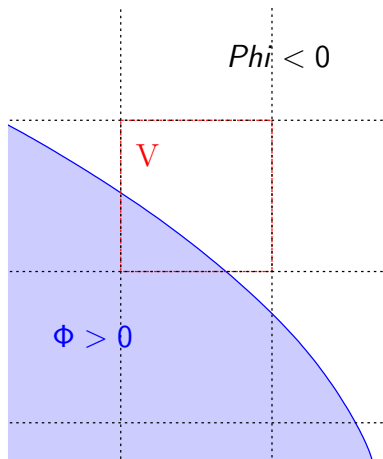
Viscosity:

$$\frac{d\tau}{d\vec{n}} = 0$$

⇓

$$\frac{1}{\mu(\Phi)} = \frac{H(\Phi)}{\mu_l(\dot{\gamma}l)} + \frac{1 - H(\Phi)}{\mu_g}$$

proof



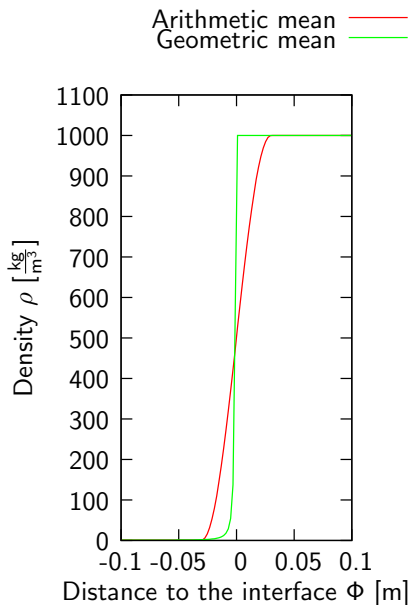
Smoothing near the interface

Geometric mean:

$$\frac{1}{\rho(\Phi)} = \frac{H(\Phi)}{\rho_l} + \frac{1 - H(\Phi)}{\rho_g}$$

Arithmetic mean:

$$\rho(\Phi) = H(\Phi)\rho_l + (1 - H(\Phi))\rho_g$$

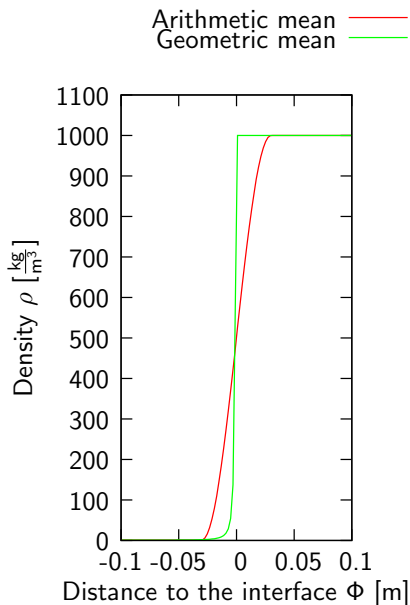


Smoothing near the interface

Geometric mean:

$$\frac{1}{\rho(\Phi)} = \frac{H(\Phi)}{\rho_l} + \frac{1 - H(\Phi)}{\rho_g}$$

- ▶ Sharp interface
- ▶ Physical interpretation:
Vapour pressure
- ▶ Jump in the density
Potential problem for the convergence!
- ▶ Numerical results match
better the experimental
results!



Projection scheme

$$\frac{\partial \vec{u}}{\partial t} = -\frac{1}{\rho} \nabla p - \vec{u} \cdot \nabla \vec{u} + \frac{1}{\rho} \nabla \cdot (\nu(\dot{\gamma})\dot{\gamma}) \quad (7)$$

$$\nabla \vec{u} = 0 \quad (8)$$

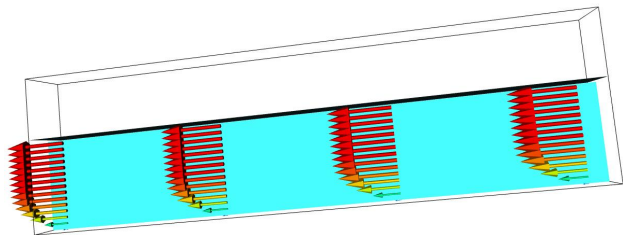
- ▶ Predictor Step: Solve momentum equation (7)

$$\frac{\vec{u}^* - \vec{u}_n}{\delta t} = -\frac{1}{\rho_n} \nabla p_n - \vec{u}_n \cdot \nabla \vec{u}_n + \frac{1}{\rho_n} \nabla \cdot \left(\frac{\nu_n}{2} (\dot{\gamma}^* + \dot{\gamma}_n) \right)$$

- ▶ Corrector Step: Correct the pressure to satisfy (8)

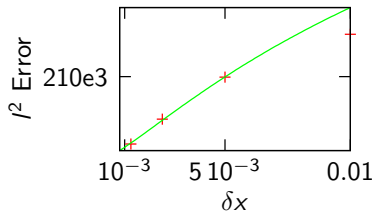
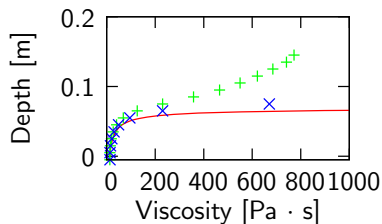
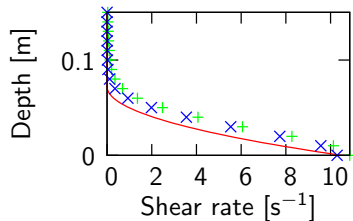
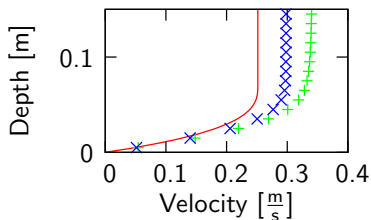
$$\begin{aligned} \frac{\vec{u}_{n+1} - \vec{u}^*}{\delta t} &= -\nabla(p_{n+1} - p^*) \\ \nabla \vec{u}^* &= \delta t \Delta(p_{n+1} - p^*) \end{aligned}$$

Comparing to steady uniform flow



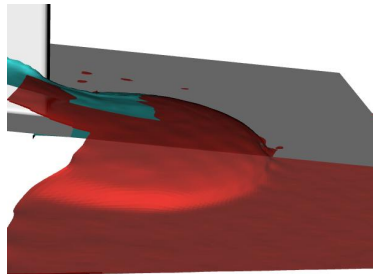
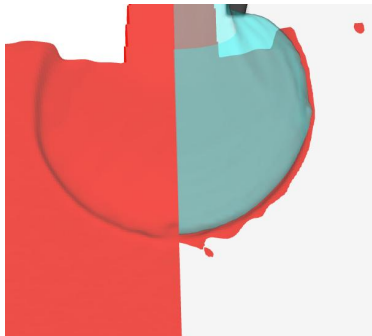
- ▶ Analytical solution for 2d one-phase free-surface flow
- ▶ Testing of:
 - ▶ Convergence of the solver
 - ▶ Influence of limiting the maximal viscosity

Convergence to analytical solution



Quasi 2d in a channel

Position of the free surface



Yield surface in the flow

Velocity profile

Fluid properties in interface cells

$$H(\Phi) = \begin{cases} 1 & , \Phi > \epsilon \\ 1 + \sin\left(\frac{\Phi}{\epsilon}\pi\right) & , -\epsilon < \Phi < \epsilon \\ 0 & , \Phi < -\epsilon \end{cases}$$

- ▶ Interpreted as volume fraction
(1st order Approximation)

Fluid properties in interface cells

Density:

$$\int_V \bar{\rho} \vec{u} dV = \int_{V \cap \{\Phi < 0\}} \rho_l \vec{u}_l + \int_{V \cap \{\Phi > 0\}} \rho_g \vec{u}_g \quad (9)$$

$$\bar{\rho} \int_V \vec{u} dV = \rho_l \int_{V \cap \{\Phi < 0\}} \vec{u}_l dV + \rho_g \int_{V \cap \{\Phi > 0\}} \vec{u}_g dV \quad (10)$$

$$\bar{\rho} \int_V dV = \rho_l \int_{V \cap \{\Phi < 0\}} dV + \rho_g \int_{V \cap \{\Phi > 0\}} dV \quad (11)$$

$$\bar{\rho} = \rho_l H(\Phi) + \rho_g (1 - H(\Phi)) \quad (12)$$

Fluid properties in interface cells

Viscosity:

$$\int_V \bar{\dot{\gamma}} dV = \int_{V \cap \{\Phi < 0\}} \dot{\gamma}_l dV + \int_{V \cap \{\Phi > 0\}} \dot{\gamma}_g dV \quad (9)$$

$$\frac{1}{\bar{\mu}} \int_V \bar{\mu} \bar{\dot{\gamma}} dV = \frac{1}{\mu_l} \int_{V \cap \{\Phi < 0\}} \mu_l \dot{\gamma}_l dV + \frac{1}{\mu_g} \int_{V \cap \{\Phi > 0\}} \mu_g \dot{\gamma}_g dV \quad (10)$$

$$\frac{1}{\bar{\mu}} \int_V \tau dV = \frac{1}{\mu_l} \int_{V \cap \{\Phi < 0\}} \tau_l dV + \frac{1}{\mu_g} \int_{V \cap \{\Phi > 0\}} \tau_g dV \quad (11)$$

$$\frac{1}{\bar{\mu}} \int_V dV = \frac{1}{\mu_l} \int_{V \cap \{\Phi < 0\}} dV + \frac{1}{\mu_g} \int_{V \cap \{\Phi > 0\}} dV \quad (12)$$

$$\frac{1}{\bar{\mu}} \approx \frac{H(\Phi)}{\mu_l} + \frac{1 - H(\Phi)}{\mu_g} \quad (13)$$

Shear rate in the liquid phase.
 (Essential to calculate the viscosity)

$$\int_{V \cap \{\Phi < 0\}} \dot{\gamma}_l dV = \int_V \bar{\dot{\gamma}} dV - \int_{V \cap \{\Phi > 0\}} \dot{\gamma}_g dV$$

$$\dot{\gamma}_l H(\Phi) = \left(\frac{1}{\bar{\mu}} - \frac{1}{\mu_g} (1 - H(\Phi)) \right) \tau$$

$$\dot{\gamma}_l H(\Phi) = \left(1 - \frac{\bar{\mu}}{\mu_g} (1 - H(\Phi)) \right) \bar{\dot{\gamma}}$$

